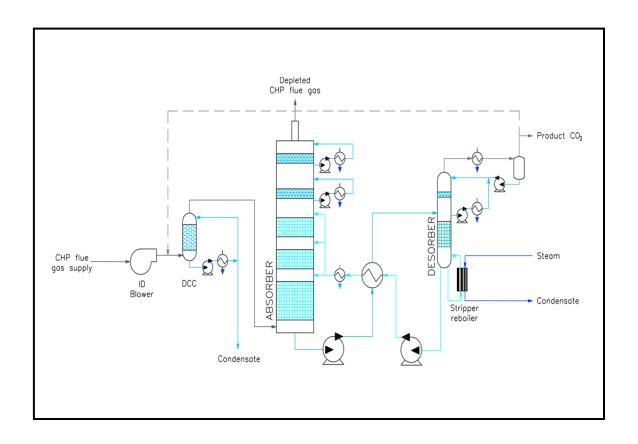


## FMH606 Master's Thesis 2019 Energy and Environmental Technology

# Process simulation of CO<sub>2</sub> absorption at TCM Mongstad



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#### **Summary:**

Developing robust and predictable process simulation tools for CO<sub>2</sub> capture is important for improving carbon capture technology and reduce man made CO<sub>2</sub> emissions.

In this thesis, five different scenarios of experimental data from the amine based CO<sub>2</sub> capture process at TCM have been simulated in rate-based model in Aspen Plus and equilibrium-based model in Aspen HYSYS and Aspen Plus. The simulations have been compared based on the prediction reliability for removal grade, temperature profile and rich loading.

In previous work, these five scenarios have been simulated and compared in Aspen HYSYS and Aspen Plus. Some of the results from earlier work are verified in this thesis.

The main purpose have been to fit the simulated results with performance data from TCM, and evaluate whether fitted parameters for one scenario gives reasonable predictions at other conditions. Two new  $E_M$ -profiles were estimated, and scaled to fit all five scenarios by developing an  $E_M$ -factor. From this work the new model with fitted parameters gave a reliable prediction of removal grade and temperature profile for all scenarios, and predicted more reliable results than rate-based model with estimated IAF.

The scenarios were also simulated with default E<sub>M</sub>-profile in Aspen HYSYS, where the removal grade was fitted to performance data by adjusting number of stages. The scenarios were also simulated with three different amine packages in Aspen HYSYS, Kent-Eisenberg, Li-Mather and Acid Gas - Liquid Treating.

## **Preface**

This report was written during the spring 2019 as my master thesis, and is part of the master program in Energy and Environmental technology at the Department of Process, Energy and Environment at the University of South-Eastern Norway.

The project focus is on performing process simulations of test data from the 2013 and 2015 campaign at TCM in Aspen HYSYS and Aspen Plus, and compare process simulations with performance data and earlier simulations of the same test data. The main purpose is to fit the removal grade, temperature profile and rich loading with performance data from TCM. Another purpose is to evaluate whether fitted parameters for one scenario gives reasonable predictions at other conditions.

I want to express my gratitude towards my supervisor, Professor Lars Erik Øi, for his supervision, guidance and great support during this thesis. Especially I appreciate that he made it possible for me to carry out all the work from Bodø, so that I was able to continue my job at Multiconsult and be with my family during the duration of this project.

I would also like to thank my family for their help and support during this work. Especially, I want to show gratitude to my boyfriend, Stefan, for his patience and help taking care of our son, Philip Edward, who turned two years during this project. I would like to thank him for giving me the time I needed to complete. Hopefully we will get more time together in the years to come.

The data-tools used during this project was:

Aspen HYSYS V10, Aspen Plus V10, MS Word 2013, MS Excel 2013 and AutoCAD Plant 3D 2018.

Bodø, 05.05.19

Sofie Fagerheim

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## **Nomenclature**

A-G Acid Gas - Liquid Treating (Amine package in Aspen HYSYS)

CCS Carbon capture and storage

CHP Combined Heat and Power plant

DCC Direct-Contact Cooler

DEA Diethanolamine

E<sub>M</sub> Murphree Efficency

e-NRTL Electrolyte non-random two-liquid (Amine package in Aspen Plus)

IAF Interfacial area factor

ID blower Inducted Draft blower

IPCC Intergovernmental Panel on Climate Change

K-E Kent-Eisenberg (Amine package in Aspen HYSYS)

L-M Li-Mather (Amine package in Aspen HYSYS)

MDEA Methyl diethanolamine

MEA Monoethanol amine

NOAA National Oceanic and Atmosperic Administration

RFCC Refinery Residue Fluid Catalytic Cracker

TCM Technology Centre Mongstad

USN University of South-Eastern Norway,

Earlier known as Telemark University College and University

College of Southeast Norway

Lean loading The CO<sub>2</sub> low amine entering the absorber

Removal grade Percent of CO<sub>2</sub> captured

Rich loading The CO<sub>2</sub> rich amine exiting the absorber

## 1 Introduction

#### 1.1 Background

TCM (Technology Centre Mongstad) is the world's largest facility for testing and improving CO<sub>2</sub> capture, and was started in 2006 when the Norwegian government and Statoil (now Equinor) made an agreement to establish the world's largest full scale CO<sub>2</sub> capture and storage project. To be able to predict process behavior, plan campaigns and verify results it is necessary to have good and robust simulation models.

There have been performed several projects at the University of Southeastern Norway, on process simulation of amine based CO<sub>2</sub> capture processes using Aspen HYSYS and Aspen Plus. Over the last decade, the MEA based CO<sub>2</sub> capture process at TCM have annually been simulated in master theses.

The focus of this report is on performing a literature review on process simulation of amine based CO<sub>2</sub> capture by absorption. Perform Aspen HYSYS and Aspen Plus simulations of the MEA based CO<sub>2</sub> capture process at TCM, and compare process simulations with performance data, and do a verification of some of the earlier work on this subject, performed in earlier master theses at USN.

#### 1.2 Outline of the thesis

In chapter 2, the carbon related climate change, and the carbon capture and storage technology is briefly described. The Process description of the CO<sub>2</sub> capture process at TCM is presented with a P&ID, followed by the chemistry of MEA and CO<sub>2</sub> absorption. A short presentation of the earlier work on the subject is reviewed. The chapter finishes with a problem description.

In chapter 3, the simulation methodology is presented, introducing different simulation tools, Murphree efficiency, and necessary calculations. A new method of estimating Murphree efficiency and fitting Murphree efficiencies with removal grade by introducing an E<sub>M</sub>-factor is developed The five scenarios used in this thesis is introduced, with performance data and input data to simulation. The chapter finishes with specification of simulation tools.

In chapter 4, the earlier theses of Zhu, Sætre and Røsvik is verified in Aspen HYSYS and Aspen Plus for all five scenarios. The simulations with the new estimated Murphree efficiency profiles in Aspen HYSYS, and simulations with the new estimated Murphree efficiency profiles and estimated interfacial area factor in Aspen Plus is presented. Followed by a comparison of the results from Aspen HYSYS and Aspen Plus. In the end the scenarios have been simulated with default Murphree efficiencies estimated by Aspen HYSYS, and with three different amine packages (Kent-Eisenberg, Li-Mather and Acid Gas).

In chapter 5, a method of estimating E<sub>M</sub>-factor based on performance data is suggested.

In chapter 6, the results from the verification, and different simulations is evaluated. A comparison between results from earlier work and results from this work is discussed and some further work is suggested.

Chapter 7 is the conclusion of the thesis.

## 2 Background and problem description

This chapter gives a brief introduction to carbon related climate change, CO<sub>2</sub> capture technologies, description of the process at TCM, summary of earlier work on the subject, and in the end a problem description.

#### 2.1 Climate change related to CO2 emission

When greenhouse gases are released to the atmosphere, they strengthen the greenhouse effect and trap heat, causing the planet surface to warm. CO<sub>2</sub> is the primary greenhouse gas emitted through human activities, mainly from burning fossil fuel. [1]

The graph in figure 2.1 shows atmospheric CO<sub>2</sub> levels measured in ppm at Mauna Loa Observatory in Hawaii, for a little more than a decade. The circle at the end of the graph shows the latest measurement from march 2019, where the level had passed 410 ppm. [2]

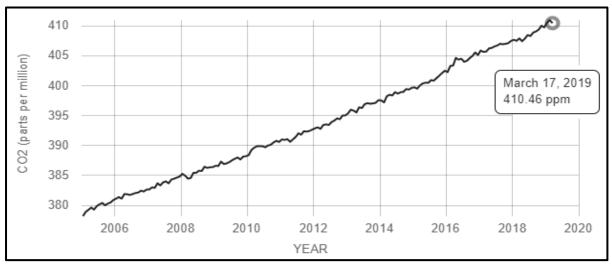


Figure 2.1: Atmospheric CO<sub>2</sub> levels measured at Mauna Loa Observatory, Hawaii. [2]

From the graph, it is clear that the CO<sub>2</sub> level in the atmosphere is increasing and will probably continue to increase in the years to come, if not some drastic changes are made. There have been implemented several protocols to reduce the global climate changes, the latest one in Paris 2015, where the main mitigation was focused on reducing emissions.

As mentioned, the largest source of CO<sub>2</sub> emissions from human activities comes from burning fossil fuels for electricity, heat and transportation. It is therefore implemented measures for these sources to emission. One measure is to develop technology to capture CO<sub>2</sub> and store it for sufficient time.

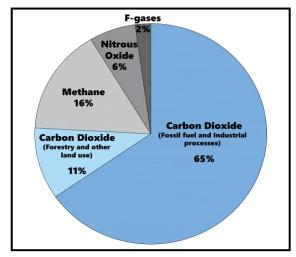


Figure 2.2: Global greenhouse gas emissions by gas, based on emissions from 2010. [1]

## 2.2 Carbon capture technologies

According to IPCC (Intergovernmental Panel on Climate Change) One considerable way to reduce climate change is CCS (Carbon Capture and Storage) [3].

There are mainly four ways to capture  $CO_2$  from a combustion process [4, 5].

#### 2.2.1 Pre-combustion CO<sub>2</sub> capture process

A pre-combustion system involves converting solid, liquid or gaseous fuel into syngas (a mixture of  $H_2$  and  $CO_2$ ) without combustion. This way the  $CO_2$  can be removed from the mixture before the  $H_2$  is used for combustion. Syngas can be produced in several ways e.g. gasification or pyrolysis.

#### 2.2.2 Post-combustion CO<sub>2</sub> capture process

By post-combustion capture, CO<sub>2</sub> can be captured from the exhaust of a combustion process by absorbing it in a solvent. The absorbed CO<sub>2</sub> is liberated from the solvent and compressed for transportation and storage. Post-combustion technology is currently the most mature process for CO<sub>2</sub> capture.

#### 2.2.3 Oxy-fuel combustion CO<sub>2</sub> capture process

In the process of oxy-fuel combustion,  $O_2$ , instead of air, is used for combustion. This oxygenrich, nitrogen-free atmosphere results in final flue-gases consisting mainly of  $CO_2$  and  $H_2O$ .

#### 2.2.4 Chemical looping CO<sub>2</sub> capture process

The chemical looping process is similar to the oxy-fuel combustion, but a metal oxide is used as an oxygen carrier for the combustion, instead of pure oxygen. During the process, metal oxide is reduced to metal while the fuel is oxidized to CO<sub>2</sub> and water.

## 2.3 Carbon transport and storage

After capturing the  $CO_2$ , it needs to be transported by pipeline, ships, trucks or rail for storage at a suitable storage facility where it can remain for a long period of time. The transportation of  $CO_2$  is very similar to transportation of natural gas, so the existing technology of transportation is considered safe [6].

Suited storage sites needs to obtain the pressure and temperature required for the CO<sub>2</sub> to remain in the liquid or supercritical phase. Such sites are typically located several kilometers under the earth's surface. Suitable storage sites include former oil and gas fields, deep saline formations or depleting oil fields where the injected CO<sub>2</sub> may increase the amount of oil recovered [4].

#### 2.4 Process description at TCM

The TCM pilot-scale amine plant was designed and constructed by Aker Solutions and Kværner. The amine plant was designed to be flexible, to allow testing of different configurations, and has respective capacities of about 80 and 750 tons CO<sub>2</sub>/day for CHP (Combined Heat and Power plant) and RFCC (refinery residue fluid catalytic cracker) flue gas operations. This paper is focused on the process with CO<sub>2</sub> capture of CHP flue gas [7]. Figure 2.3 shows a simplified process flow diagram, the numbers in the process description refers to this figure, the figure is inspired by Figure 1 in Thimsen et al., (2014) [8].

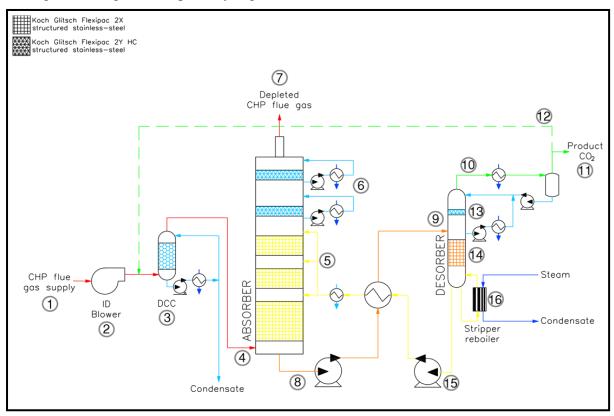


Figure 2.3: Simplified process flow diagram of the amine based CO<sub>2</sub> capture process plant at TCM

#### 2.4.1 Flue gas treatment

- 1. The flue gas containing CO<sub>2</sub> comes from the CHP at Mongstad refinery, located close to TCM.
- 2. An ID (induced draft) blower sucks the flue gas out of the CHP chimney, and transports it to TCM through insulated pipes, to avoid temperature drops, which will lead to water condensation inside the pipelines. The ID blower prevents pressure drops and blows the flue gas through the plant with a blower output capacity of up to about 270 mbar and 70,000 Sm<sup>3</sup>/h
- 3. A DCC (direct-contact cooler) system is placed after the ID blower, to quench and lower the temperature of the flue gas with a counter-current flow of water in order to improve the efficiency of the absorption process and provide pre-scrubbing on the flue gas.

#### 2.4.2 CO<sub>2</sub> capture

- 4. The cooled flue gas enters an absorber, to remove  $CO_2$  from the flue gas using an amine solvent called MEA (monoethanolamine). The absorber has a rectangular polypropylene-lined concrete column with a cross section measuring 3.55x2m and a total height of 62m.
- 5. The amine solution contacts the flue gas in the lower region of the column, which consist of three sections of structured stainless-steel packing of 12 m, 6 m and 6 m of height.
- 6. In the upper region of the column, water-wash systems are located to scrub and clean the flue gas, particularly of any solvent carry over. The water-wash system consists of two sections of structured stainless-steel packing, both have a height of 3 m. The water-wash system is also used to maintain the water balance of the solvent by using heat exchangers to adjust the temperature of the circulating water.
- 7. The CO<sub>2</sub> depleted flue gas exits the absorber column through a stack located at the top of the absorber.
- 8. The rich amine exits at the bottom of the absorber, and is from there pumped to the top of the absorption packing in the stripper. During this transportation, the rich amine recovers heat from the lean amine exiting the stripper, through a cross-flow heat exchanger.

#### 2.4.3 Amine regeneration

- 9. The stripper column recover the captured CO<sub>2</sub> and return lean solvent to the absorber. At TCM there is two independent stripper columns, the column used for CHP flue gas is cylindrical and has a diameter of 1.3 m and a height of 30 m. The other stripper column is larger and is utilized when treating flue gases of higher CO<sub>2</sub> content.
- 10. The stripper column has an overhead condenser system where CO<sub>2</sub> and water leaving the stripper is cooled down to separate the water, which is led back to the stripper, by a reflux drum, condenser and pumps.
- 11. The cooled and dried CO<sub>2</sub> is released in to the atmosphere at a safe vent location.
- 12. A portion of the product CO<sub>2</sub> can also be recycled back to the inlet of the DCC to increase the concentration of CO<sub>2</sub> in the inlet flue gas stream.
- 13. The upper region of the stripper column consist of a rectifying water-wash section of structured stainless-steel packing, with a height of 1.6 m.
- 14. The lower region of the stripper consist of structured stainless steel packing with a height of 8m.
- 15. The lean amine exits at the bottom of the desorber, and is pumped through a cross-flow heat exchanger where it releases energy to the rich amine entering the desorber. The stripped lean amine is cooled down in another heat exchanger before it enters the absorber above each of the three absorber packings.
- 16. A stream of lean amine is re-heated by steam in a stripper reboiler and put back to the stripper to keep the stripper at desired temperature.

## 2.5 Chemistry of the process

In this subchapter the advantages and disadvantages of using MEA for CO<sub>2</sub> capture is weighted and the chemical reactions of the CO<sub>2</sub> absorption is described briefly.

The CO<sub>2</sub> is absorbed in a 30/70 wt% mixture of MEA solvent and water. It is absorbed by direct contact with the solvent-mixture in a 24 meter high packing section, of structured stainless-steel.

#### 2.5.1 Generally about MEA

MEA (monoethanolamine) is the amine used as solvent for the CO<sub>2</sub> absorbation in this paper. MEA has the formula H<sub>2</sub>NC<sub>2</sub>H<sub>4</sub>OH, and is a primary alkanolamine that often is used for CO<sub>2</sub> removal. Other amines that rapidly is used for CO<sub>2</sub> removal is the secondary alkanolamine, DEA (diethanolamine) and the tertiary amine, MDEA (methyl diethanolamine).

When used as solvents, the amines are typically 20-40 wt% solutions in water. MEA in water solution reacts fast with dissolved CO<sub>2</sub> to form carbamate, and has a high CO<sub>2</sub> capacity. Reaction 2.1 shows how MEA reacts as a weak base in water. [9]

$$MEA + H_2O \leftrightarrow HMEA^+ + OH^-$$
 R(2.1)

#### 2.5.2 Advantages and disadvantages of using MEA for CO<sub>2</sub> capture

The advantages of using MEA in CO<sub>2</sub> capture is its low molecular weight, which gives the MEA high capacity even at low concentrations. Another advantage is the high alkalinity of primary amines. MEA is also considered as a relatively cheap chemical compared with other amines available for CO<sub>2</sub> capture. The toxicity is relatively low and the environmental impact is less questionable than for other amines, because MEA occurs naturally in living organisms.

The disadvantages of using MEA is the high-energy consumption needed for desorption, which is a side effect of the high absorption efficiency. Another problem with MEA in contact with exhaust gas is its tendency to degrade in high temperature and react with oxygen and other components like sulphur oxides and nitrogen oxides [10, 9]. Another important issue is the CO<sub>2</sub> emitted during the production of MEA. When MEA is produced, CO<sub>2</sub> is emitted during the Haber-Bosch process. The regeneration of solvent after the absorption is also an indirect source of CO<sub>2</sub> emission, related to the use of fuels in i.e., combustion for energy supply. The evaluation of the overall balance of CO<sub>2</sub> emitted and captured is essential to determine the efficiency of the process [11].

#### 2.5.3 Reactions of CO<sub>2</sub> absorption into MEA

The following reactions describes how CO<sub>2</sub> can be absorbed into the mixture of MEA solution Reaction 2.2 describes how CO<sub>2</sub> in a gas can be absorbed in an aqueous liquid. [9]

$$CO_2(g) \leftrightarrow CO_2(aq)$$
 R(2.2)

Since all the reactions in this system occurs in the aqueous phase, the "aq" notation is skipped. Reaction 2.3 describes how in the aqueous phase  $CO_2$  reacts with hydroxide to bicarbonate.

$$CO_2 + OH^- \leftrightarrow HCO_3^-$$
 R(2.3)

The fast proton transfer reactions (2.4, 2.5 and 2.6) also occur.

Reaction 2.4 describes the ionization of water.

$$H_2O \leftrightarrow H^+ + OH^-$$
 R(2.4)

Reaction 2.5 describes the deprotonation of carbonic acid. At equilibrium, the concentration of H<sub>2</sub>CO<sub>3</sub> is negligible compared to the concentration of free CO<sub>2</sub>. In a CO<sub>2</sub> removal process, with a pH normally higher than 8.0 this reaction is often neglected because the concentration of H<sub>2</sub>CO<sub>3</sub> becomes very small.

$$H_2CO_3 \leftrightarrow H^+ + HCO_3^-$$
 R(2.5)

Reaction 2.6 describes the deprotonation of the bicarbonate ion to carbonate ion.

$$HCO_3^- \leftrightarrow H^+ + CO_3^{2-}$$
 R(2.6)

The absorption of  $CO_2$  into MEA solution can be described by reaction 2.7, where a protonated amine ion (MEAH<sup>+</sup>) and a carbamate ion (MEACOO<sup>-</sup>) is formed. A carbamate ion is a product of the reaction of  $CO_2$  and amine, when the amine is MEA the carbamate ion has the formula  $HN(C_2H_4OH)COO^-$ .

$$2MEA + CO_2 \leftrightarrow MEAH^+ + MEACOO^-$$
 R(2.7)

Reaction 2.8 describes how a protonated amine ion and bicarbonate (HCO<sub>3</sub><sup>-</sup>) is formed.

$$CO_2 + MEA + H_2O \leftrightarrow MEAH^+ + HCO_3^-$$
 R(2.8)

The total concentration of CO<sub>2</sub> is the sum of all the concentrations of the different forms:

$$C_{CO2,TOT} = C_{CO2} + C_{HCO3} + C_{CO3} + C_{HN(C2H4OH)COO}$$
 (2.1)

The total concentration of amine is the sum of all the concentration of the different forms:

$$C_{MEA.TOT} = C_{MEA} + C_{MEAH} + C_{HN(C2H4OH)COO}$$
 (2.2)

#### 2.6 Earlier work

Some of the relevant earlier work that has been done on simulating CO<sub>2</sub> absorption is presented in this subchapter.

- In 2007, Lars Erik Øi (USN) used Aspen HYSYS to simulate CO<sub>2</sub> removal by amine absorption from a gas based power plant. The results showed that adjusting the Murphree Efficiency outside the simulation tool could be a practical approach when using Aspen HYSYS to simulate CO<sub>2</sub> removal. The paper was published at the Conference on Simulation and Modelling SIMS2007 in Gøteborg. [12]
- In 2007, Finn A. Tobiesen, Hallvard F. Svendsen and Olav Juliussen from SINTEF, developed a rigorous rate-based model of acid gas absorption, and a simplified absorber model. They validated the models against mass-transfer data obtained from a 3 month campaign in a laboratory pilot-plant absorber. It was found that the simplified model was satisfactory for lower CO<sub>2</sub> loading, whiles the rigorous model had a better fit for higher CO<sub>2</sub> loading. [13]
- In 2008, Hanne M. Kvamsdal (SINTEF) and Gary T. Rochelle (University of Texas) studied the effects of temperature bulge in CO<sub>2</sub> absorption by MEA. They compared an Aspen Plus rate based absorber with 4 sets of experimental data from a pilot plant at the University of Texas, Austin. Several adjustments were made to the model in order to create a predictable model and to study effects of change in specific parameters. [14]

- In 2009, Luo et al., from NTNU, compared and validated sixteen data sets from four different pilot plant studies, with simulations in four different simulation tools (Aspen Plus equilibrium-based, Aspen Plus rate-based, ProMax, ProTreat<sup>TM</sup> and CO<sub>2</sub>SIM). They concluded that all the simulation tools were able to present reasonable predictions on overall performance of CO<sub>2</sub> absorption rate, while the reboiler duties, concentration and temperature profiles were less predictable. [15]
- In 2011, Espen Hansen worked on his master thesis at USN. Hansen compared Aspen HYSYS, Aspen Plus and ProMAX simulations of CO<sub>2</sub> capture with MEA. He concluded that Aspen HYSYS and Aspen Plus gives similar results, while the results from ProMAX deviated from the Aspen tools. Hansen found that Kent-Eisenberg model in Aspen HYSYS was similar to the Aspen Plus equilibrium-based model for the absorber, but there was a significant difference in the reboiler duties. [16]
- In 2012, Jostein Tvete Bergstrøm worked on his master thesis at USN. Bergstrøm compared Aspen HYSYS (Kent-Esienberg and Li-Mather), Aspen Plus (Rate-based and equilibrium) and ProMAX simulations of CO<sub>2</sub> capture with MEA. Bergstrøm found that the models gave similar results, and that the equilibrium-based model in Aspen Plus and Kent-Eisenberg model in Aspen HYSYS gave coinciding results. [17]
- In 2012, Lars Erik Øi (USN) compared Aspen HYSYS and Aspen Plus (rate-based and equilibrium) simulation of CO<sub>2</sub> capture with MEA. Øi found that there was small deviations in the equilibrium-based model in Aspen HYSYS and Aspen Plus. He found larger deviations between the equilibrium-based calculations and the rate-based calculations. [18]
- In 2013, Ying Zhang and Chau Chyun Chen simulated nineteen data sets of CO<sub>2</sub> absorption in MEA with Aspen rate-based model and the traditional equilibrium-based model. Their result show that rate-based model yields reasonable predictions on all key performance measurements, while equilibrium-based model fails to reliably predict these key performance variables. [19]
- In 2013, Stian Holst Pedersen kvam worked on his master thesis at USN. Kvam compared Aspen Plus (rate based and equilibrium) and Aspen HYSYS (Kent-Eisenberg and Li-mather) simulations of CO<sub>2</sub> capture with MEA. The primary goal was to compare the energy consumption of a standard process, a process with vapour recompression and a vapour recompression with split stream, and not to evaluate the performance of the absorber. [20]
- In 2013, Even Solnes Birkelund worked on his master thesis at UIT. Birkelund compared a standard absorption process, a vapour recompression process and a lean split with vapour recompression process. He simulated the models in Aspen HYSYS and used Kent-Eisenberg as thermodynamic model for the aqueous amine solution, and Peng-Robinson for the vapour phase. All configurations were evaluated due to the energy cost. The results showed that lean split vapour recompression and vapour recompression had the lowest energy cost, while the standard absorption process was simulated to have a much higher energy cost. [21]

- In 2014, Lars Erik Øi et al, simulated different absorption and desorption configurations for 85% amine based CO<sub>2</sub> removal, from a natural gas based power plant using Aspen HYSYS. They simulated a standard process, split-stream, vapour recompressions and different combinations thereof. The simulations were used as a basis for equipment dimensioning, cost estimation and process optimization. [22]
- In 2014, Lars Erik Øi and Stian Holst Pedersen Kvam from USN, simulated different absorption and desorption configurations for 85% CO<sub>2</sub> removal from a natural gas fired combined cycle power plant, with the simulation tools Aspen HYSYS and Aspen Plus. In Aspen Plus, both an equilibrium-based model including Murphree Efficiency and a rate-based model were used. The results show that all simulation models calculate the same trends in the reduction of equivalent heat consumption, when the absorption process configuration were changed from the standard process. [23]
- In 2014, Inga Strømmen Larsen worked on her master thesis at USN. Larsen simulated a rate based Aspen Plus model and compared the results to experimental data from TCM. Larsen found that the Aspen Plus model TCM used was in general agreement with the experimental data. Larsen found temperature and loading profiles similar to the experimental data by adjusting parameters. She also did comparison of mass transfer correlations in Aspen Plus. [24]
- ❖ In 2014 Espen Steinseth Hamborg et al, published a paper with the results from the MEA testing at TCM during the 2013 test campaign. The paper reveals CO₂ removal grade, temperature measurement, and experimental data for the process. [7]
- In 2015 Espen Steinseth Hamborg from TCM presented some of the results from the campaign in 2013 and the results from USN-student Inga Strømmen Larsen's master thesis from 2014, at the PCCC3 in Canada. A v.7.3 Aspen Plus rate-based model was compared to the experimental data. The temperature and loading profile from Aspen Plus presented in this paper gave a good reproduction of the experimental data. [25]
- In 2015, Solomon Aforkoghene Aromada and Lars Erik Øi studied how reduction of energy consumption can be achieved by using alternative configurations. They simulated standard vapour recompression and vapour recompression combined with split stream configurations in Aspen HYSYS, for 85% amine-based CO<sub>2</sub> removal. The results showed that it is possible to reduce energy consumption with both the vapour recompression and the vapor recompression combined with split-stream processes. [26]
- In 2015, Coarlie Desvignes worked on a master thesis at Lyon CPE. Desvignes evaluated the performance of the TCM flowsheet model in Aspen Plus, and compared with the data obtained in the 2013 and 2014 test campaign at TCM. Desvignes found that the Aspen Plus model TCM used performed quite well for 30 and 40wt% MEA, but not for higher flue gas temperature and solvent flowrate. [10]

- In 2015, Ye Zhu worked on his master thesis at USN. Zhu simulated an equilibrium model in Aspen HYSYS, Based on the data from TCM 2013 campaign published in Hamborg et al [7]. Zhu adjusted the Murphree Efficiency to fit the CO<sub>2</sub> removal grade and temperature profile from the experimental results. Zhu found that linear decrease in Murphree efficiency from top to bottom gave good temperature predictions. [27]
- In 2016, Kai Arne Sætre worked on a master's thesis at USN. Sætre simulated seven sets of experimental data from the amine based CO<sub>2</sub> capture process at TCM, with Aspen HYSYS (Kent-Eisenberg and Li-Mather) and Aspen Plus (rate-based and equilibrium). He found that it is possible to fit a rate-based model by adjusting the IAF and equilibrium-based model by adjusting the E<sub>M</sub>, both Aspen HYSYS and Aspen Plus will give good results if there are only small changes in the parameters. [28]
- In 2016, Babak Pouladi, Mojtaba Nabipoor Hassankiadeh and Flor Behroozshad, studies the potential to optimize the conditions of CO<sub>2</sub> capture of ethane gas in phase 9 and 10 of south pars in Iran, using DEA as absorbent solvent. They simulated the process in Aspen HYSYS and found the effect of temperature to be significant. [29]
- In 2017, Monica Garcia, Hanna K. Knuutila and Sai Gu, validated a simulation model of the desorption column built in Aspen Plus v8.6. They used four experimental pilot campaigns with 30wt% MEA. The results showed a good agreement between the experimental data and the simulated results. [30]
- In 2017, Mohammad Rehan et al., studied the performance and energy savings of installing an intercooler in a CO<sub>2</sub> capture system based on chemical absorption with MEA as absorption solvent. They used Aspen HYSYS to simulate the CO<sub>2</sub> capture model. The results showed improved CO<sub>2</sub> recovery performance and potential of significant savings in MEA solvent loading and energy requirements, by installing an intercooler in the system. [31]
- ❖ In 2017 Leila Faramarzi et al, published a paper with the results from the MEA testing at TCM during the 2015 test campaign. The paper reveals CO₂ removal grade, temperature measurement, and experimental data for the process. [32]
- In 2018, Ole Røsvik worked on his master thesis at USN. Røsvik simulated the TCM data from the test campaign in 2013, published by Hamborg et al [7]. And the data from TCM's test campaign in 2015, published by Faramarzi et al [32] in Aspen HYSYS and Aspen Plus (equilibrium and rate-based). He found that both Aspen HYSYS and Aspen Plus will give good results if there are only small changes in the parameters. [33]
- In 2018, Lare Erik Øi, Kai Arne Sætre and Espen Steinseth Hamborg, compared four sets of experimental data from the amine based CO<sub>2</sub> capture process at TCM, with different equilibrium-based models in Aspen HYSYS and Aspen Plus, and a rate based model in Aspen Plus. The results show that equilibrium and rate-based models perform equally well in both fitting performance data and in predicting performance at changed conditions. The paper was presented at the Conference on Simulation and Modelling SIMS 59 in Oslo. [34]

## 2.7 Problem description

#### Background

TCM is offered to vendors of solvent based CO<sub>2</sub> capture and is mostly running on the vendor's solvents and parameters. TCM does not have permission to publish the results conducted at the vendor's premises. However, TCM have conducted their own test-campaigns in order to publish results.

The results from one scenario from TCM's test-campaign in 2013 was published by Hamborg et al., (2014) [7], and the result from one scenario from the test-campaign in 2015 was published by Faramarzi et al., (2017) [32].

USN and NTNU have produced several papers on amine based CO<sub>2</sub> capture with different simulation tools, throughout the last decade. Performance data from the test-campaigns at TCM have been used in these papers. In addition to the published results some un-published results have been provided to USN by TCM. The repeated conclusion from these papers have been that the rate-based model in Aspen Plus, and the equilibrium-based model in Aspen HYSYS and Aspen Plus perform equally well in both fitting performance data, and in predicting performance at changed conditions. The model with fitted parameters will give a predictable simulation only when there are small changes in process parameters [15] [16] [17] [18] [23] [28] [33] [34].

Another published papers state that the rate-based model yields reasonable predictions on all key performance measurements, while equilibrium-based model fails to predict reliable performance variables [19].

#### **Approach**

In this thesis the candidate have simulated 5 scenarios from the test-campaigns at TCM from 2013 and 2015. The candidate have tried to further develop the method of estimating Murphree efficiencies for equilibrium-based models. The candidate have also compared the accuracy of rate-based model and equilibrium-based model in Aspen Plus and Aspen HYSYS.

#### Aim of Project

The aim of the project was to contribute to achieve predictable models which gives an accurate removal grade and satisfactory temperature- and loading profile. The model should be easy to use for several scenarios with different parameters, and be able to predict reasonable results even when the parameters are changed.

Another aim of the project was to compare if rate-based model and the equilibrium-based model will perform equally well in predicting reliable performance data.

## 3 Method

In this chapter the method for the simulations, the Murphree efficiency, some necessary calculations methods and decisions is presented and explained. A new  $E_M$ -factor is developed. The experimental data from TCM's test campaigns is presented with the input data to the simulations, and specifications of the simulation tools.

## 3.1 Simulation methodology

The data from TCM is for some cases given in units that needs to be converted to be implemented in Aspen HYSYS and Aspen Plus. Some necessary decisions and fittings needed to be done.

- Only the absorber is simulated
- Experimental data from TCM is converted to units that can be used as parameters in the simulation program
- The pressure loss over the absorber is assumed to be zero
- The main goal is to achieve the same CO<sub>2</sub> removal grade, temperature profile and rich loading as in performance data for the five scenarios.
- The second goal is to compare the reliability in predicting performance data for equilibrium-based model with estimated E<sub>M</sub>-profile and rate-based model with estimated IAF.

#### 3.1.1 Simulation tools

Several simulation programs can be used to calculate CO<sub>2</sub> removal by absorption, such as Aspen HYSYS, Aspen Plus, Pro/II, ProTreat and ProMax. In this thesis, the process simulation tool that have been used to perform simulation of CO<sub>2</sub> absorption into amine solution are the equilibrium-based models in Aspen HYSYS and Aspen Plus, and the rate-based model in Aspen Plus. The equilibrium-based models are based on the assumption of equilibrium at each stage. By introducing a Murphree efficiency, the model can be extended. Rate-based models are based on rate expressions for chemical reactions, mass transfer and heat transfer.

#### 3.1.2 Murphree efficiency

There are few tools available for the estimation of stage efficiencies in CO<sub>2</sub> absorption columns. There is a model available for estimation of Murphree efficiency for one plate in a plate column. The estimation model is based on the work of Tomcej et al., (1987) [35], modified later by Rangwala et al., (1992) [36]. This model is based on the assumption that a pseudo first order absorption rate expression is valid. However, there is no model for estimation of Murphree efficiency for a specific packing section height in a structured packing column.

The calculation of necessary column height for CO<sub>2</sub> removal is an important design factor in CO<sub>2</sub> absorption using amine solutions. A simple way to improve the available estimation model is to use Murphree efficiencies for a specific packing height. In a plate column, an efficiency value is estimated for each tray based on the ratio of change in mole fraction from a stage to the next, divided by the change assuming equilibrium. In a packed column, a packing height

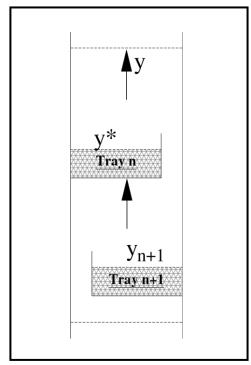


Figure 3.1: Illustration of Murphree efficiency, inspired by Øi (2012) [9].

of e.g. 1 meter could be defined as one tray with a Murphree efficiency. The Murphree efficiencies can be estimated outside the simulation program, before it is implemented to the simulation program. The overall tray efficiency is defined in equation 3.1, as the number of ideal equilibrium trays divided by the actual number of trays.

$$E_O = \frac{N_{IDEAL}}{N_{REAL}} \tag{3.1}$$

The Murphree tray efficiency related to the gas side for tray number "n" is traditionally defined by equation 3.2 [37].

$$E_M = \frac{(y - y_{n+1})}{(y^* - y_{n+1})} \tag{3.2}$$

Where y is the mole fraction in the gas from the tray,  $y_{n+1}$  is the mole fraction from the tray below and  $y^*$  is in equilibrium with the liquid at tray n. This is illustrated in figure 3.1.

Table 3.1 Murphree efficiencies used in this thesis

Murı	Murphree efficiencies for each meter of the packed column from top to bottom								
EM	0,1	Zhu	Lin	SF1	SF2				
1	0.1	0.2300	0.17	0,2450	0,2400				
2	0.1	0.2192	0.17	0,2425	0,2350				
3	0.1	0.2085	0.17	0,2400	0,2300				
4	0.1	0.1977	0.17	0,2375	0,2250				
5	0.1	0.1869	0.17	0,2350	0,2200				
6	0.1	0.1800	0.16	0,2325	0,2150				
7	0.1	0.1762	0.15	0,2300	0,2300				
8	0.1	0.1546	0.14	0,2000	0,2000				
9	0.1	0.1438	0.13	0,1700	0,1700				
10	0.1	0.1331	0.12	0,1400	0,1400				
11	0.1	0.1223	0.11	0,1100	0,1100				
12	0.1	0.1115	0.10	0,0800	0,0800				
13	0.1	0.1007	0.09	0,0500	0,0550				
14	0.1	0.0900	0.08	0,0475	0,0525				
15	0.1	0.0100	0.07	0,0450	0,0500				
16	0.1	0.0100	0.06	0,0425	0,0475				
17	0.1	0.0100	0.05	0,0400	0,0450				
18	0.1	0.0100	0.04	0,0375	0,0425				
19	0.1	0.0100	0.03	0,0350	0,0400				
20	0.1	0.0100	0.02	0,0001	0,0001				
21	0.1	0.0100	0.01	0,0001	0,0001				
22	0.1	0.0100	0.01	0,0001	0,0001				
23	0.1	0.0100	0.01	0,0001	0,0001				
24	0.1	0.0100	0.01	0,0001	0,0001				

The Murphree efficiencies of each stage in the 24m high packed column we have at TCM, is estimated for 24 stages of 1m height, the Simulations have been done with both constant and varying efficiency for all stages.

Table 3.1 presents some estimated Murphree efficiency profiles from earlier simulations of TCM data.  $E_M = 0.1$  was simulated in Zhu (2015) [27] to see how constant Murphree efficiency impacts the simulating results. He simulated data from Hamborg et al., (2014) [25], and found that the best fit for removal grade and temperature profile was  $E_M = Zhu$ .  $E_M = Zhu$  were later used for several scenarios by Sætre (2016) [28].  $E_M = Lin$ , was the best fit, according to Røsvik (2018) [33] where he simulated data from Faramarzi et al., (2017) [32].

The mentioned  $E_M$ -profiles have been simulated in this report to verify earlier work, and new  $E_M$ -profiles have been estimated based on these results.  $E_M = SF1$  and  $E_M = SF2$  have been estimated in this thesis to fit scenario H14, and also scaled to fit the other scenarios by introducing an  $E_M$ -factor. (See 3.2.2)

#### 3.1.3 Converting Sm<sup>3</sup>/h to kmol/h

The inlet gas flow is given in Sm<sup>3</sup>/h and needs to be given in kmol/h. In 2016, Sætre [28] created a formula to calculate the mole flow, this is given in equation 3.3. The factor 0.023233 is calculated based on standard conditions chosen by TCM to be 15°C and 1 atm, and the ideal gas law.

$$\left[\frac{kmol}{h}\right] = \left[\frac{Sm^3}{h}\right] \times \frac{1}{0,023233} \left[\frac{mol}{Sm^3}\right] \tag{3.3}$$

He commented that the results from using this formula deviated from measured data for some of the scenarios, where inlet gas flow was given in both volume flow and molar flow. He concluded that these deviations probably occurred due to uncertainties in the measured data of the experimental data at TCM. Therefore he decided to use the calculated molar flow instead of the measured molar flow, for those scenarios. This decision have also been used for this thesis.

#### 3.1.4 Calculating composition of lean amine

The lean amine is specified in the reports from TCM [7] [32], by the following parameters:

- Lean MEA concentration in water [wt%]
- Lean CO<sub>2</sub> loading [mol CO<sub>2</sub> / mol MEA]
- Lean amine supply flow rate [kg/h]
- Lean amine supply flow temperature [°C]
- Lean amine density [kg/m<sup>3</sup>]

To get the most accurate result, it is desired to implement the mole fractions of the lean amine in to the simulations. To accomplish this, some calculation is necessary.

Sætre used a method where he found the molar flow of MEA by using the weight%, mass flow and molar weight, implemented in equation 3.4.

$$\frac{kmol\ MEA}{h} = \frac{MEA\ [wt\%\ in\ water] \times mass\ flow\ rate\ \left[\frac{kg}{h}\right]}{MEA\ molar\ weight\ \left[\frac{kmol}{kg}\right]} \tag{3.4}$$

Following, the H<sub>2</sub>O molar flow can be found with the same method, shown in equation 3.5.

$$\frac{kmol H_2 O}{h} = \frac{(1 - MEA)[wt\% in water] \times mass flow rate \left[\frac{kg}{h}\right]}{H_2 O \ molar \ weight \left[\frac{kmol}{kg}\right]}$$
(3.5)

Finally, the CO<sub>2</sub> molar flow can be found by implementing the MEA molar flow and Lean CO<sub>2</sub> loading into equation 3.6.

$$\frac{kmol\ CO_2}{h} = MEA\ molar\ flow\ rate\ \left[\frac{kmol}{h}\right] \times CO_2\ loading\ \left[\frac{kmol\ CO_2}{kmol\ MEA}\right] \tag{3.6}$$

When all the tree molar flows are found the molar fractions is easily calculated and can be implemented to the simulations.

#### 3.1.5 Calculating CO<sub>2</sub> removal grade

The CO<sub>2</sub> capture efficiency can be quantified in four ways as described in Thimsen et al., (2014) [8] and shown in table 3.2, in addition CO<sub>2</sub> recovery calculation is given in table 3.2, and is a measure of the CO<sub>2</sub> mass balance [7].

Table 3.2: Methods for calculating CO<sub>2</sub> removal grade and CO<sub>2</sub> recovery

Method 1	Method 2	Method 3	Method 4	CO <sub>2</sub> Recovery
$\frac{P}{S}$	$\frac{P}{P+D}$	$\frac{S-D}{S}$	$1 - \frac{O_{CO2}}{1 - O_{CO2}} \frac{(1 - I_{CO2})}{I_{CO2}}$	$\frac{D+P}{S}$

S = Flue gas supply

OCO<sub>2</sub> = Depleted flue gas CO<sub>2</sub> content, dry basis

D = Depleted flue gas

ICO<sub>2</sub> = Flue gas supply CO<sub>2</sub> content, dry basis

P = Product CO<sub>2</sub>

In this report method 3, from table 3.2, is used to calculate removal grade. This method is only dependent on the CO<sub>2</sub> flow in the flue gas supply and the depleted flue gas, the CO<sub>2</sub> flow from the desorber is not included in these calculations. The uncertainty of this method was calculated to be 2,8% in Hamborg et al., (2014) [7], but it was stated that it might be even higher.

## 3.2 Suggested method for estimating Murphree efficiency

#### 3.2.1 Estimating E<sub>M</sub>-profile by calculating overall removal efficiency

To calculate an estimated Murphree efficiency profile the overall removal grade based on the efficiency of each stage, was calculated with equation 3.7. Where y is the CO<sub>2</sub> removal efficiency of each stage in the absorber packing and n is the number of stages.

removal grade = 
$$100\% - (100\% \cdot ((1 - y_1) \cdot (1 - y_2) \cdot (\dots) \cdot (1 - y_n)))$$
 (3.7)

The calculated efficiency was compared with the simulated efficiency. The results showed that an  $E_M$ -profile calculated to  $\approx 94\%$  gave a simulated result close to 90% for scenario H14. For scenario 2B5 an  $E_M$ -profile calculated to  $\approx 89.4\%$  gave a simulated result close to 87.3%. For scenario 6w an  $E_M$ -profile calculated to  $\approx 81.1\%$  gave a simulated result close to 83.7%. For scenario Goal1 an  $E_M$ -profile calculated to  $\approx 92.3\%$  gave a simulated result close to 90.1%. For scenario F17 an  $E_M$ -profile calculated to  $\approx 85.3\%$  gave a simulated result close to 83.7%. When the required overall efficiency was estimated, the Murphree efficiency of each stage was adjusted to fit the temperature profile of the performance data. This was performed in excel, by adjusting the efficiencies of each stage while keeping the overall removal efficiency close to the estimated required overall efficiency level.

#### 3.2.2 Fitting E<sub>M</sub> to several scenarios by introducing an E<sub>M</sub>-factor

This method evolves around the idea that two similar scenarios with different removal grade might fit the same  $E_M$ -profile. If one  $E_M$ -profile provides a good fit to the temperature profile of one scenario with high removal grade, the idea is that the  $E_M$ -profile can be scaled down to fit the temperature profile of another scenario with lower removal grade, or scaled up to fit a scenario with even higher removal grade. The method is given by equation 3.8.

Where y is the Murphree efficiency of each stage, n is the number of stages, k is a constant, from now on known as the  $E_M$ -factor, estimated by guessing a value of k, and adjusting the value until the requested removal grade for the new scenario is achieved by equation 3.7. Here e.g. the bisection method could be used to converge to the correct  $E_M$ -factor.

#### 3.3 Scenarios

This subchapter contains the most important data from all five scenarios used in this report. These scenarios are used as performance data for the simulations in this report, and are all taken from test-campaigns at TCM in 2013 and 2015. All scenarios were run with amine concentrations close to 30 wt% MEA in water. The scenarios are given in tables with performance data and tables with converted data implemented to the simulations.

#### 3.3.1 Scenario H14

Scenario H14 is data from the report published by Hamborg et al., (2014) [7]. This report was produced during the 2013-test campaign at TCM. The scenario was a part of an independent verification protocol, it had low MEA-emissions and MEA-related degradation, and was within all emission limits set by the Norwegian Environment Agency [28].

This scenario has been used in several Master theses at USN earlier, and some of the results are verified in sub-chapter 4.1 and 4.2.

Table 3.3 shows the experimental and measured data from TCM and table 3.4 shows the input data to the simulation. The complete data set is attached in appendix B.

	TCM data for scenario H14						
Amine inlet Flue gas inlet							
Flow rate	[kg/h]	54900	Flow rate	[Sm³/h]	46970		
Temperature	[C]	36.5	Temperature	[C]	25.0		
MEA (CO <sub>2</sub> free)	[wt%]	30.00	CO <sub>2</sub>	[vol%]	3.70		
loading	[mol CO <sub>2</sub> / molMEA]	0.23	O <sub>2</sub>	[vol%]	13.60		

Table 3.3: Experimental and measured data from TCM for scenario H14

Table 3.4: Input data to simulations for scenario H14
---

Input data for scenario H14						
Amine inlet			Flue gas inlet			
Flow rate	[kg/h]	54900	Flow rate	[kmol/h]	2022	
Temperature	[C]	36.5	Temperature	[C]	25.0	
MEA	[mol%]	10.94	CO <sub>2</sub>	[mol%]	3.70	
H <sub>2</sub> O	[mol%]	86.54	H <sub>2</sub> O	[mol%]	2.95	
CO <sub>2</sub>	[mol%]	2.52	O <sub>2</sub>	[mol%]	13.60	
Pressure	[bara]	1.0313	$N_2$	[mol%]	79.75	
			Pressure	[bara]	1.0630	

The removal grade is given to be close to 90.0% in Hamborg et al., (2014) [7].

The inlet flue gas molar flow is calculated by equation 3.3 in chapter 3.1.3, and the mole fractions of the lean amine is found by using the method in chapter 3.1.4. The flue gas compositions is given in vol% for  $O_2$  and  $CO_2$  but is used as mol% in the simulations. The fraction of  $H_2O$  is assumed from similar scenarios like 6w in Sætre (2016) [28]. The implemented parameters are the same parameters as used in  $\emptyset$ i, Sætre and Hamborg (2018) [34].

#### 3.3.2 Scenario 2B5

Scenario 2B5 is data from the 2015-campaign at TCM, that was supplied to USN from TCM.

This scenario were used in Sætre's Master thesis from USN (2016) [28], some of the results are verified in this report in sub-chapter 4.1 and 4.2.

Table 3.5 shows the experimental and measured data from TCM and table 3.6 shows the input data to the simulation. Different from scenario H14 and F17, this scenario is given with four different measured sets of temperature profiles, with an average removal grade for all sets. The complete data set from appendix J in Sætre (2016) [28] is attached in appendix D.

TCM data for scenario 2B5 Flue gas inlet Amine inlet Flow rate [kg/h] 49485 Flow rate [Sm<sup>3</sup>/h]46982 Temperature [C] 36.8 Temperature [C] 28.2 MEA (CO<sub>2</sub> free) [wt%] 31.60 [mol%] 3.57  $CO_2$ loading 0.20  $O_2$ [mol%] 14.60 [mol CO<sub>2</sub>/ molMEA] H<sub>2</sub>O [mol%] 3.70  $N_2$ [mol%] 77.20 Ar [mol%] 0.90

Table 3.5: Experimental and measured data from TCM for scenario 2B5

Table 3.6: Input data to simulations for scenario 2B5

Input data for scenario 2B5						
Amine inlet			Flue gas inlet			
Flow rate [kg/h] 49485			Flow rate	[kmol/h]	2022	
Temperature	[C]	36.8	Temperature	[C]	28.2	
MEA	[mol%]	11.67	CO <sub>2</sub>	[mol%]	3.57	
H <sub>2</sub> O	[mol%]	85.65	H <sub>2</sub> O	[mol%]	3.70	
CO <sub>2</sub>	[mol%]	2.68	O <sub>2</sub>	[mol%]	14.60	
Pressure	[bara]	1.0313	N <sub>2</sub>	[mol%]	78.08	
			Pressure	[bara]	1.0630	

The average removal grade is given to be 87.3% in the data set from TCM. The implemented parameters to the simulation are the same parameters as used in Øi, Sætre and Hamborg (2018) [34].

#### 3.3.3 Scenario 6w

Scenario 6w is data from the 2013-campaign at TCM, the data is collected from appendix D in the master's thesis of Sætre (2016) [28].

This scenario have earlier been used in the USN master's theses of Larsen (2014) [24], Desvignes (2015) [10] and Sætre (2016) [28]. Some of the results from Sætre's theses are verified in this report in sub chapter 4.1 and 4.2.

Table 3.7 shows the experimental and measured data from TCM and table 3.8 shows the input data to the simulation. Like scenario 2B5, this scenario is given with four different measured sets of temperature profiles, with an average removal grade for all sets. The complete data set from appendix D in Sætre (2016) [28] is attached in appendix D.

TCM data for scenario 6w							
Amine inlet			Flue gas inlet				
Flow rate	[kg/h]	54915	Flow rate	[Sm³/h]	46602		
Temperature	[C]	36.9	Temperature	[C]	25.0		
MEA (CO <sub>2</sub> free)	[wt%]	30.40	CO <sub>2</sub>	[mol%]	3.57		
loading	[mol CO <sub>2</sub> /	0.25	O <sub>2</sub>	[mol%]	13.60		
	molMEA]		H <sub>2</sub> O	[mol%]	3.00		
			N <sub>2</sub>	[mol%]	79.83		
			Ar	[mol%]	0.00		

Table 3.7: Experimental and measured data from TCM for scenario 6w

Table 3.8: Input data to simulations for scenario 6w

Input data for scenario 6w							
Amine inlet			Flue gas inlet				
Flow rate	[kg/h]	54915	Flow rate	[kmol/h]	2005		
Temperature	[C]	36.9	Temperature	[C]	25.0		
MEA	[mol%]	11.13	CO <sub>2</sub>	[mol%]	3.57		
H <sub>2</sub> O	[mol%]	86.37	H <sub>2</sub> O	[mol%]	3.00		
CO <sub>2</sub>	[mol%]	2.50	O <sub>2</sub>	[mol%]	13.60		
Pressure	[bara]	1.0313	N <sub>2</sub>	[mol%]	79.83		
			Pressure	[bara]	1.0630		

The average removal grade is given to be 79.0% in the data set from TCM. The implemented parameters to the simulation are equal to the parameters used in Øi, Sætre and Hamborg (2018) [34].

#### 3.3.4 Scenario Goal1

Scenario Goal1 is data from the 2015-campaign at TCM, that was supplied to USN from TCM. The data is collected from appendix K in the master's thesis of Sætre (2016) [28].

This scenario were used in Sætre's Master thesis from USN (2016) [28], some of the results are verified in this report in sub chapter 4.1.

Table 3.9 shows the experimental and measured data from TCM and table 3.10 shows the input data to the simulation. Just like for Scenario 2B5 and 6w, this scenario is given with four different measured sets of temperature profiles, with an average removal grade for all sets. The complete data set from appendix K in Sætre (2016) [28] is attached in appendix E.

TCM data for scenario Goal1							
Amine inlet			Flue gas inlet				
Flow rate	[kg/h]	44391	Flow rate	[Sm³/h]	46868		
Temperature	[C]	36.5	Temperature	[C]	25.0		
MEA (CO <sub>2</sub> free)	[wt%]	32.40	CO <sub>2</sub>	[mol%]	3.62		
loading	[mol CO <sub>2</sub> /	0.20	O <sub>2</sub>	[mol%]	14.30		
	molMEA]		H <sub>2</sub> O	[mol%]	3.10		
_			N <sub>2</sub>	[mol%]	78.10		
			Ar	[mol%]	0.90		

Table 3.9: Experimental and measured data from TCM for scenario Goal1

Table 3.10: Input data to simulations for scenario Goal1

Input data for scenario Goal1					
Amine inlet		Flue gas inlet	Flue gas inlet		
Flow rate	[kg/h]	44391	Flow rate	[kmol/h]	2017
Temperature	[C]	36.5	Temperature	[C]	25.0
MEA	[mol%]	11.57	CO <sub>2</sub>	[mol%]	3.62
H <sub>2</sub> O	[mol%]	86.29	H <sub>2</sub> O	[mol%]	3.10
CO <sub>2</sub>	[mol%]	2.14	O <sub>2</sub>	[mol%]	14.30
Pressure	[bara]	1.0313	N <sub>2</sub>	[mol%]	79.00
			Pressure	[bara]	1.0630

The average removal grade is given to be 90.1% in the data set from TCM. The implemented parameters to the simulation are the same parameters as used in Øi, Sætre and Hamborg (2018) [34]. Except for the lean amine temperature, which was 28.6 °C in Sætre (2016) and Øi, Sætre and Hamborg (2018). From appendix K in Sætre (2016) the lean amine temperature was found to be 36.5 °C, while the rich amine temperature was 28.6 °C. The mole fraction composition of amine was also adjusted to fit the MEA wt% from performance data.

#### 3.3.5 Scenario F17

Scenario F17 is data from the report published by Faramarzi et al, (2017) [32]. This report was produced during the 2015- test campaign at TCM. The scenario was part of an independent verification protocol, Emission levels of MEA, NH<sub>3</sub>, aldehydes, nitrosamines and other compounds were also measured and were all below the permissible levels set by the Norwegian Environment Agency.

This scenario was used in the USN master thesis of Røsvik (2018) [33]. Some of the results are verified in sub chapter 4.1 and 4.2.

Table 3.11 shows the experimental and measured data from TCM and table 3.12 shows the input data to the simulation. The complete data set is attached in appendix F.

TCM data for scenario F17					
	Amine inlet		1	Flue gas inlet	
Flow rate	[kg/h]	57434	Flow rate	[Sm³/h]	59430
Temperature	[C]	37.0	Temperature	[C]	29.8
MEA (CO <sub>2</sub> free)	[wt%]	31.00	CO <sub>2</sub>	[vol%]	3.70
loading	[mol CO <sub>2</sub> / molMEA]	0.20	O <sub>2</sub>	[vol%]	14.60

Table 3.11: Experimental and measured data from TCM for scenario F17

Table 3.12: Input data to simulations for scenario F17	Table 3.12:	Input data	to simulations	for scenario F1	7
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Input data for scenario F17						
Amine inlet			Flue gas inlet	Flue gas inlet		
Flow rate	[kg/h]	57434	Flow rate	[kmol/h]	2558	
Temperature	[C]	37.0	Temperature	[C]	29.8	
MEA	[mol%]	11.44	CO <sub>2</sub>	[mol%]	3.70	
H <sub>2</sub> O	[mol%]	86.27	H <sub>2</sub> O	[mol%]	3.70	
CO <sub>2</sub>	[mol%]	2.29	O <sub>2</sub>	[mol%]	14.60	
Pressure	[bara]	1.0313	N <sub>2</sub>	[mol%]	78.00	
			Pressure	[bara]	1.0100	

The removal grade is given to be close to 83.5% in Faramarzi et al., (2017) [32].

The inlet flue gas molar flow is calculated by equation 3.3 in chapter 3.1.3, and the mole fractions of the lean amine is found by using the method in chapter 3.1.4, just like for scenario H14. The flue gas compositions is given in vol% for  $O_2$  and  $CO_2$  but is used as mol% in the simulations. The implemented parameters are the same parameters as used in Røsvik (2018) [33].

## 3.4 Specifications of the simulation tools

#### 3.4.1 Equilibrium-based model

The Aspen HYSYS equilibrium-based file used in this thesis is named "KaiHamborgABSver.HSC"

Properties of the file is given in table 3.13 below.

Table 3.13: Specification for Aspen HYSYS Equilibrium-based model

Specifications - Aspen HYSYS Equilibrium					
Properties					
Amine package	Kent-Eisenberg				
(Amine packages used for	(Li-Mather)				
comparison in chapter 4.7)	(Acid Gas - Liquid Treating)				
Abso	orber				
Number of stages	24				
Nominal pressure	106.3 [kPa]				
Rat	ing				
Uniform section	Yes				
Internal type	Sieve				
Diameter	3m				
Tray space	0.5				
Weeping factor	1000				

The Aspen Plus equilibrium-based file used in this thesis is named "Aspenpluseq6w.apwz". Properties of the file is given in table 3.14 below.

Table 3.14: Specification for Aspen Plus Equilibrium-based model

Specifications - Aspen Plus Equilibrium					
Properties					
Method	ElecNRTL				
Henry comp ID	MEA				
Chemistry ID	MEA				
Configuration					
Calculation type	Equilibrium				
Number of stages	24				
Valid phases	Vapor-Liquid				
Pressure stage 1	1.04 bara				
Efficiencies					
Efficiency type	Murphree Efficiency				
Method	Individual comp.				
Rating					
Not specified					

#### 3.4.2 Rate-based model

The Aspen Plus rate-based file used in this thesis is named "TCM2B5Rev6-4\_abs.apw". The specifications in this file is provided in the table below.

Table 3.15: Specification of the model used for rate-based simulation

Tuble 3.13. Specification of the model used for face based simulation						
Specifications - Aspen Plus Rate-based						
Calculation type	Rate-based					
Number of stages	50					
Efficiency type	Vaporization efficiencies					
Reaction ID	MEA-NEW					
Holdup	0.0001 stage 1 to 50					
Reaction conduction factor	0.9					
Packing type	Koch metal 2x					
Section diameter [m]	3					
Section packed height [m]	24					
Flow model	Countercurrent					
Interfacial area factor	0.29 to 1					
Film Liquid phase	Discrxn					
Film Vapor phase	Film					
Mass transfer coeff method	Bravo et al., (1985)					
Heat transfer coeff method	Chilton and Colburn					
Interfacial area method	Bravo et al., (1985)					
Holdup method	Bravo et al., (1992)					
Add. Discretize points liquid	5					

The files used in both Aspen HYSYS and Aspen Plus have been provided to me by my supervisor, these files were created and used by Sætre (2016) [28], for his master thesis. These files are the basis for figure 3 and 4 in Øi, Sætre and Hamborg (2018) [34].

## 4 Results

This chapter presents the results from the simulations of all scenarios in Aspen Plus and Aspen HYSYS. The five scenarios have been used for earlier master theses:

- Scenario H14 have been simulated in both Aspen HYSYS and Aspen Plus in earlier master thesis's at USN. In 2015 Ye Zhu simulated the scenario in Aspen HYSYS, for his master thesis. Then in 2016 and 2018, Kai Arne Sætre and Ole Røsvik, respectively, simulated the same scenario in both Aspen HYSYS and Aspen Plus.
- Scenario 2B5 have been simulated in both Aspen HYSYS and Aspen Plus in Kai Arne Sætre's master thesis from 2016.
- Scenario 6w have been simulated in both Aspen HYSYS and Aspen Plus in earlier USN master's theses by Larsen (2014), Desvignes (2015) and Sætre (2016).
- Scenario Goal1 have been simulated in both Aspen HYSYS and Aspen Plus in Kai Arne Sætre's master thesis from 2016.
- Scenario F17 have been simulated in both Aspen HYSYS and Aspen Plus in Ole Røsvik's master thesis from 2018.

An introduction and description of the simulations in each sub-chapter is given below:

#### • 4.1 Verification of earlier work in Aspen HYSYS

This sub-chapter presents the simulation of the five scenarios compared with results from earlier work and performance data. All data in this sub-chapter is simulated in equilibrium-based model in Aspen HYSYS with Kent Eisenberg as amine package.

The simulated temperature profile from Aspen HYSYS compared with simulated results from earlier theses is attached in appendix G.

#### • 4.2 Verification of earlier work in Aspen Plus

This sub-chapter presents the simulation of the five scenarios compared with results from earlier work and performance data. All scenarios have been simulated in rate-based model and equilibrium-based model in Aspen Plus with e-NRTL.

The simulated temperature profile from Aspen Plus compared with simulated results from earlier theses is attached in appendix H.

#### 4.3 Simulation in Aspen HYSYS with estimated E<sub>M</sub>

Earlier studies have focused on the packed section as one packing with Murphree efficiencies from top to bottom. The results from these studies showed that a linear decrease in Murphree efficiency from the top to the lower middle of the packing, followed by a low constant efficiency for the bottom part of the packing have given the best fit to the temperature profile, e.g.  $E_M$ =Zhu.

During this project several combinations of Murphree efficiencies have been tested, some of them based on the idea that the three separated packing sections in the column might have higher efficiencies at the top of each section, because fresh amine enters at the top of each section. Based on this theory, two new  $E_M$ -profiles were estimated with equation 3.7,  $E_M$ =SF1 and  $E_M$ =SF2. Both with linearly decreasing efficiency in each packing section in the packed column. These two sets was first estimated for Scenario H14, and later scaled to fit the other scenarios, by introducing the  $E_M$ -factor in equation 3.8.

In this sub-chapter the five  $E_M$ -profiles given in table 3.1 in sub chapter 3.1.2, have been scaled for each scenario to produce requested removal grade in simulation. All simulations in this sub-chapter have been simulated in equilibrium-based model in Aspen HYSYS with Kent Eisenberg.

The estimated Murphree efficiency profiles is attached in appendix I, along with the simulated temperature profiles and important data from simulation.

Some interesting connections between  $E_M$ -factor and performance data was seen in the results from these simulations, which led to the calculations in chapter 5.

#### • 4.4 Simulation in Aspen Plus with estimated E<sub>M</sub> and IAF

In this sub-chapter all the  $E_M$ -profiles used in sub-chapter 4.3 have been scaled to achieve requested removal grade for all  $E_M$ -profiles in all five scenarios in Aspen Plus, by adjusting the  $E_M$ -factor. The simulations have been simulated in equilibrium-based model in Aspen Plus with e-NRTL.

The interfacial area factor have been adjusted to achieve requested removal grade for all scenarios in rate-based model in Aspen plus.

The estimated IAF is attached in appendix J, along with the simulated temperature profiles and important data from simulation.

#### • 4.5 Comparison of Rate-based and Equilibrium-based model

In this sub-chapter the simulated results from sub-chapter 4.3 and 4.4 have been compared.

The simulated temperature profiles and important data from simulation is attached in appendix K.

#### • 4.6 Simulation with default E<sub>M</sub> in Aspen HYSYS

There is a possibility to get Aspen HYSYS to estimate the Murphree efficiencies, these efficiencies is from now on called default efficiencies. The method that was used to achieve the requested removal grade with default efficiencies, was to vary the amount of stages in the packed column. In this sub chapter the simulations of each scenario with default efficiencies have been compared with the results from the estimated simulation of  $E_M$ =SF1 for each scenario.

The default  $E_M$ -profiles estimated by Aspen HYSYS is attached in appendix L, along with the simulated temperature profiles and important data from simulation.

#### 4.7 Comparison of Kent-Eisenberg, Li-Mather and Acid-Gas

There is three equilibrium-based amine packages available for simulation of absorption in Aspen HYSYS. In earlier master theses from USN, Kent-Eisenberg and Li-Mather have been compared. In this sub-chapter all three amine packages are compared for all scenarios with all the  $E_{M}$ -profiles used in the simulation chapter.

In this sub-chapter each scenario is presented with a figure that compares the temperature profiles for each set of Murphree efficiency simulated with each of the three amine packages. Each scenario is also presented with a table that compares the key data for each set of Murphree efficiency simulated with each of the three amine packages.

The simulated temperature profiles and important data for all simulations in this subchapter is attached in appendix M.

Comments on the results from all simulations can be found in chapter 6.

## 4.1 Verification of earlier work in Aspen HYSYS

#### 4.1.1 Verification of scenario H14 in Aspen HYSYS

In the first simulation the Murphree efficiency was adjusted to 0,1 and was constant for all stages. Figure 4.1 shows the temperature profiles for performance data and simulated data, compared with simulated data from Zhu (2015) [27], Sætre (2016) [28] and Røsvik (2018) [33]. Table 4.1 shows the key results from simulation compared with performance data, and data from earlier simulations of the same scenario.

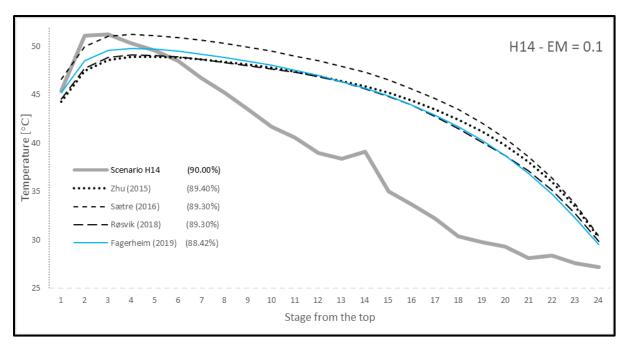


Figure 4.1: Verification of Scenario H14 with  $E_M = 0.1$  (HYSYS)

Table 4.1: Key results from simulation of scenario H14 with  $E_M = 0.1$  (HYSYS)

	TCM data	Zhu (2015)	Sætre (2016)	Røsvik (2018)	Fagerheim (2019)
Removal grade	90.00%	89.40%	87,00%	89.30%	88.42%
Rich loading	0.4800	0.4870	0.4920	-	0.4885
Ttop [°C]	45.40	44.29	46.60	44,52	45.20
Tmax [°C]	51.20	48.93	51.20	49,10	49.79
Tbtm [°C]	27.20	30.26	30.40	29,84	29,48

In 2015 Zhu [27] simulated scenario H14 and adjusted the Murphree efficiency to fit the temperature profiles. He achieved the best fit, for both removal grade and temperature profile when he adjusted the first stages (1-14) linearly from 0.23-0.09, the remaining stages (15-24) were set constant to 0.01 for each stage. In this thesis, this E<sub>M</sub>-profile is called Zhu.

Figure 4.2 presents the temperature profiles with E<sub>M</sub> adjusted according to Zhu.

Table 4.2 provide the key results from simulation compared with performance data, and data from earlier simulations of the same scenario.

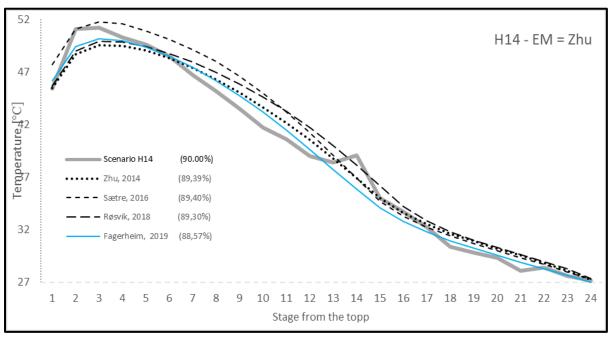


Figure 4.2: Verification of Scenario H14 with  $E_M = Zhu$  (HYSYS)

Table 4.2: Key results from simulation of scenario H14 with  $E_M = Zhu$  (HYSYS)

	TCM data	Zhu (2015)	Sætre (2016)	Røsvik (2018)	Fagerheim (2019)
Removal grade	90.00%	89.39%	86.90%	89.30%	88.57%
Rich loading	0.4800	0.4789	0.4910	-	0.4890
Ttop [°C]	45.40	45.48	47.70	45.66	46.14
Tmax [°C]	51.20	49.56	51.80	49.94	50.16
Tbtm [°C]	27.20	27.22	27.30	27.38	27.00

### 4.1.2 Verification of scenario 2B5 in Aspen HYSYS

Figure 4.3 presents the results from the simulation of data for scenario 2B5 with  $E_{\rm M}=0.1$ . Scenario 2B5 consist of a data set with four sets of temperature measurements, the thick blue line in figure 4.3 is the average temperature values of each stage from the data set.

Table 4.3 provides the key results from the simulation compared with performance data and results from Sætre (2016) [28].

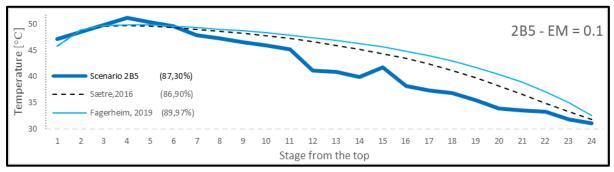


Figure 4.3: Verification of Scenario 2B5 with  $E_M = 0.1$  (HYSYS)

Table 4.3: Key results from simulation of scenario 2B5 with  $E_M = 0.1$  (HYSYS)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	87.30%	86.90%	89.97%
Rich loading	0.5000	0.4900	0.4715
Ttop [°C]	47.09	45.80	45.80
Tmax [°C]	51.47	49.70	49.89
Tbtm [°C]	30.99	31.80	32.51

Figure 4.4 and table 4.4 below, presents the results from the simulation of data for scenario 2B5 with  $E_M = Zhu$ .

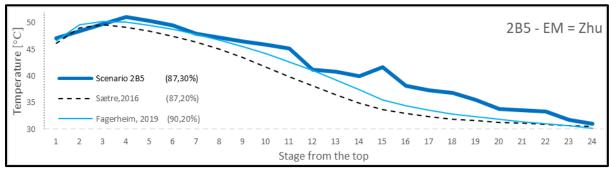


Figure 4.4: Verification of Scenario 2B5 with  $E_M = Zhu$  (HYSYS)

Table 4.4: Key results from simulation of scenario 2B5 with  $E_M = Zhu \; (HYSYS)$ 

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	87.30%	87.20%	90.20%
Rich loading	0.5000	0.4901	0.4722
Ttop [°C]	47.09	46.20	47.09
Tmax [°C]	51.47	49.10	51.16
Tbtm [°C]	30.99	30.50	30.74

#### 4.1.3 Verification of scenario 6w in Aspen HYSYS

Figure 4.5 presents the results from the simulation of data for scenario 6w with  $E_{\rm M}=0.1$ . Scenario 6w also consist of a data set with four sets of temperature measurements, the thick purple line in figure 4.5 is the average temperature values of each stage from the data set.

Table 4.5 provides the key results from the simulation compared with performance data and results from Sætre (2016) [28].

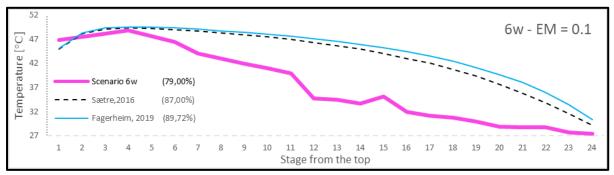


Figure 4.5: Verification of Scenario 6w with  $E_M = 0.1$  (HYSYS)

Table 4.5: Key results from simulation of scenario 6w with  $E_M = 0.1$  (HYSYS)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	79.00%	87.00%	89.72%
Rich loading	0.4600	0.4920	0.4721
Ttop [°C]	46.10	45.00	45.04
Tmax [°C]	49.35	49.30	49.52
Tbtm [°C]	27.33	29.10	30.33

Figure 4.6 and table 4.6 below, presents the results from the simulation of data for scenario 6w with  $E_M = Zhu$ .

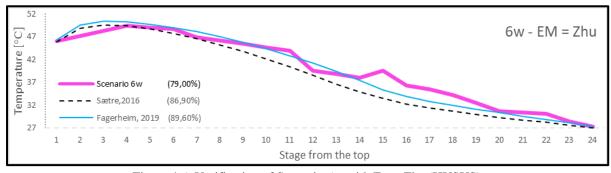


Figure 4.6: Verification of Scenario 6w with  $E_M = Zhu$  (HYSYS)

Table 4.6: Key results from simulation of scenario 6w with  $E_M = Zhu$  (HYSYS)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	79.00%	86.90%	89.60%
Rich loading	0.4600	0.4910	0.4721
Ttop [°C]	46.10	45.80	46.24
Tmax [°C]	49.35	49.50	50.29
Tbtm [°C]	27.33	27.00	27.30

#### 4.1.4 Verification of scenario Goal1 in Aspen HYSYS

Figure 4.7 presents the results from the simulation of data for scenario Goal1 with  $E_M = 0.1$ . Scenario Goal1 does also consist of a data set with four sets of temperature measurements, the thick gray line in figure 4.7 is the average temperature values of each stage from the data set.

Table 4.7 provides the key results from the simulation compared with performance data and results from Sætre (2016) [28].

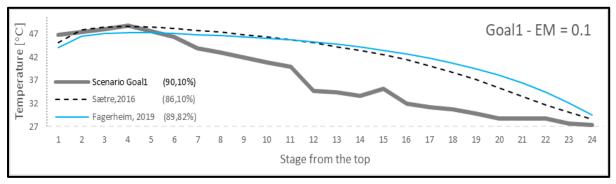


Figure 4.7: Verification of Scenario Goal1 with  $E_M = 0.1$  (HYSYS)

Table 4.7: Key results from simulation of scenario Goal1 with  $E_M = 0.1$  (HYSYS)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	90.10%	86.10%	89.82%
Rich loading	0.5000	0.5000	0.4863
Ttop [°C]	46.81	45.10	44.03
Tmax [°C]	48.81	48.70	47.30
Tbtm [°C]	27.31	28.50	29.55

Figure 4.8 and table 4.8 below, presents the results from the simulation of data for scenario Goal 1 with  $E_M = Zhu$ .

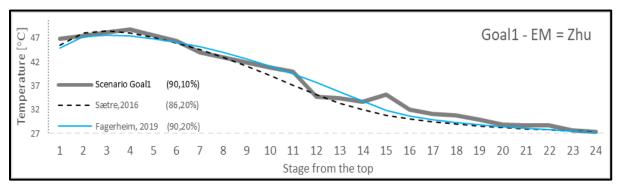


Figure 4.8: Verification of Scenario Goal1 with  $E_M = Zhu \; (HYSYS)$ 

Table 4.8: Key results from simulation of scenario Goal1 with  $E_{\text{M}}$  = Zhu (HYSYS)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	90.10%	86.20%	90.20%
Rich loading	0.5000	0.5000	0.4876
Ttop [°C]	46.81	45.50	44.83
Tmax [°C]	48.81	48.50	47.64
Tbtm [°C]	27.31	27.30	27.20

#### 4.1.5 Verification of scenario F17 in Aspen HYSYS

Figure 4.9 underneath presents the temperature profiles of performance data and simulated data for scenario F17 with  $E_M = 0.1$ , the thick black line in figure 4.9 is the temperature values of each stage from the data set.

Table 4.9 provides the key results from the simulation compared with performance data and results from Røsvik (2018) [33].

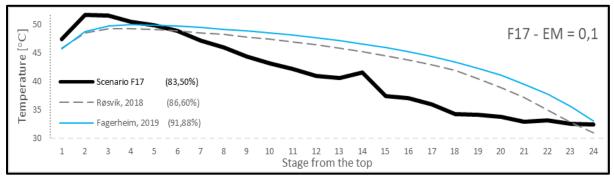


Figure 4.9: Verification of Scenario F17 with  $E_M = 0.1$  (HYSYS)

Table 4.9: Key results from simulation of scenario F17 with  $E_M = 0.1$  (HYSYS)

	TCM data	Røsvik (2018)	Fagerheim (2019)
Removal grade	83.50%	86.60%	91.88%
Rich loading	0.4800	-	0.3554
Ttop [°C]	47.40	45.84	45.72
Tmax [°C]	51.70	49.31	49.96
Tbtm [°C]	32.40	30.98	33.00

Figure 4.10 underneath presents the temperature profiles for performance data and simulated data for scenario F17 with  $E_M = Zhu$ , and table 4.10 provides the key results from the simulation compared with performance data and results from Røsvik (2018) [33].

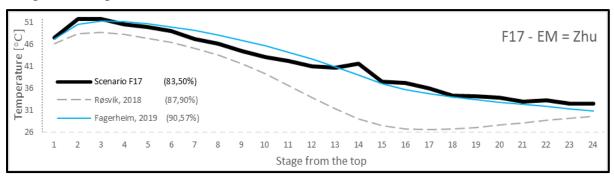


Figure 4.10: Verification of Scenario F17 with  $E_M = Zhu$  (HYSYS)

Table 4.10: Key results from simulation of scenario F17 with  $E_M = Zhu$  (HYSYS)

	TCM data	Røsvik (2018)	Fagerheim (2019)
Removal grade	83.50%	87.90%	90.57%
Rich loading	0.4800	-	0.4552
Ttop [°C]	47.40	46.04	47.09
Tmax [°C]	51.70	48.63	51.16
Tbtm [°C]	32.40	29.59	30.75

Figure 4.11 and table 4.11 underneath, shows the results from the simulation of data for scenario F17 with  $E_M = Lin$ , which was concluded to be the best fit in Røsvik's master's thesis from 2018 [33].

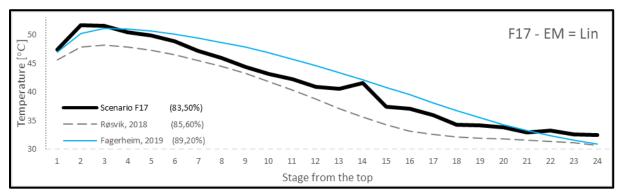


Figure 4.11: Verification of Scenario F17 with  $E_M = Lin (HYSYS)$ 

Table 4.11: Key results from simulation of scenario F17 with  $E_M = Lin (HYSYS)$ 

	TCM data	Røsvik (2018)	Fagerheim (2019)
Removal grade	83.50%	85.60%	89.20%
Rich loading	0.4800	-	0.4514
Ttop [°C]	47.40	45.60	46.92
Tmax [°C]	51.70	48.19	51.09
Tbtm [°C]	32.40	30.64	30.88

# 4.2 Verification of earlier work in Aspen Plus

## 4.2.1 Verification of scenario H14 in Aspen Plus

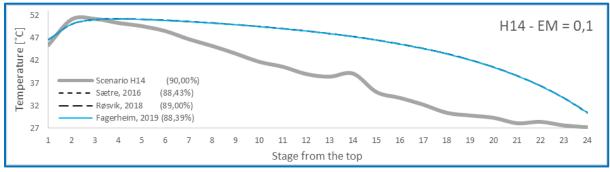


Figure 4.12: Verification of Scenario H14 with  $E_M = 0.1$  (Plus)

Table 4.12: Key results from simulation of scenario H14 with  $E_{\rm M}=0.1$  (Plus)

	TCM data	Sætre (2016)	Røsvik (2018)	Fagerheim (2019)
Removal grade	90.00%	87.20%	88.40%	88.40%
Rich loading	0.4800	0.4910	=	0.4880
Ttop [°C]	45.40	46.50	46.65	46.60
Tmax [°C]	51.20	50.90	51.28	51.19
Tbtm [°C]	27.20	30.20	30.50	30.43

Figure 4.12 presents the temperature profiles of performance data and data simulated in Aspen Plus for scenario H14 with  $E_M = 0.1$ , Table 4.12 provides the key results from the simulation compared with performance data and results from Sætre (2016) [28] and Røsvik (2018) [33].

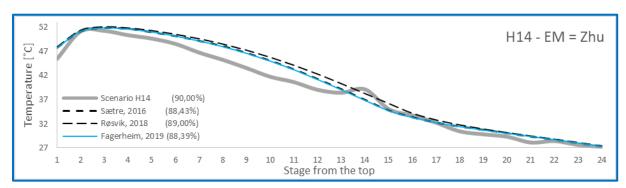


Figure 4.13: Verification of Scenario H14 with  $E_M = Zhu$  (Plus)

Table 4.13: Key results from simulation of scenario H14 with  $E_M = Zhu$  (Plus)

	TCM data	Sætre (2016)	Røsvik (2018)	Fagerheim (2019)
Removal grade	90.00%	86.90%	89.00%	88.39%
Rich loading	0.4800	0.4900	-	0.4880
Ttop [°C]	45.40	47.40	47.83	47.69
Tmax [°C]	51.20	51.20	52.03	51.79
Tbtm [°C]	27.20	27.50	27.33	27.29

Figure 4.13 presents the temperature profiles of performance data and simulated data for scenario H14 with  $E_M = Zhu$ , Table 4.13 provides the key results from the simulation compared with performance data and results from Sætre and Røsvik.

Figure 4.14 presents the temperature profiles of performance data and simulated data, simulated with Aspen Plus rate-based model for scenario H14, Table 4.14 provides the key results from the simulation compared with performance data and results from Sætre and Røsvik.

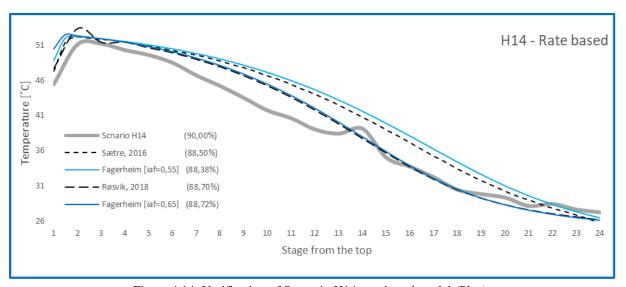


Figure 4.14: Verification of Scenario H14 rate-based model (Plus)

Table 4.14: Key results from simulation of scenario H14 rate-based model (Plus)

	TCM data	Sætre (2016)	Røsvik (2018)	Fagerhei	m (2019)
				IAF=0.55	IAF=0.65
Removal grade	90.00%	88.50%	88.70%	88.38%	88.72%
Rich loading	0.4800	0.4880	-	0.4881	0.4891
Ttop [°C]	45.40	48.10	47.73	48.82	50.46
Tmax [°C]	51.20	52.10	51.45	52.21	52.45
Tbtm [°C]	27.20	26.10	26.07	26.43	26.09

## 4.2.2 Verification of scenario 2B5 in Aspen Plus

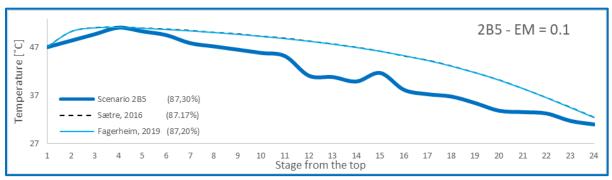


Figure 4.15: Verification of Scenario 2B5 with  $E_M = 0.1$  (Plus)

Table 4.15: Key results from simulation of scenario 2B5 with  $E_{\rm M}=0.1$  (Plus)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	87.30%	87.20%	87.20%
Rich loading	0.5000	0.4900	0,4887
Ttop [°C]	47.09	47.20	47.19
Tmax [°C]	51.47	51.20	51.17
Tbtm [°C]	30.99	32.40	32.41

Figure 4.15 presents the temperature profiles of performance data and simulated data for scenario 2B5 with  $E_M = 0.1$ , Table 4.15 provides the key results from the simulation compared with performance data and results from Sætre (2016) [28].

Figure 4.16 and table 4.16 presents the results from the simulation, compared with performance data and results from Sætre, for scenario 2B5 with  $E_M$ =Zhu.

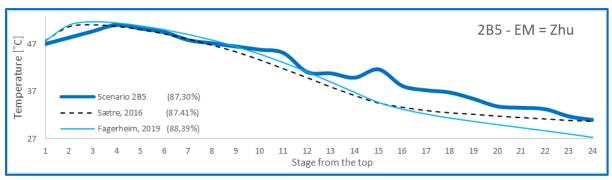


Figure 4.16: Verification of Scenario 2B5 with  $E_M = Zhu$  (Plus)

Table 4.16: Key results from simulation of scenario 2B5 with  $E_M = Zhu$  (Plus)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	87.30%	87.40%	88.39%
Rich loading	0.5000	0.4900	0.4880
Ttop [°C]	47.09	47.80	47.69
Tmax [°C]	51.47	51.20	51.78
Tbtm [°C]	30.99	30.70	27.28

Figure 4.17 presents the temperature profiles of performance data and simulated data, simulated with Aspen Plus rate-based model for scenario 2B5. Table 4.17 provides the key results from the simulation compared with performance data and results from Sætre.

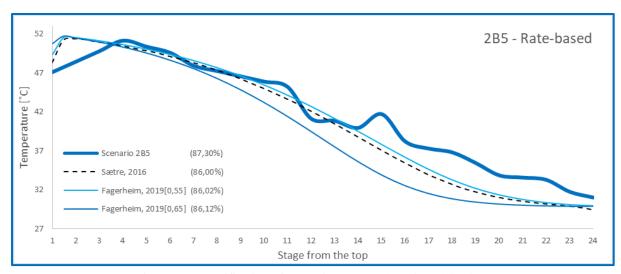


Figure 4.17: Verification of Scenario 2B5 rate-based model (Plus)

Table 4.17: Key results from simulation of scenario 2B5 rate-based model (Plus)

	TCM data	Sætre (2016)	Fagerheir	n (2019)
			IAF=0.55	IAF=0.65
Removal grade	87.30%	86.00%	86.02%	86.12%
Rich loading	0.5000	0.4900	0.4854	0.4856
Ttop [°C]	47.09	48.30	49.35	50.75
Tmax [°C]	51.47	51.50	51.54	51.71
Tbtm [°C]	30.99	29.50	29.94	29.87

### 4.2.3 Verification of scenario 6w in Aspen Plus

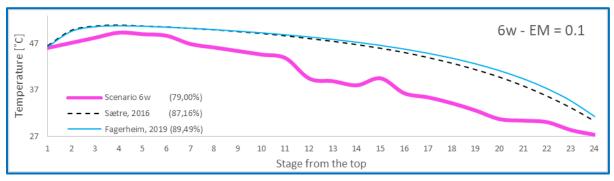


Figure 4.18: Verification of Scenario 6w with  $E_M = 0.1$  (Plus)

Table 4.18: Key results from simulation of scenario 6w with  $E_{\rm M}=0.1$  (Plus)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	79.00%	87.20%	89.49%
Rich loading	0.4600	0.4910	0.4707
Ttop [°C]	46.10	46.50	46.31
Tmax [°C]	49.35	50.90	50.80
Tbtm [°C]	27.33	30.20	31.26

Figure 4.18 and table 4.18 presents the results from the simulation, compared with performance data and results from Sætre, for scenario 6w with  $E_M$ =0.1.

Figure 4.19 and table 4.19 presents the results from the simulation, compared with performance data and results from Sætre, for scenario 6w with  $E_M$ =Zhu.

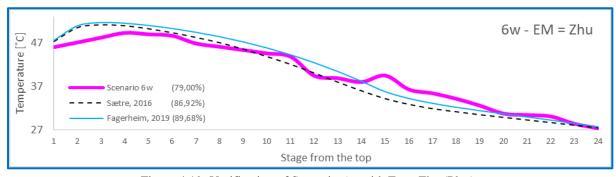


Figure 4.19: Verification of Scenario 6w with  $E_M = Zhu$  (Plus)

Table 4.19: Key results from simulation of scenario 6w with  $E_M = Zhu$  (Plus)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	79.00%	86.90%	89.68%
Rich loading	0.4600	0.4900	0.4702
Ttop [°C]	46.10	47.40	47.62
Tmax [°C]	49.35	51.20	51.73
Tbtm [°C]	27.33	27.50	27.64

Figure 4.20 and table 4.20 presents the results from the simulation, compared with performance data and results from Sætre, for scenario 6w with rate-based model.

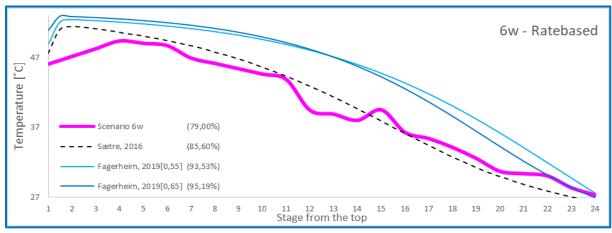


Figure 4.20: Verification of Scenario 6w rate-based model (Plus)

Table 4.20: Key results from simulation of scenario 6w rate-based model (Plus)

	TCM data	Sætre (2016)	Fagerheim (2	2019)
			IAF=0.55	IAF=0.65
Removal grade	79.00%	86.10%	93.53%	95.19%
Rich loading	0.4600	0.4880	0.4819	0.4865
Ttop [°C]	46.10	47.57	48.92	50.86
Tmax [°C]	49.35	51.33	52.38	52.86
Tbtm [°C]	27.33	26.17	27.63	26.94

## 4.2.4 Verification of scenario Goal1 in Aspen Plus

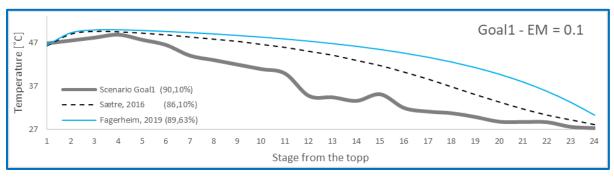


Figure 4.21: Verification of Scenario Goal1 with  $E_M = 0.1$  (Plus)

Table 4.21: Key results from simulation of scenario Goal1 with  $E_M = 0.1$  (Plus)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	90.10%	82.70%	89.63%
Rich loading	0.5000	0.5000	0.4854
Ttop [°C]	46.81	46.30	46.39
Tmax [°C]	48.81	49.60	49.93
Tbtm [°C]	27.31	28.10	30.29

Figure 4.21 and table 4.21 presents the results from the simulation, compared with performance data and results from Sætre, for scenario Goal1 with  $E_M$ =0.1.

Figure 4.22 and table 4.22 presents the results from the simulation, compared with performance data and results from Sætre, for scenario Goal1 with  $E_M$ =Zhu.

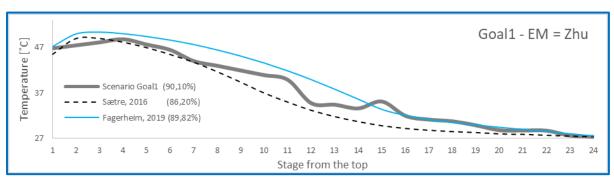


Figure 4.22: Verification of Scenario Goal1 with  $E_M = Zhu$  (Plus)

Table 4.22: Key results from simulation of scenario Goal1 with  $E_M = Zhu$  (Plus)

	TCM data	Sætre (2016)	Fagerheim (2019)
Removal grade	90.10%	82.70%	89.82%
Rich loading	0.5000	0.5000	0.4860
Ttop [°C]	46.81	46.50	47.22
Tmax [°C]	48.81	49.00	50.37
Tbtm [°C]	27.31	27.40	27.52

Figure 4.23 and table 4.23 presents the results from the simulation, compared with performance data and results from Sætre, for scenario Goal1 with rate-based model.

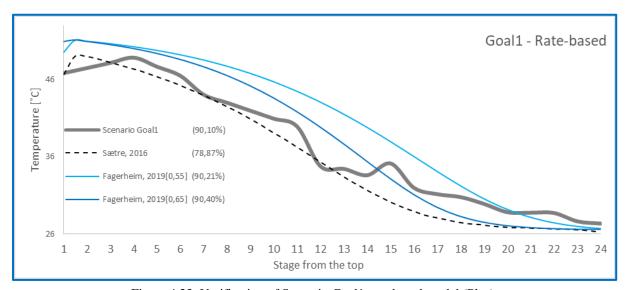


Figure 4.23: Verification of Scenario Goal1 rate-based model (Plus)

Table 4.23: Key results from simulation of scenario Goal1 rate-based model (Plus)

	TCM data	Sætre (2016)	Fagerheim (2	2019)
			IAF=0.55	IAF=0.65
Removal grade	90.10%	78.90%	90.21%	90.40%
Rich loading	0.5000	0.4900	0.4877	0.4880
Ttop [°C]	46.81	46.70	49.51	50.90
Tmax [°C]	48.81	49.00	51.05	51.11
Tbtm [°C]	27.31	26.20	26.68	26.57

## 4.2.5 Verification of scenario F17 in Aspen Plus

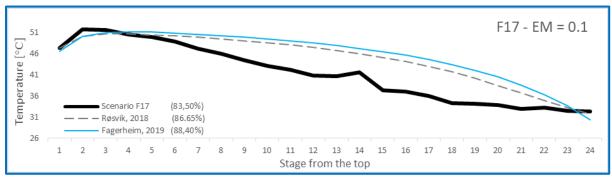


Figure 4.24: Verification of Scenario F17 with  $E_M = 0.1$  (Plus)

Table 4.24: Key results from simulation of scenario F17 with  $E_{\rm M}=0.1$  (Plus)

	TCM data	Røsvik (2018)	Fagerheim (2019)
Removal grade	83.50%	86.65%	88.40%
Rich loading	0.4800	-	0.4880
Ttop [°C]	47.40	47.34	46.59
Tmax [°C]	51.70	50.69	51.19
Tbtm [°C]	32.40	31.74	30.43

Figure 4.24 and table 4.24 presents the results from the simulation, compared with performance data and results from Røsvik (2018) [33], for scenario F17 with  $E_M$ =0.1.

Figure 4.25 and table 4.25 presents the results from the simulation, compared with performance data and results from Røsvik, for scenario F17 with  $E_M$ =Zhu.

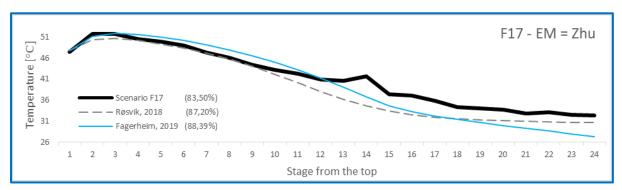


Figure 4.25: Verification of Scenario F17 with  $E_M = Zhu$  (Plus)

Table 4.25: Key results from simulation of scenario F17 with  $E_M = Zhu$  (Plus)

	TCM data	Røsvik (2018)	Fagerheim (2019)
Removal grade	83.50%	87.20%	88.39%
Rich loading	0.4800	-	0.4880
Ttop [°C]	47.40	47.72	47.69
Tmax [°C]	51.70	50.55	51.79
Tbtm [°C]	32.40	30.63	27.28

Figure 4.26 and table 4.26 presents the results from the simulation, compared with performance data and results from Røsvik, for scenario F17 with  $E_M$ =Lin, which was presented as the best result for scenario F17 in his thesis.

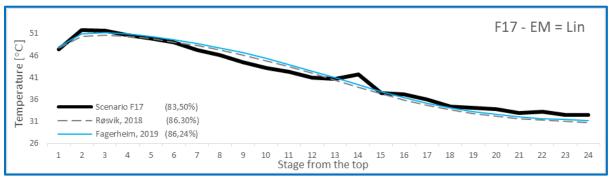


Figure 4.26: Verification of Scenario F17 with  $E_M = Lin$  (Plus)

Table 4.26: Key results from simulation of scenario F17 with  $E_M = Lin$  (Plus)

	TCM data	Røsvik (2018)	Fagerheim (2019)
Removal grade	83.50%	86.30%	86.24%
Rich loading	0.4800	-	0.4929
Ttop [°C]	47.40	47.58	47.97
Tmax [°C]	51.70	50.63	51.19
Tbtm [°C]	32.40	30.71	31.11

Figure 4.27 presents the temperature profiles of performance data and simulated data, simulated with Aspen Plus rate-based model for scenario F17, Table 4.27 provides the key results from the simulation compared with performance data and results from Røsvik.

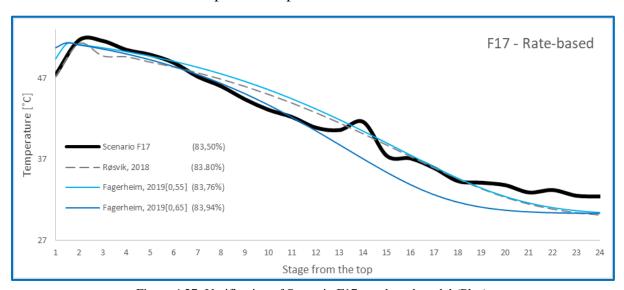


Figure 4.27: Verification of Scenario F17 rate-based model (Plus)

Table 4.27: Key results from simulation of scenario F17 rate-based model (Plus)

	TCM data	Røsvik (2018)	Fagerheim (2019)		
			IAF=0.55	IAF=0.65	
Removal grade	83.50%	83.80%	83.76%	83.94%	
Rich loading	0.4800	-	0.4845	0.4852	
Ttop [°C]	47.40	47.13	49.38	50.74	
Tmax [°C]	51.70	51.27	51.23	51.37	
Tbtm [°C]	32.40	30.08	30.42	30.32	

# 4.3 Simulation in Aspen HYSYS with estimated E<sub>M</sub>

#### 4.3.1 Simulation of H14 with estimated E<sub>M</sub>

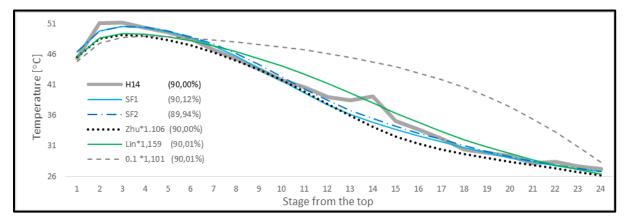


Figure 4.28: Simulated results for scenario H14 with estimated E<sub>M</sub> (HYSYS)

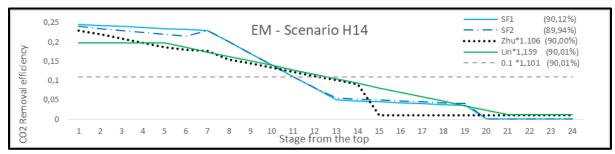


Figure 4.29: Estimated E<sub>M</sub> sets for scenario H14 (HYSYS)

Table 4.28: Key results from simulation of scenario H14 with estimated E<sub>M</sub> (HYSYS)

E <sub>M</sub>	TCM data	SF1	SF2	Zhu*1.106	Lin*1.159	0.1*1.101
Removal grade	90.00%	90.12%	.12% 89.94%		90.01%	90.01%
Rich loading	0.4800	0.4936	0.4931	0.4932	0.4933	0.4932
Ttop [°C]	45.4	46.4	46.4	45.6	45.5	44.8
Tmax [°C]	51.2	50.6	50.6	49.2	49.4	48.9
Tbtm [°C]	27.2	26.7	26.8	26.1	26.3	28.3

Figure 4.28 illustrates the results from the simulation with the new estimated  $E_{M}$ -profiles compared with some of the  $E_{M}$ -profiles used in earlier theses, scaled to give requested removal grade.

Figure 4.29 shows the slope of the  $E_M$ -profiles, which illustrates that  $E_M$ =SF1, have highest efficiency at the top of the packing section, with a soft decreasing slope (-0.002) from stage 1-7. Continued with a steeper decreasing slope (-0.025) from stage 7-13, again followed by a soft decreasing slope (0.002) from stage 13-19 before the efficiency remains constant at 0.0001 for step stages 20-24.  $E_M$ =SF2, have a curve similar to  $E_M$ =SF1, except from stage 1-6, which have a decreasing slope twice as steep (-0.004), followed by an increase (+0.015) from 6-7. From stage 7-24 the curve follows  $E_M$ =SF1, except from stage 13-19, where the slope is the same as for SF1, but the efficiencies are lower.

#### 4.3.2 Simulation of 2B5 with estimated E<sub>M</sub>

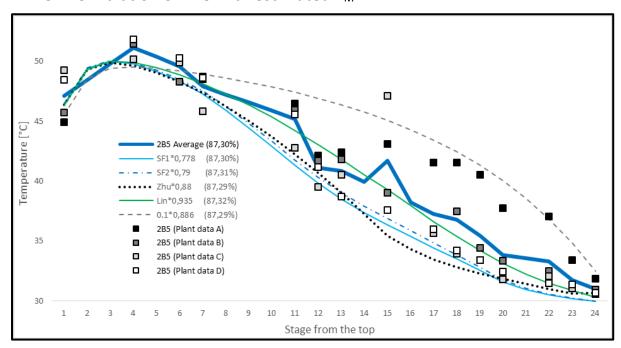


Figure 4.30: Simulated results for scenario 2B5 with downscaled estimated E<sub>M</sub> for H14 (HYSYS)

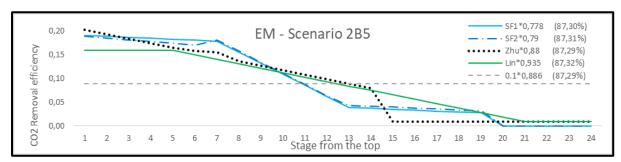


Figure 4.31: Estimated E<sub>M</sub> sets for scenario 2B5 (HYSYS)

Table 4.29: Key results from simulation of scenario 2B5 with estimated E<sub>M</sub> (HYSYS)

E <sub>M</sub>	TCM data	SF1*0.778	SF2*0.79	Zhu*0.88	Lin*0.935	0.1*0.886
Removal grade	87.30%	87.30%	87.31%	87.29%	87.32%	87.29%
Rich loading	0.5000	0.4635	0.4635	0.4634	0.4635	0.4634
Ttop [°C]	47.09	46.44	46.45	46.36	46.31	45.55
Tmax [°C]	51.47	50.02	50.05	49.88	50.01	49.54
Tbtm [°C]	30.99	29.96	29.97	30.67	30.32	32.51

Figure 4.30 present the results from simulation of scenario 2B5, with all the different  $E_{M-}$  profiles scaled down to produce simulations with removal grade close to 87.3%. Scenario 2B5 have four sets of measurement, the individual measurements are given as points in the graph while the thick blue line illustrates the average values of these measurements.

Figure 4.31 illustrates the slopes of the scaled  $E_{M}$ -profiles, which is equal to Scenario H14, but the values are lower.

#### 4.3.3 Simulation of 6w with estimated E<sub>M</sub>

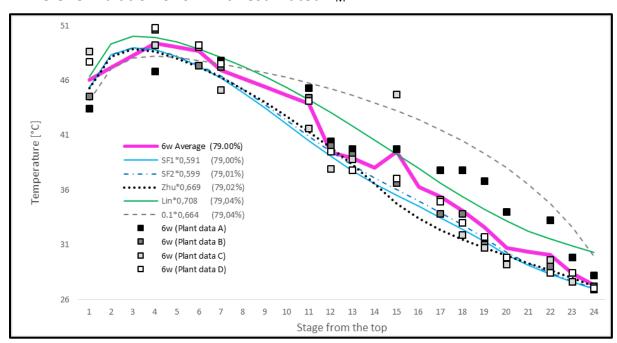


Figure 4.32: Simulated results for scenario 6w with downscaled estimated  $E_M$  for H14 (HYSYS)

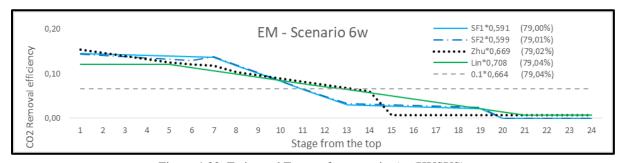


Figure 4.33: Estimated E<sub>M</sub> sets for scenario 6w (HYSYS)

Table 4.30: Key results from simulation of scenario 6w with estimated E<sub>M</sub> (HYSYS)

E <sub>M</sub>	TCM data	SF1*0.591	SF2*0.599	Zhu*0.669	Lin*0.708	0.1*0.664
Removal grade	rade 79.00%		79.01% 79.02%		79.04%	79.04%
Rich loading	0.4600	0.4426	0.4426	0.4426	0.4427	0.4426
Ttop [°C]	46.10	45.34	45.33	45.26	46.31	44.16
Tmax [°C]	49.35	48.99	48.99	48.82	50.01	48.19
Tbtm [°C]	27.33	26.97	27.01	27.21	30.32	29.92

Figure 4.32 presents the results for scenario 6w. Just like for Scenario 2B5, the E<sub>M</sub>-profiles used for scenario H14 have been scaled down to produce simulations with removal grade close to 79.0%. Scenario 6w have four sets of measurement, the individual measurements are given as points in the graph while the thick purple line illustrates the average values of these measurements.

Figure 4.33 illustrates the slopes of the scaled E<sub>M</sub>-profiles, which is equal to Scenario H14 and 2B5, but the values are lower.

#### 4.3.4 Simulation of Goal1 with estimated E<sub>M</sub>

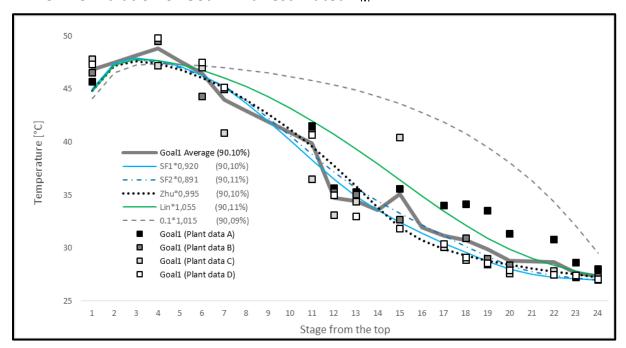


Figure 4.34: Simulated results for scenario Goal1 with downscaled estimated E<sub>M</sub> for H14 (HYSYS)

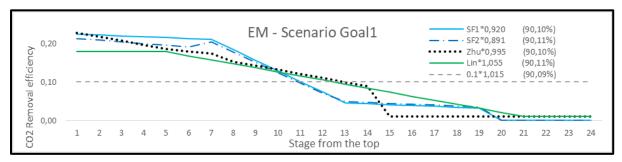


Figure 4.35: Estimated E<sub>M</sub> sets for scenario Goal1 (HYSYS)

Table 4.31: Key results from simulation of scenario Goal1 with estimated E<sub>M</sub> (HYSYS)

E <sub>M</sub>	TCM data	SF1*0.920	SF2*0.891	Zhu*0.995	Lin*1.055	0.1*1.015
Removal grade	90.10%	90.10%	90.11%	90.10%	90.11%	90.09%
Rich loading	0.5000	0.4904	0.4874	0.4873	0.4875	0.4872
Ttop [°C]	46.81	44.98	44.88	44.82	44.78	44.07
Tmax [°C]	48.81	47.89	47.75	47.62	47.78	47.36
Tbtm [°C]	27.31	26.95	26.98	27.20	27.34	29.51

Figure 4.34 presents the result from the simulation of scenario Goal1 with all E<sub>M</sub>-profiles scaled to produce simulations with removal grade close to 90.1 %. Just like for Scenario 2B5 and 6w, scenario goal1 have four sets of measurement, the individual measurements are given as points in the graph while the thick gray line illustrates the average values of these measurements.

Figure 4.35 illustrates the slopes of the scaled  $E_M$ -profiles, here the values are higher than for scenario 2B5 and 6w, which is natural since the removal grade is higher. But the values are lower than for scenario H14, the assumed reason for this is discussed in chapter 5.

#### 4.3.5 Simulation of F17 with estimated E<sub>M</sub>

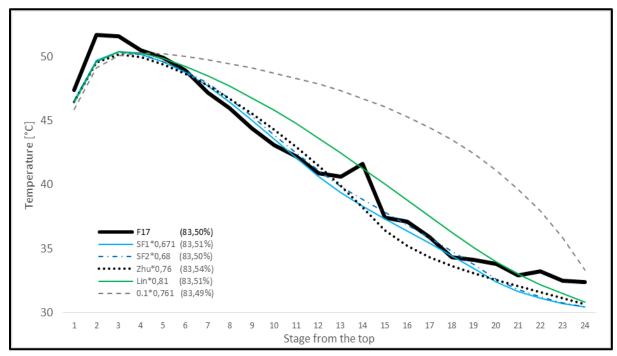


Figure 4.36: Simulated results for scenario F17 with downscaled estimated E<sub>M</sub> for H14 (HYSYS)

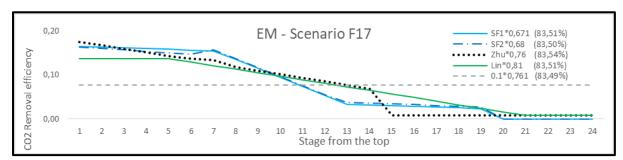


Figure 4.37: Estimated E<sub>M</sub> sets for scenario F17 (HYSYS)

Table 4.32: Key results from simulation of scenario F17 with estimated E<sub>M</sub> (HYSYS)

E <sub>M</sub>	TCM data	SF1*0.671	SF2*0.68	Zhu*0.76	Lin*0.81	0.1*0.761
Removal grade	83.70%	83.51%	83.50%	83.54%	83.51%	83.49%
Rich loading	0.4800	0.4354	0.4353	0.4354	0.4353	0.4353
Ttop [°C]	47.40	46.56	46.54	45.46	46.41	45.88
Tmax [°C]	51.70	50.38	50.35	50.20	50.35	50.28
Tbtm [°C]	32.40	30.42	30.44	30.67	30.82	33.33

Figure 4.36 illustrates the results from the simulations of scenario F17 with all E<sub>M</sub>-profiles scaled down to produce simulations with removal grade close to 83.5 %.

Figure 4.37 shows the slopes of the  $E_{M}$ -profiles, here the values are higher than for scenario 6w and lower than for scenario 2B5, which is natural since the removal grade is in between these two scenarios.

## 4.4 Simulation in Aspen Plus with estimated E<sub>M</sub> and IAF

#### 4.4.1 Simulation of H14 with estimated E<sub>M</sub> and IAF

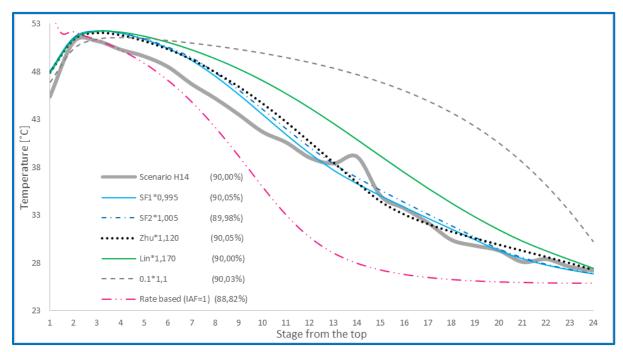


Figure 4.38: Simulated results for scenario H14 with estimated E<sub>M</sub> and IAF (Plus)

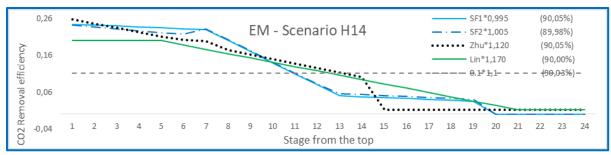


Figure 4.39: Estimated E<sub>M</sub> sets for scenario H14 (Plus)

Table 4.33: Key results from simulation of scenario H14 with estimated E<sub>M</sub> and IAF (Plus)

E <sub>M</sub>		TCM data	SF1*0,995	SF2*1,005	Zhu*1,12	Lin*1,17	0.1*1,1	RB (IAF=1)
Remova	al grade	90.00%	90.05%	89.98%	90.05%	90.00%	90.03%	88.82%
Rich loading		0.4800	0.4929	0.4929	0.4929	0.4928	0.4928	0.4894
Ttop	[°C]	45.40	48.05	48.03	47.91	47.85	46.89	54.40
Tmax	[°C]	51.20	52.27	52.26	52.06	52.21	51.58	54.40
Tbtm	[°C]	27.20	26.86	26.88	27.27	27.44	30.21	25.91

Figure 4.38 illustrates the results from the simulations of scenario H14 with all  $E_M$ -profiles scaled to produce simulations in Aspen Plus equilibrium-based model with removal grade close to 90%. The pink line is simulated in Aspen Plus rate-based model with IAF adjusted to get the removal grade as near 90% as possible.

Figure 4.39 shows the slopes of the Murphree efficiency profiles.

## 4.4.2 Simulation of 2B5 with estimated E<sub>M</sub> and IAF

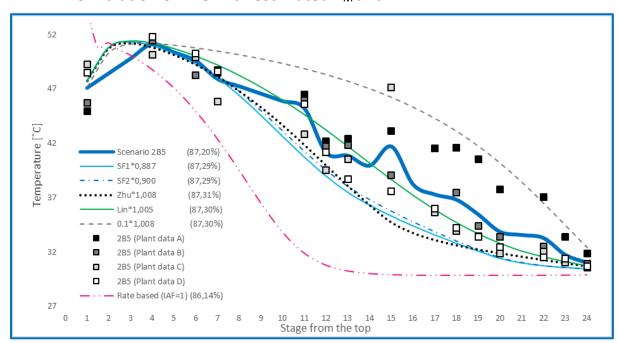


Figure 4.40: Simulated results for scenario 2B5 with estimated E<sub>M</sub> and IAF (Plus)

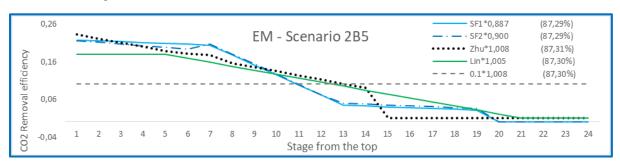


Figure 4.41: Estimated E<sub>M</sub> sets for scenario 2B5 (Plus)

Table 4.34: Key results from simulation of scenario 2B5 with estimated E<sub>M</sub> and IAF (Plus)

E <sub>M</sub>	E <sub>M</sub>		SF1*0.887	SF2*0.900	Zhu*1.008	Lin*1.005	0.1*1.008	RB(IAF=1)
Removal grad	de	87.30%	87.29%	87.29%	87.31%	87.30%	87.30%	86.14%
Rich loading		0.5000	0.4891	0.4891	0.4892	0.4891	0.4891	0.4857
Ttop [°C]		47.09	47.82	47.81	47.75	47.73	47.21	54.26
Tmax [°C]		51.47	51.32	51.33	51.19	51.41	51.19	54.26
Tbtm [°C]		30.99	30.44	30.45	30.66	30.72	32.38	29.87

Figure 4.40 illustrates the results from the simulations of scenario 2B5 with all  $E_M$ -profiles scaled to produce simulations in Aspen Plus equilibrium-based model with removal grade close to 87,20%. The pink line is simulated in Aspen Plus rate-based model with IAF adjusted to get the removal grade as near 87.20% as possible.

Figure 4.41 shows the slopes of the Murphree efficiency profiles.

## 4.4.3 Simulation of 6w with estimated E<sub>M</sub> and IAF

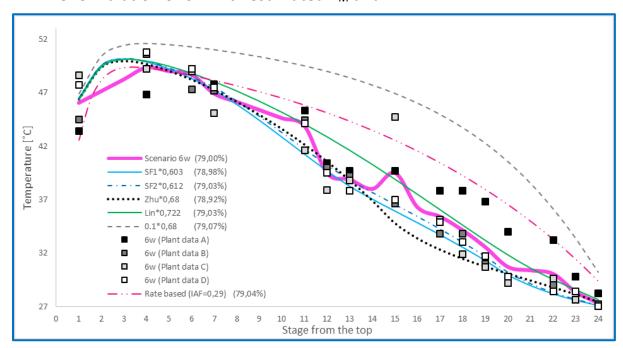


Figure 4.42: Simulated results for scenario 6w with estimated E<sub>M</sub> and IAF (Plus)

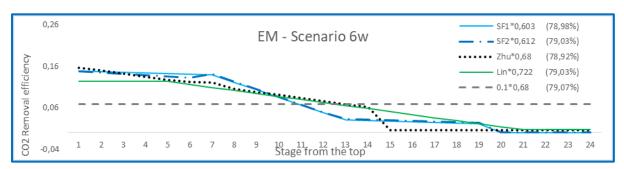


Figure 4.43: Estimated E<sub>M</sub> sets for scenario 6w (Plus)

Table 4.35: Key results from simulation of scenario 6w with estimated E<sub>M</sub> and IAF (Plus)

E <sub>M</sub>		TCM data	SF1*0.603	SF2*0.612	Zhu*0.680	Lin*0.722	0.1*0.680	RB(IAF=0.29)
Remov	al grade	79.00%	78.98%	79.03%	78.92%	79.03%	79.07%	79.04%
Rich loa	ading	0.4600	0.4418	0.4420	0.4413	0.4419	0.4420	0.4870
Ttop	[°C]	46.10	46.49	46.49	46.37	46.31	45.22	42.55
Tmax	[°C]	49.35	50.16	50.17	49.94	50.10	49.25	49.39
Tbtm	[°C]	27.33	27.10	27.13	27.43	27.63	30.53	29.41

Figure 4.42 illustrates the results from the simulations of scenario 6w with all  $E_M$ -profiles scaled to produce simulations in Aspen Plus equilibrium-based model with removal grade close to 79%. The pink line is simulated in Aspen Plus rate-based model with IAF adjusted to get the removal grade as near 79% as possible.

Figure 4.43 shows the slopes of the Murphree efficiency profiles.

## 4.4.4 Simulation of Goal1 with estimated E<sub>M</sub> and IAF

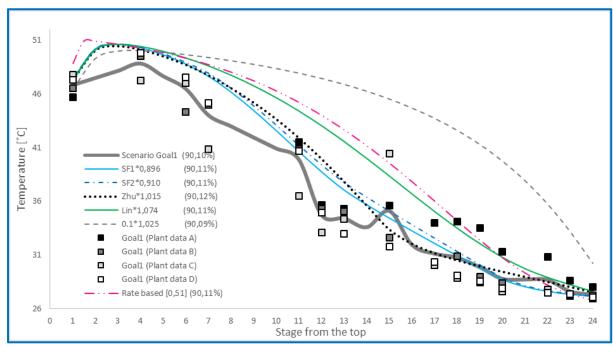


Figure 4.44: Simulated results for scenario Goal1 with estimated E<sub>M</sub> and IAF (Plus)

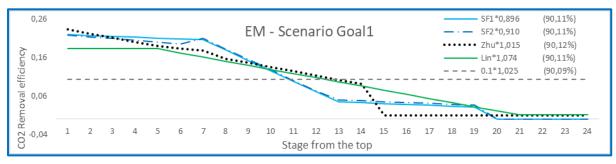


Figure 4.45: Estimated E<sub>M</sub> sets for scenario Goal1 (Plus)

Table 4.36: Key results from simulation of scenario Goal1 with estimated E<sub>M</sub> and IAF (Plus)

E <sub>M</sub>	TCM data	SF1*0.896	SF2*0.910	Zhu*1.015	Lin*1.074	0.1*1.025	RB(IAF=0.51)
Removal grade	90.10%	90.11%	90.11%	90.12%	90.11%	90.09%	90.11%
Rich loading	0.5000	0.4870	0.4870	0.4871	0.4871	0.4869	0.4870
Ttop [°C]	46.81	47.36	47.36	47.26	47.23	46.47	48.83
Tmax [°C]	48.81	50.59	50.59	50.43	50.59	50.04	50.91
Tbtm [°C]	27.31	27.15	27.16	27.52	27.61	30.24	44.73

Figure 4.44 illustrates the results from the simulations of scenario Goal1 with all  $E_M$ -profiles scaled to produce simulations in Aspen Plus equilibrium-based model with removal grade close to 90.1%. The pink line is simulated in Aspen Plus rate-based model with IAF adjusted to get the removal grade as near 90.1% as possible.

Figure 4.45 shows the slopes of the Murphree efficiency profiles.

## 4.4.5 Simulation of F17 with estimated E<sub>M</sub> and IAF

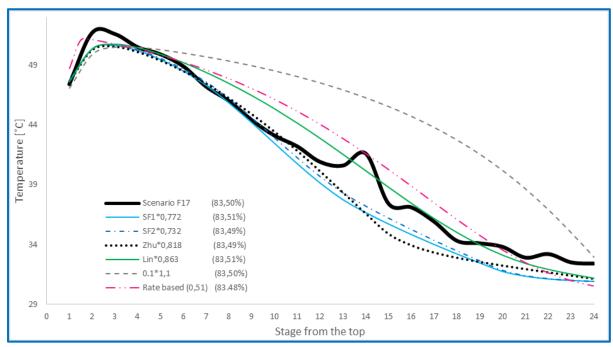


Figure 4.46: Simulated results for scenario F17 with estimated E<sub>M</sub> and IAF (Plus)

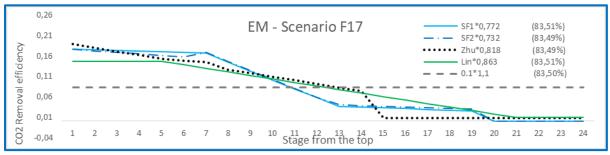


Figure 4.47: Estimated E<sub>M</sub> sets for scenario F17 (Plus)

Table 4.37: Key results from simulation of scenario F17 with estimated E<sub>M</sub> and IAF (Plus)

E <sub>M</sub>		TCM data	SF1*0.772	SF2*0.732	Zhu*0.818	Lin*0.863	0.1*1.1	RB(IAF=0.51)
Removal	grade	83.70%	83.51%	83.49%	83.49%	83.51%	83.50%	83.48%
Rich load	ing	0.4800	0.4837	0.4836	0.4836	0.4837	0.4836	0.4836
Ttop	[°C]	47.40	47.67	47.68	47.61	47.59	47.59	48.72
Tmax	[°C]	51.70	50.64	50.66	50.51	50.74	50.74	51.12
Tbtm	[°C]	32.40	30.91	30.91	31.14	31.18	31.18	44.73

Figure 4.46 illustrates the results from the simulations of scenario F17 with all  $E_M$ -profiles scaled to produce simulations in Aspen Plus equilibrium-based model with removal grade close to 83.5%. The pink line is simulated in Aspen Plus rate-based model with IAF adjusted to get the removal grade as near 83.5% as possible.

Figure 4.47 shows the slopes of the Murphree efficiency profiles.

## 4.5 Comparison of Rate-based and Equilibrium-based model

## 4.5.1 Comparison of Rate-based and Equilibrium for Scenario H14

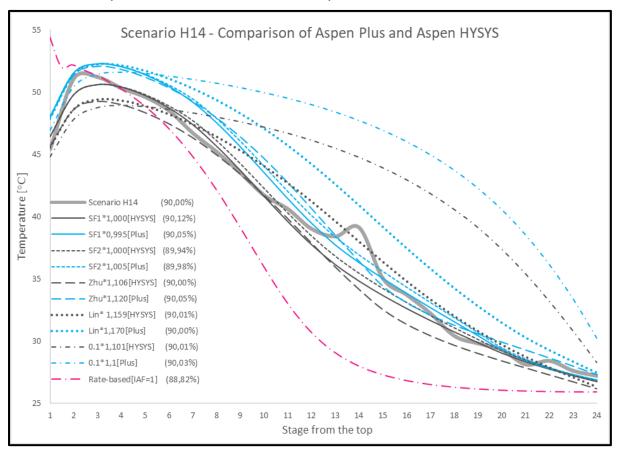


Figure 4.48: Comparison of Rate-based and Equilibrium for Scenario H14

Table 4.38: Key results from comparison of Rate-based and Equilibrium for Scenario H14

	Comparison HYSYS and Plus - Scenario H14											
	TCM Data	SI	-1	SI	F2	ZI	าน	Li	in	0	.1	Rate-based
		HYSYS	Plus	Plus								
EM-Factor	Scenario H14	1.000	0.995	1.000	1.005	1.106	1.120	1.159	1.170	1.101	1.100	IAF = 1
Removal grade	90.00%	90.12	90.05	89.94	89.98	90.00	90.05	90.01	90.00	90.01	90.03	88.82
Rich loading	0.4800	0.4936	0.4929	0.4931	0.4929	0.4932	0.4929	0.4933	0.4928	0.4932	0.4928	0.4894
Ttop	45.40	46.43	48.05	46.41	48.03	45.59	47.91	45.53	47.85	44.79	46.90	54.40
Tmax	51.20	50.59	51.56	50.58	51.54	48.58	52.06	48.60	52.21	48.93	51.58	54.40
Tbtm	27.20	26.73	26.86	26.76	26.88	26.14	27.27	26.31	27.44	28.29	30.21	24.73

Figure 4.48 presents the simulated temperature results of scenario H14 from sub-chapter 4.3.1 and 4.4.1. The thick gray line illustrates the performance temperature profile. The thin gray lines are simulated in equilibrium-based model in Aspen HYSYS, thin blue lines are simulated in equilibrium-based model in Aspen Plus and the pink line is simulated in rate-based model in Aspen Plus. Table 4.38 provides the key results from the simulation of scenario H14 in Aspen plus and Aspen HYSYS compared with performance data.

## 4.5.2 Comparison of Rate-based and Equilibrium-based for Scenario 2B5

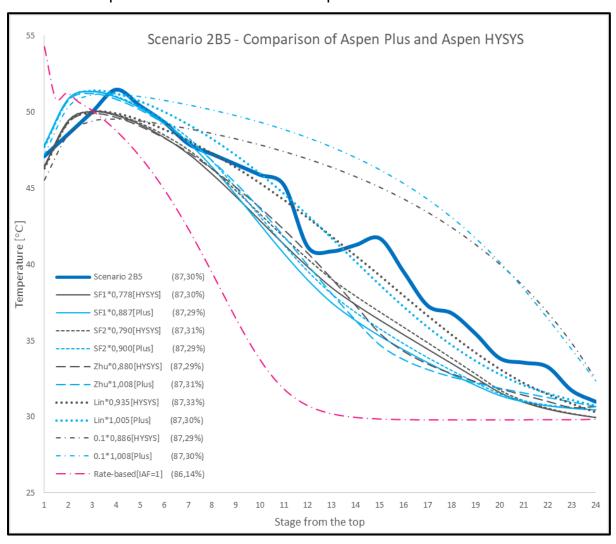


Figure 4.49: Comparison of Rate-based and Equilibrium for Scenario 2B5

Table 4.39: Key results from comparison of Rate-based and Equilibrium for Scenario 2B5

	Comparison HYSYS and Plus - Scenario 2B5													
	T014 D .	SI	F1	SI	F2	Zł	nu	Li	in	0.	.1	Rate-based		
	TCM Data Scenario	HYSYS	Plus	Plus										
EM-Factor	2B5	0.778	0.887	0.790	0.900	0.880	1.008	0.935	1.005	0.886	1.008	IAF = 1		
Removal grade	87.30%	87.30	87.29	87.31	87.29	87.29	87.31	87.32	87.30	87.29	87.30	86.14		
Rich loading	0.5000	0.4635	0.4891	0.4635	0.4891	0.4534	0.4892	0.4635	0.4891	0.4634	0.4891	0.4857		
Ttop	47.09	46.44	47.82	46.45	47.81	46.36	47.75	46.31	47.37	45.55	47.21	54.27		
Tmax	51.47	50.02	51.33	50.05	51.34	49.88	51.20	50.02	51.41	49.41	51.19	51.25		
Tbtm	30.99	29.96	30.44	29.97	30.45	30.67	30.66	30.32	30.72	32.51	32.38	29.87		

Figure 4.49 presents the simulated temperature results of scenario 2B5 from sub-chapter 4.3.2 and 4.4.2.

Table 4.39 provides the key results from the simulation of scenario 2B5 in Aspen plus and Aspen HYSYS compared with performance data.

## 4.5.3 Comparison of Rate-based and Equilibrium-based for Scenario 6w

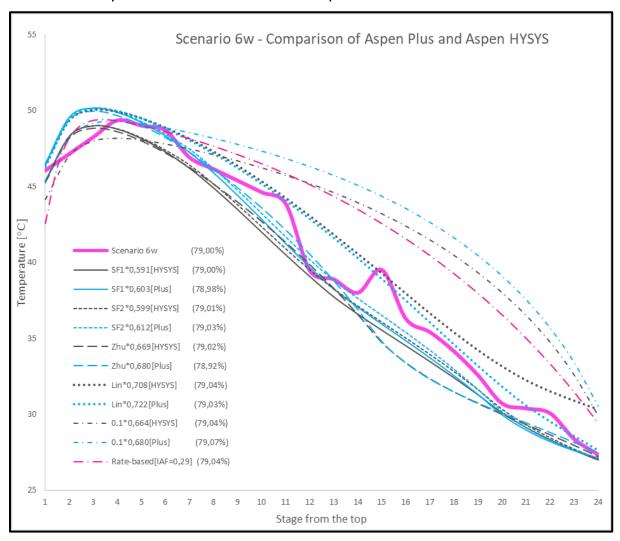


Figure 4.50: Comparison of Rate-based and Equilibrium for Scenario 6w

Table 4.40: Key results from comparison of Rate-based and Equilibrium for Scenario 6w

	Comparison HYSYS and Plus - Scenario 6w													
		SI	SF1		SF2		Zhu		in	0	.1	Rate-based		
	TCM Data Scenario	HYSYS	Plus	Plus										
EM-Factor	6w	0.591	0.603	0.599	0.612	0.669	0.680	0.708	0.722	0.664	0.680	IAF = 0.29		
Removal grade	79.00%	79.00	78.98	79.01	79.03	79.02	78.92	79.04	79.03	79.04	79.07	79.04		
Rich loading	0.4600	0.4426	0.4418	0.4426	0.4420	0.4426	0.4413	0.4427	0.4419	0.4426	0.4420	0.4870		
Ttop	46.10	45.34	47.00	45.33	46.49	45.25	46.36	46.31	46.30	44.16	45.22	42.55		
Tmax	49.35	48.99	50.16	48.99	50.16	48.82	49.94	50.02	50.10	48.19	49.26	49.39		
Tbtm	27.33	26.98	27.10	27.01	27.13	27.21	27.43	30.32	27.64	29.92	30.53	29.41		

Figure 4.50 presents the simulated temperature results of scenario 6w from sub-chapter 4.3.3 and 4.4.3.

Table 4.40 provides the key results from the simulation of scenario 6w in Aspen plus and Aspen HYSYS compared with performance data.

## 4.5.4 Comparison of Rate-based and Equilibrium-based for Scenario Goal1

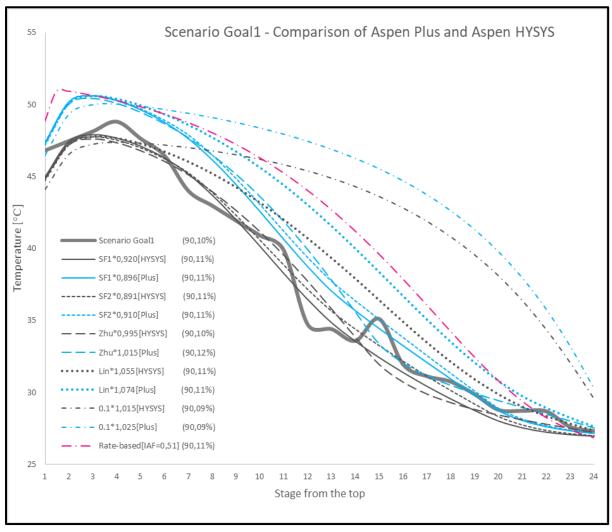


Figure 4.51: Comparison of Rate-based and Equilibrium for Scenario Goal1

Table 4.41: Key results from comparison of Rate-based and Equilibrium for Scenario Goal1

	Comparison HYSYS and Plus - Scenario Goal1														
		SI	F1	SI	-2	ZI	าน	L	in	0	.1	Rate-based			
	TCM Data Scenario	HYSYS	Plus	Plus											
EM-Factor	Goal1	0.920	0.896	0.891	0.910	0.995	1.015	1.055	1.074	1.015	1.025	IAF = 0.51			
Removal grade	90.10%	90.10	90.11	90.11	90.11	90.10	90.12	90.11	90.11	90.09	90.09	90.11			
Rich loading	0.5000	0.4904	0.4870	0.4874	0.4870	0.4873	0.4871	0.4875	0.4871	0.4872	0.4869	0.4870			
Ttop	46.81	46.44	47.82	46.45	47.81	46.36	47.75	46.31	47.73	45.55	47.21	54.27			
Tmax	48.81	50.02	51.33	50.05	51.34	49.88	51.20	50.02	51.41	49.41	51.19	51.25			
Tbtm	27.31	29.96	30.44	29.97	30.45	30.67	30.66	30.32	30.72	32.51	32.38	29,87			

Figure 4.51 presents the simulated temperature results of scenario Goal1 from sub-chapter 4.3.4 and 4.4.4.

Table 4.41 provides the key results from the simulation of scenario Goal1 in Aspen plus and Aspen HYSYS compared with performance data.

## 4.5.5 Comparison of Rate-based and Equilibrium-based for Scenario F17

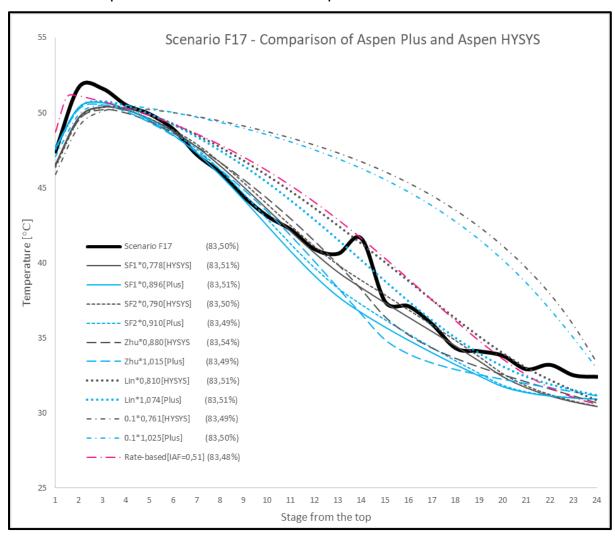


Figure 4.52: Comparison of Rate-based and Equilibrium for Scenario F17

Table 4.42: Key results from comparison of Rate-based and Equilibrium for Scenario F17

	Comparison HYSYS and Plus - Scenario F17													
		SI	F1	SI	F2	ZI	ıu	Li	in	0.	.1	Rate-based		
	TCM Data	HYSYS	Plus	Plus										
EM-Factor	Scenario F17	0.920	0.896	0.891	0.910	0.995	1.015	1.055	1.074	1.015	1.025	IAF = 0.51		
Removal grade	83.50%	83.51	83.51	83.50	83.49	83.54	83.49	83.51	83.51	83.49	83.50	83.48		
Rich loading	0.4800	0.4354	0.4837	0.4353	0.4836	0.4354	0.4836	0.4353	0.4837	0.4353	0.4836	0.4836		
Ttop	47.40	46.56	47.67	46.54	47.67	46.46	47.60	46.41	47.59	45.88	47.08	48.72		
Tmax	51.70	50.38	50.65	50.35	50.66	50.20	50.51	50.36	50.74	50.29	50.50	51.13		
Tbtm	32.40	30.42	30.91	30.44	30.91	30.67	31.13	30.82	31.18	33.33	32.95	30.55		

Figure 4.52 presents the simulated temperature results of scenario F17 from sub-chapter 4.3.5 and 4.4.5.

Table 4.42 provides the key results from the simulation of scenario F17 in Aspen plus and Aspen HYSYS compared with performance data.

## 4.6 Simulation with default E<sub>M</sub> in Aspen HYSYS

#### 4.6.1 Default VS Estimated E<sub>M</sub> for scenario H14

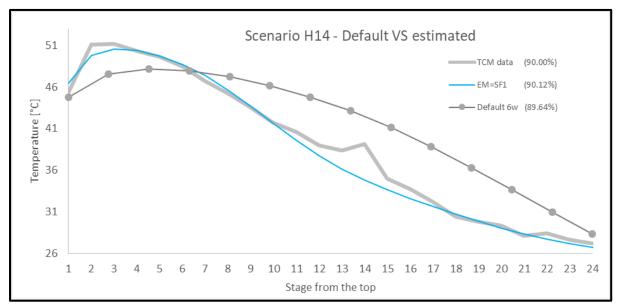


Figure 4.53: Simulated results for scenario H14 with default E<sub>M</sub>

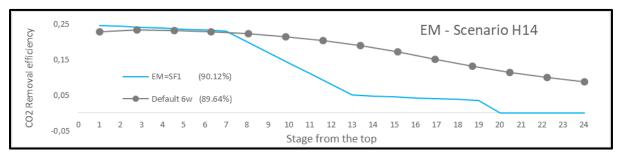


Figure 4.54: Estimated E<sub>M</sub>=SF1 VS default E<sub>M</sub> for scenario H14

Table 4.43: Key results from simulation of scenario H14 with estimated E<sub>M</sub>

Em	TCM data	SF1	Default 6w
Removal grade	90.00%	90.12%	89.64%
Rich loading	0.4800	0.4936	0.4921
Ttop [°C]	45.4	46.4	44.74
Tmax [°C]	51.2	50.6	48.19
Tbtm [°C]	27.2	26.7	28.33

Figure 4.53 illustrates the temperature profile of the simulation of scenario H14 with a default Murphree efficiency profile compared with performance data and simulation with estimated E<sub>M</sub>=SF1. The pointed line illustrates the default temperature profile, the simulation produced the removal grade closest to performance data with 14 stages, the 14 points on the line is the simulated measurements.

Figure 4.54 illustrates the slopes of the default Murphree efficiency profile compared with the slope of  $E_M$ =SF1. Table 4.43 provides the key results from simulation.

#### 4.6.2 Default VS Estimated E<sub>M</sub> for scenario 2B5

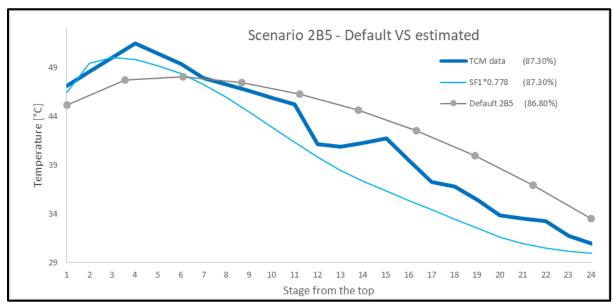


Figure 4.55: Simulated results for scenario 2B5 with default E<sub>M</sub>

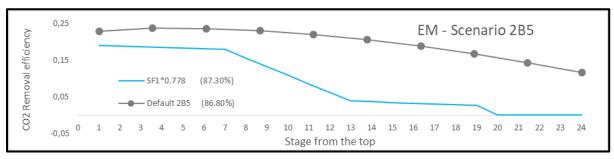


Figure 4.56: Estimated E<sub>M</sub>=SF1 VS default E<sub>M</sub> for scenario 2B5

Table 4.44: Key results from simulation of scenario 2B5 with estimated  $E_{\text{M}}$ 

E <sub>M</sub>	TCM data	SF1*0.778	Default 2B5
Removal grade	87.30%	87.30%	86.80%
Rich loading	0.5000	0.4635	0.4619
Ttop [°C]	47.09	46.44	45.12
Tmax [°C]	51.47	50.02	48.05
Tbtm [°C]	30.99	29.96	33.53

Figure 4.55 illustrates the temperature profile of the simulation of scenario 2B5 with default Murphree efficiencies compared with performance data and simulation with estimated  $E_M=SF1*0.778$ . The pointed line illustrates the default temperature profile, the simulation produced the removal grade closest to performance data with 10 stages, the 10 points on the line is the simulated measurements.

Figure 4.56 illustrates the slopes of the default Murphree efficiency profile compared with the slope of  $E_M$ =SF1\*0.778. Table 4.44 provides the key results from simulation.

#### 4.6.3 Default VS Estimated E<sub>M</sub> for scenario 6w

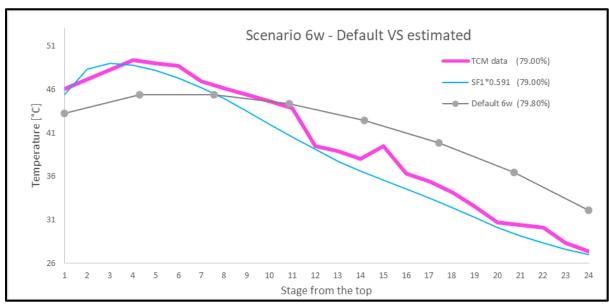


Figure 4.57: Simulated results for scenario 6w with default E<sub>M</sub>

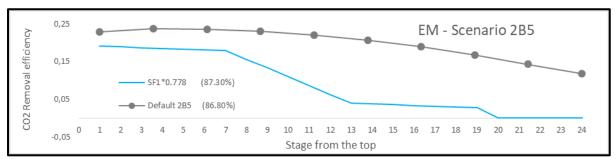


Figure 4.58: Estimated E<sub>M</sub>=SF1 VS default E<sub>M</sub> for scenario 6w

Table 4.45: Key results from simulation of scenario 6w with estimated  $E_M$ 

Ем	TCM data	SF1*0.591	Default 6w
Removal grade	79.00%	79.00%	79.80%
Rich loading	0.4600	0.4426	0.4446
Ttop [°C]	46.10	45.34	43.26
Tmax [°C]	49.35	48.99	45.40
Tbtm [°C]	27.33	26.97	32.11

Figure 4.57 illustrates the temperature profile of the simulation of scenario 6w with a default Murphree efficiency profile compared with performance data and simulation with estimated  $E_M=SF1*0.591$ . The pointed line illustrates the default temperature profile, the simulation produced the removal grade closest to performance data with 8 stages, the 8 points on the line is the simulated measurements.

Figure 4.45 illustrates the slopes of the default Murphree efficiency profile compared with the slope of  $E_M=SF1*0.591$ . Table 4.45 provides the key results from simulation.

#### 4.6.4 Default VS Estimated E<sub>M</sub> for scenario Goal1

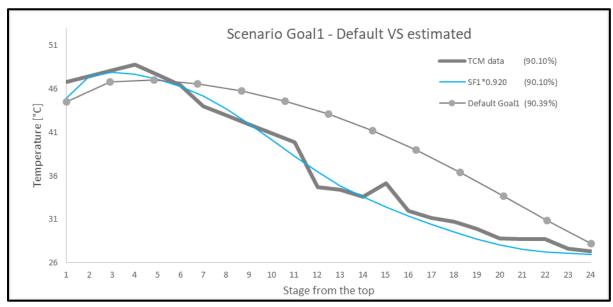


Figure 4.59: Simulated results for scenario Goal1 with default E<sub>M</sub>

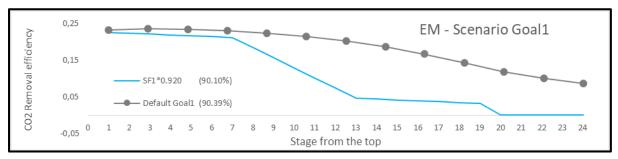


Figure 4.60: Estimated E<sub>M</sub>=SF1 VS default E<sub>M</sub> for scenario Goal1

Table 4.46: Key results from simulation of scenario Goal1 with estimated  $E_{\text{M}}$ 

E <sub>M</sub>	TCM data	SF1*0.920	Default Goal1
Removal grade	90.10%	90.10%	90.39%
Rich loading	0.5000	0.4904	0.4883
Ttop [°C]	46.81	44.98	44.53
Tmax [°C]	48.81	47.89	47.06
Tbtm [°C]	27.31	26.95	28.20

Figure 4.59 illustrates the temperature profile of the simulation of scenario Goal1 with default Murphree efficiency profile compared with performance data and simulation with estimated  $E_M=SF1*0.920$ . The pointed line illustrates the default temperature profile, the simulation produced the removal grade closest to performance data with 13 stages, the 13 points on the line is the simulated measurements.

Figure 4.60 illustrates the slopes of the default Murphree efficiency profile compared with the slope of  $E_M=SF*0.920$ . Table 4.46 provides the key results from simulation.

#### 4.6.5 Default VS Estimated E<sub>M</sub> for scenario F17

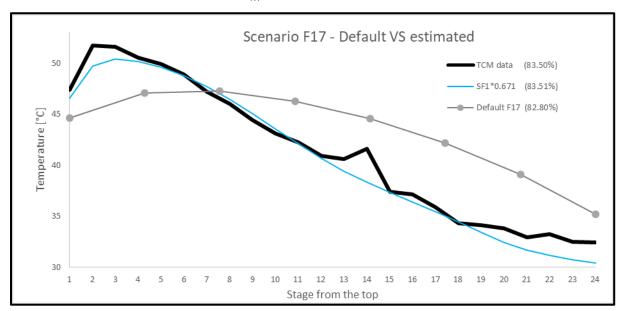


Figure 4.61: Simulated results for scenario F17 with default E<sub>M</sub>

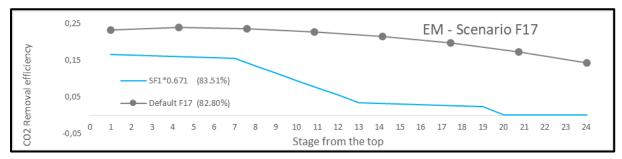


Figure 4.62: Estimated E<sub>M</sub>=SF1 VS default E<sub>M</sub> for scenario F17

Table 4.47: Key results from simulation of scenario F17 with estimated  $E_M$ 

E <sub>M</sub>	TCM data	SF1*0.671	Default F17
Removal grade	83.50%	83.51%	82.80%
Rich loading	0.4800	0.4354	0.4332
Ttop [°C]	47.4	46.56	44.63
Tmax [°C]	51.7	50.38	47.24
Tbtm [°C]	32.4	30.42	35.15

Figure 4.61 illustrates the temperature profile of the simulation of scenario F17 with default Murphree efficiency profiles compared with performance data and simulation with estimated  $E_M=SF1*0.671$ . The pointed line illustrates the default temperature profile, the simulation produced the removal grade closest to performance data with 8 stages, the 8 points on the line is the simulated measurements.

Figure 4.62 illustrates the slopes of the default Murphree efficiency profile compared with the slope of  $E_M=SF1*0.671$ . Table 4.47 provides the key results from simulation.

# 4.7 Comparison of Amine package in Aspen HYSYS

## 4.7.1 Comparison of amine packages for scenario H14

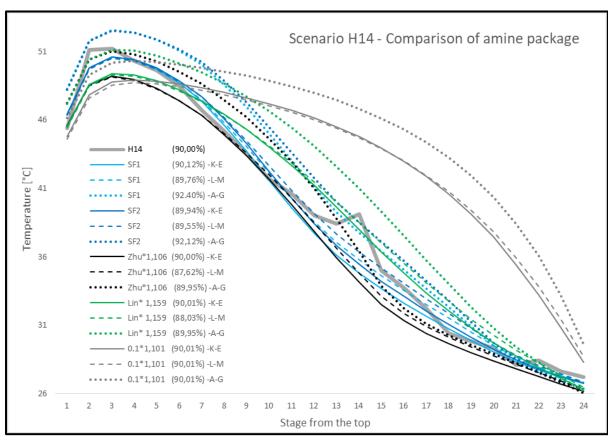


Figure 4.63: Comparison of Amine fluid packages for Scenario H14

Table 4.48: Comparison of key results from simulation with different amine packages for scenario H14

	Comparison of amine Packages in Aspen HYSYS											
Scenario H14			Zhu*1,106	5		Lin*1,159		0.1*1,101				
		K-E	L-M	A-G	K-E	L-M	A-G	K-E	L-M	A-G		
Capture rate	[%]	90.00	89.64	92.14	90.01	89.63	91.85	90.01	89.87	91.92		
Rich loading		0.4932	0.4922	0.4986	0.4933	0.4922	0.4977	0.4932	0.4928	0.4980		
Ttop	[°C]	45.59	45.52	47.24	45.53	45.45	47.19	44.79	44.62	46.14		
Tmax	[°C]	49.21	49.13	51.00	49.37	49.27	51.14	48.93	48.73	50.33		
Tbtm	[°C]	26.14	26.25	26.02	26.31	26.44	26.17	28.29	28.69	29.57		
			SF1			SF2						
		K-E	L-M	A-G	K-E	L-M	A-G					
Capture rate	[%]	90.12	89.76	92.40	89.94	89.55	92.12					
Rich loading		0.4936	0.4925	0.4994	0.4931	0.4919	0.4986					
Ttop	[°C]	46.43	46.38	48.25	46.41	46.34	48.22					
Tmax	[°C]	50.59	50.52	52.55	50.58	50.49	52.52					
Tbtm	[°C]	26.73	26.80	26.35	26.76	26.83	26.37					

Figure 4.63 illustrates the temperature profile of the Scenario H14 simulated with all five  $E_{M}$ -profiles in three different amine-packages. Table 4.48 provides the key results from simulation.

## 4.7.2 Comparison of amine packages for scenario 2B5

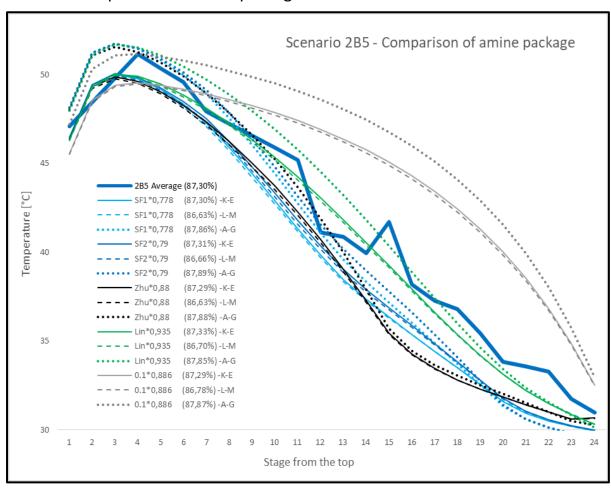


Figure 4.64: Comparison of Amine fluid packages for Scenario 2B5

Table 4.49: Comparison of key results from simulation with different amine packages for scenario 2B5

	Comparison of amine Packages in Aspen HYSYS for scenario 2B5											
			Zhu*0.88			Lin*0.935		0.1*0,886				
		K-E	L-M	A-G	K-E	L-M	A-G	K-E	L-M	A-G		
Capture rate	[%]	87.29	86.63	87.88	87.32	86.70	87.85	87.29	86.78	87.87		
Rich loading		0.4634	0.4615	0.4643	0.4635	0.4616	0.4644	0.4634	0.4618	0.4643		
Ttop	[°C]	46.36	46.31	48.02	46.31	46.27	47.96	45.55	45.50	47.20		
Tmax	[°C]	49.88	49.78	51.56	50.02	49.95	51.69	49.53	49.46	51.16		
Tbtm	[°C]	30.67	30.66	30.27	30.32	30.32	30.15	32.51	32.48	32.93		
		;	SF1*0,778	3		SF1*0,79						
		K-E	L-M	A-G	K-E	L-M	A-G					
Capture rate	[%]	87.30	86.63	87.86	87.31	86.66	87.89					
Rich loading		0.4635	0.4615	0.4643	0.4635	0.4615	0.4644					
Ttop	[°C]	46.44	46.39	48.13	46.45	46.39	48.14					
Tmax	[°C]	50.02	49.93	51.74	50.05	49.94	51.76					
Tbtm	[°C]	29.96	29.97	29.60	29.97	29.97	29.60					

Figure 4.64 illustrates the temperature profile of the Scenario 2B5 simulated with all five  $E_{M-}$  profiles in three different amine-packages. Table 4.49 provides the key results from simulation.

## 4.7.3 Comparison of amine packages for scenario 6w

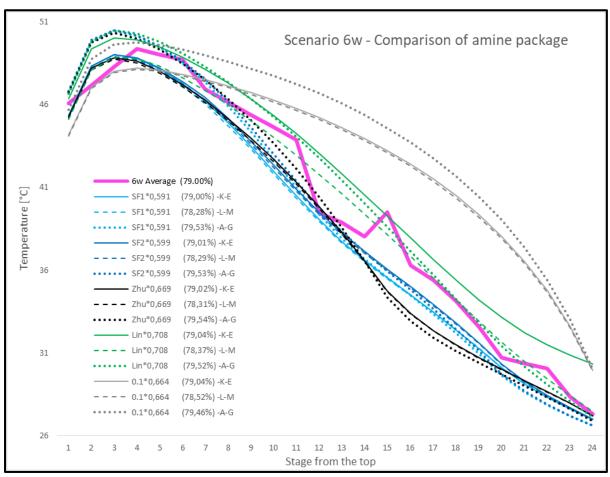


Figure 4.65: Comparison of Amine fluid packages for Scenario 6w

Table 4.50: Comparison of key results from simulation with different amine packages for scenario 6w

	Comparison of amine Packages in Aspen HYSYS for scenario 6w											
			Zhu*0.669	)		Lin*0.708	}		0.1*0,664			
		K-E	L-M	A-G	K-E	L-M	A-G	K-E	L-M	A-G		
Capture rate	[%]	79.02	78.31	79.54	79.04	78.37	79.52	79.04	78.52	79.46		
Rich loading		0.4426	0.4407	0.4433	0.4427	0.4408	0.4433	0.4426	0.4412	0.4431		
Ttop	[°C]	45.26	45.19	46.72	46.31	45.09	46.65	44.16	44.10	45.66		
Tmax	[°C]	48.82	48.71	50.30	50.01	48.84	50.45	48.18	48.11	49.74		
Tbtm	[°C]	27.21	27.20	26.89	30.32	27.44	27.11	29.91	29.88	30.03		
			SF1*0,591	L		SF1*0,599	)					
		K-E	L-M	A-G	K-E	L-M	A-G					
Capture rate	[%]	79.00	78.28	79.53	79.01	78.29	79.53					
Rich loading		0.4426	0.4406	0.4433	0.4426	0.4406	0.4433					
Ttop	[°C]	45.34	46.39	48.13	45.33	46.39	46.80					
Tmax	[°C]	48.99	49.93	51.74	48.99	48.88	50.45					
Tbtm	[°C]	26.98	29.97	29.60	27.01	27.01	26.63					

Figure 4.65 illustrates the temperature profile of the Scenario 6w simulated with all five  $E_{M-}$  profiles in three different amine-packages. Table 4.50 provides the key results from simulation.

#### 4.7.4 Comparison of amine packages for scenario Goal1

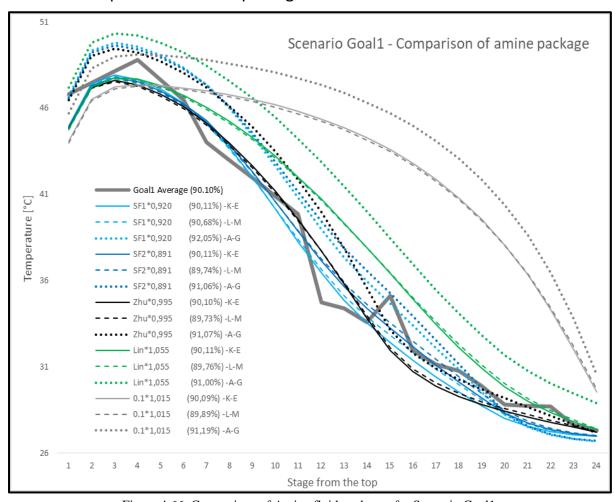


Figure 4.66: Comparison of Amine fluid packages for Scenario Goal1

Table 4.51: Comparison of key results from simulation with different amine packages for scenario Goal1

Comparison of amine Packages in Aspen HYSYS for scenario Goal1										
	Zhu*0.995 Lin*1.055							0.1*0.01015		
		K-E	L-M	A-G	K-E	L-M	A-G	K-E	L-M	A-G
Capture rate	[%]	90.10	89.73	91.07	90.11	89.76	91.00	90.09	89.89	91.19
Rich loading		0.4873	0.4861	0.4896	0.4875	0.4862	0.4894	0.4872	0.4865	0.4900
Ttop	[°C]	44.82	44.77	46.47	44.78	44.73	47.19	44.07	44.00	45.70
Tmax	[°C]	47.62	47.54	49.45	47.78	47.71	50.33	47.36	47.12	49.11
Tbtm	[°C]	27.20	27.24	27.14	27.34	27.39	28.90	29.51	29.68	30.53
			SF1*0.920	)	SF2*0.891					
		K-E	L-M	A-G	K-E	L-M	A-G			
Capture rate	[%]	90.10	90.68	92.05	90.11	89.74	91.06			
Rich loading		0.4904	0.4893	0.4929	0.4874	0.4861	0.4896			
Ttop	[°C]	44.98	44.94	46.69	44.88	44.85	46.60			
Tmax	[°C]	47.90	47.83	49.78	47.75	47.71	49.64			
Tbtm	[°C]	26.95	26.98	26.68	26.98	26.99	26.69			

Figure 4.66 illustrates the temperature profile of the Scenario Goal1 simulated with all five  $E_{M-}$  profiles in three different amine-packages. Table 4.51 provides the key results from simulation.

#### 4.7.5 Comparison of amine packages for scenario F17

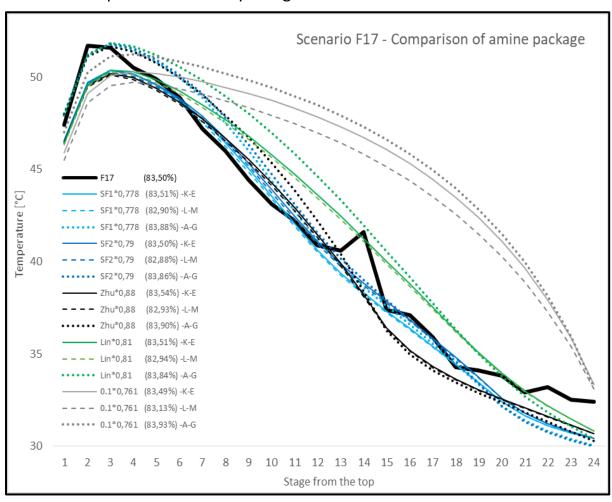


Figure 4.67: Comparison of Amine fluid packages for Scenario F17

Table 4.52: Comparison of key results from simulation with different amine packages for scenario F17

Comparison of amine Packages in Aspen HYSYS for scenario F17										
			Zhu*0,88			Lin*0,81			0.1*0,761	
		K-E	L-M	A-G	K-E	L-M	A-G	K-E	L-M	A-G
Capture rate	[%]	83.54	82.93	83.90	83.51	82.94	83.84	83.49	83.13	83.93
Rich loading		0.4254	0.4337	0.4357	0.4353	0.4337	0.4355	0.4353	0.4342	0.4357
Ttop	[°C]	46.46	46.40	47.94	46.41	46.34	47.90	45.88	45.49	47.01
Tmax	[°C]	50.20	50.11	51.67	50.36	50.25	51.83	50.29	49.70	52.22
Tbtm	[°C]	30.67	30.66	30.27	30.82	30.81	30.39	33.33	33.08	33.21
			SF1*0,778	3	SF2*0,79					
		K-E	L-M	A-G	K-E	L-M	A-G			
Capture rate	[%]	83.51	82.90	83.88	83.50	82.88	83.86			
Rich loading		0.4354	0.4336	0.4356	0.4353	0.4336	0.4355			
Ttop	[°C]	46.56	46.49	47.99	46.54	46.48	48.03			
Tmax	[°C]	50.17	50.04	51.48	50.35	50.26	51.82			
Tbtm	[°C]	30.42	30.42	30.04	30.44	30.44	29.98			

Figure 4.67 illustrates the temperature profile of the Scenario F17 simulated with all five  $E_{M}$ -profiles in three different amine-packages. Table 4.52 provides the key results from simulation.

# 5 Suggested method for estimating E<sub>M</sub>-factor

From the simulations in sub-chapter 4.3, there is an interest for studying the connections between  $E_{M}$ -factor and performance data, with the interest of finding a method of estimating the  $E_{M}$ -factor for any given scenario.

Scenario	E <sub>M</sub> - Factor for SF1 (E <sub>M</sub> )	Lean Amine flow [kg/h]	Gas inlet flow [Sm3/h]	Ratio [Sm³/ kg]	Amine inlet temp [°C]	Gas inlet temp [°C]	Lean loading	Rich loading	Max temp [°C]	Removal grade (RG%) [%]
H14	1.000	54900	46970	0.86	36.5	25.0	0.2300	0.4800	51.2	90.00
Goal1	0.920	44391	46864	1.06	36.5	25.0	0.2000	0.5000	48.8	90.10
2B5	0.778	49485	46981	0.95	36.8	28.2	0.2000	0.5000	51.1	87.30
F17	0.671	57434	59430	1.03	37.0	29.8	0.2000	0.4800	51.7	83.50
6w	0.591	54915	46602	0.85	36.9	25.0	0.2500	0.4600	49.4	79.00

Table 5.1: Comparison of key performance data from each scenario

Based on the data in table 5.1, it becomes clear that the  $E_M$ -factor decreases almost linearly with the removal grade, with some exceptions. Equation 5.1 was used to create a line with linear interpolation between  $E_M$ -factor for  $E_M$ =SF1 and removal grade for scenario H14 and 6w. This was done to investigate the nonlinearities, since these two scenarios contains similar experimental data.  $E_M$ =SF1 is illustrated by the filled blue rectangles in Figure 5.1.

$$E_{M} - factor = E_{M[0]} + (RG\% - RG\%_{[0]}) \frac{E_{M[1]} - E_{M[0]}}{RG\%_{[1]} - RG\%_{[0]}}$$
(5.1)

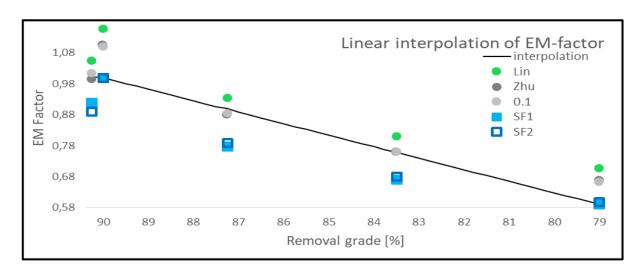


Figure 5.1: Linear interpolation between E<sub>M</sub>-factors

The deviation from the line is calculated for scenario Goal1 (-0.08), 2B5 (-0.12) and F17 (-0.09). From these results one can assume that the ratio of amine and gas impacts the choice of  $E_{M}$ -factor. It is therefore assumed that if the experimental performance data were closer to the data for scenario H14 and 6w, the  $E_{M}$ -factor could be calculated for any removal grade from equation 5.1.

If the key data is deviating from the data in scenario H14 and 6w, the suggested method could be combined with an estimating method e.g. you could calculate the  $E_M$ -factor with equation 5.1 and simulate with the calculated  $E_M$ -factor. If the simulated removal grade is higher than performance removal grade, you could guess a lower value for  $E_M$ -factor and continue with e.g the bisection method until an  $E_M$ -factor which predicts the correct removal grade is found. In the same way you would guess a higher value for  $E_M$ -factor if the simulated removal grade is lower than performance data.

It is assumed that this method will converge to the correct  $E_M$ -factor quicker than the try and fail method suggested in sub-chapter 3.2.2.

## 6 Discussion

In this chapter, the verification simulations in Aspen HYSYS and Aspen Plus are evaluated. The simulations with estimated  $E_M$ -profiles in Aspen HYSYS and estimated  $E_M$ -profiles and interfacial area factor in Aspen Plus are evaluated. The comparison between estimated simulations in Equilibrium-based and rate-based model are evaluated. The simulations with default  $E_M$ -profiles compared with estimated  $E_M$ =SF1 in Aspen HYSYS are evaluated. The comparison of simulation with different amine packages in Aspen HYSYS are evaluated. And at last, a comparison of results from this work and results from earlier work is discussed, before some further work is suggested.

#### 6.1 Evaluation of verification simulation in Aspen HYSYS

#### 6.1.1 Evaluation of scenario H14 verification in Aspen HYSYS

The verification of scenario H14 for Zhu, Sætre and Røsvik was not producing identical temperature profile with any of their results, but a similar temperature profile for both scenario H14 with  $E_M = 0.1$  and  $E_M = Zhu$ . The removal grade for  $E_M = 0.1$  was lower than performance data (-1.58%), lower than Zhu (-0.98%), higher than Sætre (+1.42%) and lower than Røsvik (-0.88%). While the rich loading was higher than performance data (+0.0085), higher than Zhu (+0.0015) and lower than Sætre (-0.0035). The removal grade for  $E_M = Zhu$  was lower than performance data (-1.43%), lower than Zhu (-0.82%), higher than Sætre (+1.67%) and lower than Røsvik (-0.73%). While the rich loading was higher than performance data (+0.0090), higher than Zhu (+0.0010) and lower than Sætre (-0.0020).

Zhu got a higher removal grade and a lower rich loading while Sætre got a lower removal grade and higher rich loading for botm  $E_M$ =0.1 and  $E_M$ =Zhu. The reason for this deviation is assumed to be because Zhu used a lower input flue gas flow than given by Hamborg et al., (2014) [7] for scenario H14. This assumption gets supported when the results are compared to Sætre's verification in his master thesis from 2016 [28], where he verified Zhu with the same input flue gas flow as Zhu and got a removal grade and rich loading almost identical with Zhu.

#### 6.1.2 Evaluation of scenario 2B5 verification in Aspen HYSYS

The verification of Sætre's simulation of 2B5 results in a non-identical but slightly similar temperature profile for both  $E_M$ =0.1 and  $E_M$ =Zhu. The removal grade for  $E_M$ =0.1 was slightly higher than Sætre (+3.07%) and performance data (+2.77%) while the rich loading was lower than Sætre (-0.0200) and performance data (-0.0300). The removal grade for  $E_M$  =Zhu was also slightly higher than Sætre (+3.00%) and performance data (+3%) while the rich loading was lower than Sætre (-0.0200) and performance data (-0.0300).

The reason for these deviations might be caused by uncertainties in measurements, variations in different versions of simulation programs or unknown differences in process input variables to simulation.

#### 6.1.3 Evaluation of scenario 6w verification in Aspen HYSYS

The verification on Sætre's work on scenario 6w also produces a temperature profile similar but not identical to Sætre, for both  $E_M$  =0.1 and  $E_M$  =Zhu. The removal grade for  $E_M$  =0.1 were higher than for Sætre (+2.72%) and performance data (+10.72%) while the rich loading was lower than Sætre (-0.0200) but higher than performance data (+0.0100). The removal grade of  $E_M$  =Zhu was also slightly higher than Sætre (+2.70%) and performance data (+10.60%) while rich loading was lower than for Sætre (-0.0200) and higher than for performance data (+0.0100).

#### 6.1.4 Evaluation of scenario Goal1 verification in Aspen HYSYS

The verification on Sætre's work on scenario Goal1 produces a curve fairly similar to sætre for both  $E_M$ =0.1 and  $E_M$ =Zhu. The removal grade for  $E_M$  =0.1 were higher than for Sætre (+0.94%) but lower than performance data (-3.06%), while the rich loading was a little bit lower than both (-0.0070). For  $E_M$  =Zhu the removal grade was also higher than Sætre (+1.22%) and lower than performance data (-2.68%), while the rich loading was lower than both (-0.0060).

#### 6.1.5 Evaluation of scenario F17 verification in Aspen HYSYS

The verification of Røsvik's simulation of scenario F17, with  $E_M$ =0.1, produced a temperature profile similar to Røsvik, but with slightly higher main temperature. The removal grade deviated from both Røsvik (+5.28%) and performance data (+8.18%). The verification of Røsvik's simulation of scenario F17, with  $E_M$ =Zhu, produced results that deviated a lot from Røsvik, but fitted the temperature profile for the performance data better than Røsvik's simulation. The removal grade on the other hand deviated from both Røsvik (+2.67%) and performance data (+6.87%). The verification of Røsviks simulation of scenario F17 with  $E_M$ =Lin, produced a slightly higher temperature profile, the removal grade had some deviations from Røsvik (+3.60%) and the performance data (+5.50%). The simulated rich loading was slightly lower than the rich loading from performance data for all  $E_M$ -profiles,  $E_M$ =0.1 (-0.1200),  $E_M$ =Zhu (-0.0200),  $E_M$ =Lin (-0.0300).

The reason for the deviations is assumed to be for the reason that Røsvik used a much lower input pressure than given in Faramarzi et al., (2017) [32] for scenario F17. In addition, the E<sub>M</sub>-profiles used in this verification will give a removal grade higher than performance data because they have a too high overall efficiency to be able to fit this scenario well, this we can also see in scenario 6w which also have a lower removal grade.

#### 6.2 Evaluation of verification simulation in Aspen Plus

#### 6.2.1 Evaluation of scenario H14 verification in Aspen Plus

The verification of scenario H14 for Sætre and Røsvik's equilibrium-based Aspen Plus simulation, produced close to identical results for temperature profile for both  $E_M$ =0.1 and  $E_M$ =Zhu. The removal grade for  $E_M$ =0.1 was lower than performance data (-1.60%), higher than Sætre (+1.20%) and equal to Røsvik. While the rich loading was higher than performance data (+0.0080), lower than Sætre (-0.0030). The removal grade for  $E_M$ =Zhu was lower than performance data (-1.61%), higher than Sætre (+1.49%) and lower than Røsvik (-0.61%). While the rich loading was higher than performance data (+0.008) and lower than Sætre (-0.0020).

The rate-based verification of scenario H14 for Sætre and Røsvik, produced close to identical temperature profiles for Sætre, when IAF was set to 0.55, and Røsvik when IAF was set to 0.65. The removal grade for IAF=0.55 was lower than performance data (-1.62%) and lower than Sætre (-0.12%) while the rich loading was higher than performance data (+0.0091) and higher than Sætre (+0.0001). The removal grade for IAF=0.65 was lower than performance data (-1.28%) and lower than Røsvik (-0.38%).

#### 6.2.2 Evaluation of scenario 2B5 verification in Aspen Plus

The verification of scenario 2B5 for Sætre's equilibrium-based Aspen Plus simulation, produced close to identical results for temperature profile for  $E_M$ =0.1, while  $E_M$ =Zhu had some deviations. The removal grade for  $E_M$ =0.1 was lower than performance data (-0.10%) and equal to Sætre. The rich loading was lower than performance data (-0.0113) and lower than Sætre (-0.0013). The removal grade for  $E_M$ =Zhu was higher than performance data (+1.09%), and higher than Sætre (+0.99%). The rich loading was lower than performance data (-0.0120) and lower than Sætre (-0.0020).

The rate-based verification of scenario 2B5 for Sætre, produced close to identical temperature profiles when IAF was set to 0.55. The removal grade for IAF=0.55 was lower than performance data (-1.28%) and higher than Sætre (+0.02%) while the rich loading was higher than performance data (+0.0146) and lower than Sætre (-0.0046).

#### 6.2.3 Evaluation of scenario 6w verification in Aspen Plus

The verification of scenario 6w for Sætre's equilibrium-based Aspen Plus simulation, produced close to identical results for temperature profile for  $E_M$ =0.1, while  $E_M$ =Zhu deviated more.. The removal grade for  $E_M$ =0.1 was higher than performance data (+10.49%) and higher than Sætre (+2.29%). The rich loading was higher than performance data (-0.0107) and lower than Sætre (-0.0203). The removal grade for  $E_M$ =Zhu was higher than performance data (+10.68%), and higher than Sætre (+2.78%). The rich loading was higher than performance data (+0.0102) and lower than Sætre (-0.0198).

The rate-based verification of scenario 6w for Sætre, produced temperature profiles with similar curves as Sætre but higher temperatures, both when IAF was set to 0.55

and 0.65. The removal grade for IAF=0.55 was higher than performance data (-14.53%) and higher than Sætre (+7.43%) while the rich loading was higher than performance data (+0.0219) and lower than Sætre (-0.0061). The removal grade for IAF=0.65 was higher than performance data (-16.19%) and higher than Sætre (+9.09%) while the rich loading was higher than performance data (+0.0265) and lower than Sætre (-0.0015).

The removal grade was closer to Sætre for IAF=0.55, while the rich loading was closer for IAF=0.65, none of them gave a god fit to temperature profile. It is assumed that Sætre used a lower interfacial area factor.

#### 6.2.4 Evaluation of scenario Goal1 verification in Aspen Plus

The verification of scenario Goal1 for Sætre's equilibrium-based Aspen Plus simulation, produced temperature profiles with similar curves as Sætre for both  $E_M$ =0.1, and  $E_M$ =Zhu. The removal grade for  $E_M$ =0.1 was lower than performance data (-0.47%) and higher than Sætre (+6.93%). The rich loading was lower than both performance data and Sætre (-0.0146). The removal grade for  $E_M$ =Zhu was lower than performance data (-0.28%), and higher than Sætre (+7.12%). The rich loading was lower than both performance data and Sætre (-0.0140).

The rate-based verification of scenario Goal1 for Sætre, produced temperature profiles with similar curves as Sætre, but higher temperatures. The removal grade for IAF=0.55 was higher than performance data (+0.11%) and higher than Sætre (+11.31%) while the rich loading was lower than performance data (-0.0123) and lower than Sætre (-0.0020). The removal grade for IAF=0.65 was higher than performance data (+0.30%) and higher than Sætre (+11.50%) while the rich loading was lower than performance data (-0.0120) and lower than Sætre (-0.0020).

The removal grade was closer to Sætre for IAF=0.55, while the rich loading was closer for IAF=0.65, none of them gave a god fit to temperature profile.

#### 6.2.5 Evaluation of scenario F17 verification in Aspen Plus

The verification of scenario F17 for Røsvik's equilibrium-based Aspen Plus simulation, produced similar results for temperature profile for  $E_M$ =0.1, while  $E_M$ =Zhu had some deviations. The temperature profile for  $E_M$ =Lin is close to identical with Røsvik. The removal grade for  $E_M$ =0.1 was higher than performance data (+4.90%) and higher than Sætre (+1.75%). The rich loading was higher than performance data (+0.0080). The removal grade for  $E_M$ =Zhu was higher than performance data (+4.89%), and higher than Sætre (+1.19%). The rich loading was higher than performance data (+0.0080). The removal grade for  $E_M$ =Lin was higher than performance data (+2.74%), and lower than Sætre (-0.06%). The rich loading was higher than performance data (+0.0129).

The rate-based verification of scenario F17 for Røsvik, produced close to identical temperature profiles when IAF was set to 0.55. The removal grade for IAF=0.55 was higher than performance data (+0.26%) and lower than Sætre (-0.04%) while the rich loading was higher than performance data (+0.0450).

#### 6.3 Evaluation of simulation with estimated E<sub>M</sub> in Aspen HYSYS

#### 6.3.1 Evaluation of scenario H14 with estimated E<sub>M</sub> in Aspen HYSYS

For scenario H14 it was estimated two new  $E_M$ -profiles,  $E_M$ =SF1 and  $E_M$ =SF2. These two profiles are based on the idea of higher  $CO_2$  removal efficiency at the top of each packing section in the absorber column, and were created by equation 3.7 in sub-chapter 3.2.1. The simulation in figure 4.28 indicates that both these  $E_M$ 's fit the performance data well. It looks as  $E_M$ =SF1 have the best fit for temperature profile, while  $E_M$ =SF2 have the removal grade closest to performance data. The deviations are small for both  $E_M$ =SF1 and  $E_M$ =SF2. Compared with  $E_M$ =Zhu, it looks as though the new sets might have an even better fit for both temperature and removal grade for scenario H14.

#### 6.3.2 Evaluation of scenario 2B5 with estimated E<sub>M</sub> in Aspen HYSYS

For scenario 2B5, the  $E_M$ -profiles created for scenario H14 were scaled and fitted to the performance removal grade for scenario 2B5. 2B5 is a scenario with four different sets of temperature measurements, and a given average removal grade. In figure 4.30 the simulation is compared with a blue line of average temperature as well as the measured temperatures. The simulated results of the new developed  $E_M$ -profiles,  $E_M$ =SF1 and  $E_M$ =SF2, did not fit well for the average temperature profile based on the average removal grade, but had a sufficient fit to the temperature profile of plant data C and D. For this scenario the  $E_M$ -profile with the best fit to the average temperature profile was  $E_M$ =Lin\*0.935.

One can see that the measurement in plant data A is slightly higher than for C and D, while B is in between. The independent removal grade for each data set can be assumed to vary a lot, as the temperature varies a lot. It is assumed that  $E_M$ =SF1 and  $E_M$ =SF2 would fit the average line best if plant data A was neglected.

#### 6.3.3 Evaluation of scenario 6w with estimated E<sub>M</sub> in Aspen HYSYS

For scenario 6w, the  $E_M$ -profiles created for scenario H14 were scaled and fitted to the performance removal grade for scenario 6w just like for scenario 2B5, 6w is also a scenario with four different sets of temperature measurements, and a given average removal grade. In figure 4.32 the simulation is compared with a purple line of average temperature as well as the measured temperatures. The simulated results of the new developed  $E_M$ -profiles based on the average removal grade did fit the average temperature profile better than for scenario 2B5, but was a little too low. Just like for scenario SB5,  $E_M$ =SF1 and  $E_M$ =SF2 had a sufficient fit to the temperature profile of plant data C and D, but also for B.

If plant data A was removed from the average line the temperature profile would fit better. Like for scenario 2B5, the independent removal grade for each data set for scenario 6w can be assumed to vary a lot for these four data sets, as the temperature varies a lot.

#### 6.3.4 Evaluation of scenario Goal1 with estimated E<sub>M</sub> in Aspen HYSYS

For scenario Goal1, the  $E_M$ -profiles created for scenario H14 were scaled to fit the performance removal grade for scenario Goal1, just like for scenario 2B5 and 6w. Goal1 is also a scenario with four different sets of temperature measurements, and a given average removal grade. In figure 4.34 the simulation is compared with a gray line of average temperature as well as the measured temperatures. The simulated results for the new developed  $E_M$ -profiles based on the average removal grade, did give a sufficient fit to the average performance data. Just like for scenario SB5,  $E_M$ =SF1 and  $E_M$ =SF2 had a sufficient fit to the temperature profile of plant data B, C and D, while A deviated a lot.

If plant data A was removed from the average line the temperature profile would fit even better. The independent removal grade for each data set for scenario Goal1 can be assumed to vary a lot for these four data sets, as the temperature varies a lot.

#### 6.3.5 Evaluation of scenario F17 with estimated E<sub>M</sub> in Aspen HYSYS

For scenario F17 the  $E_M$ -profiles created for scenario H14 were used. They were scaled down and fitted to the removal grade given in the performance data by equation 3.8 in sub-chapter 3.2.2. As were  $E_M$ =Zhu and  $E_M$ =Lin. The simulation in figure 4.36 indicates that the best fit in both temperature profile and removal grade was  $E_M$ =SF2, but  $E_M$ =SF1 and  $E_M$ =Zhu.

By the results from these simulation it looks like the estimation method of  $E_M$ -profile by equation 3.7 and 3.8 gives satisfactory results.  $E_M$ =Zhu have proven to give a good fit to several scenarios in earlier master theses, but these results provides better results for  $E_M$ =SF1 and  $E_M$ =SF2. The main difference between Zhu and SF1 & SF2, is that Zhu has constant low efficiency from stage 13 and down. While SF1 & SF2 have constant low efficiency from stage 20 and down. The fact that SF1 & SF2 fit better than Zhu might deciphering that the bottom packing have a higher removal efficiency than suggested in earlier theses.

## 6.4 Evaluation of simulation with estimated $E_{\text{M}}$ and IAF in Aspen Plus

#### 6.4.1 Evaluation of scenario H14 with estimated E<sub>M</sub> and IAF in Aspen Plus

For the equilibrium-based model, the  $E_M$ -profiles used for simulation of scenario H14 in Aspen HYSYS were scaled to fit the removal grade for scenario H14 in Aspen Plus by adjusting the  $E_M$ -factor. From figure 4.38 it is visible that this gave similar temperature profiles as in Aspen HYSYS with god fit to the performance temperature for  $E_M$ =Zhu\*1.12,  $E_M$ =SF1\*0.995 and  $E_M$ =SF2\*1.005, while  $E_M$ =Lin\*1.17 and  $E_M$ =0.1\*1.1 deviated from the performance data. All  $E_M$ -profiles were easy to fit with removal grade by adjusting the  $E_M$ -factor.

For the rate-based model, the IAF was adjusted up to give the best fit to removal grade. For scenario H14 the IAF was not able to fit the removal grade to 90%. The highest achieved removal grade was for IAF=1, which gave a removal grade of 88.82%. The temperature profile deviated from performance data and simulations with equilibrium-based model.

#### 6.4.2 Evaluation of scenario 2B5 with estimated E<sub>M</sub> and IAF in Aspen Plus

For the equilibrium-based model, the  $E_M$ -profiles were scaled to fit the removal grade for scenario 2B5 in Aspen Plus by adjusting the  $E_M$ -factor. From figure 4.40 it is visible that this gave similar temperature profiles as in Aspen HYSYS. With the best fit to average-temperature profile for  $E_M$ =Lin\*1.005.

For the rate-based model, the IAF was adjusted up to give the best fit to removal grade. For scenario 2B5 the IAF was not able to fit the removal grade to 87.20%. The highest achieved removal grade was for IAF=1, which gave a removal grade of 86.14%. The temperature profile deviated from performance data and simulations with equilibrium-based model. The temperature profile is very similar to the rate-based temperature in scenario H14.

#### 6.4.3 Evaluation of scenario 6w with estimated E<sub>M</sub> and IAF in Aspen Plus

For the equilibrium-based model, the  $E_M$ -profiles were scaled to fit the removal grade for scenario 6w in Aspen Plus by adjusting the  $E_M$ -factor. From figure 4.42 it is visible that this gave similar temperature profiles as in Aspen HYSYS. With the best fit to average-temperature profile for  $E_M$ =SF1\*0.603 and  $E_M$ =SF2\*0.612.  $E_M$ =Lin\*0.722 fit the performance temperature better in Aspen Plus than in Aspen HYSYS.

For the rate-based model, the IAF was adjusted up to give the best fit to removal grade. For scenario 6w the best result was achieved with IAF=0.29, which gave a removal grade of 79.04%, performance data is 79.00%. The temperature profile deviated from performance data and simulations with equilibrium-based model, but have a better fit to the performance temperatures than rate-based for scenario H14 and 2B5.

#### 6.4.4 Evaluation of scenario Goal1 with estimated E<sub>M</sub> and IAF in Aspen Plus

For the equilibrium-based model, the  $E_M$ -profiles were scaled to fit the removal grade for scenario Goal1 in Aspen Plus by adjusting the  $E_M$ -factor. From figure 4.44 it is visible that this gave similar temperature profiles as in Aspen HYSYS. Overall the temperature profiles fit the performance temperature better in HYSYS. The best fit to average-temperature profile was for  $E_M$ =Zhu\*1.015.

For the rate-based model, the IAF was adjusted to give the best fit to removal grade. For scenario Goal1 the best result was achieved with IAF=0.51, which gave a removal grade of 90.11%, performance data is 90.10%. The temperature profile deviated from performance data, but had a similar profile as E<sub>M</sub>=Lin\*1.074.

#### 6.4.5 Evaluation of scenario F17 with estimated E<sub>M</sub> and IAF in Aspen Plus

For the equilibrium-based model, the  $E_M$ -profiles were scaled to fit the removal grade for scenario F17 in Aspen Plus by adjusting the  $E_M$ -factor. From figure 4.46 it is visible that this gave similar temperature profiles as in Aspen HYSYS, but in Aspen HYSYS the best fit was for  $E_M$ =SF1 and  $E_M$ =Zhu. In Aspen Plus the best fit to performance temperature was for  $E_M$ =Lin\*0.863. Overall the temperature profiles fit the performance temperature better in HYSYS.

For the rate-based model, the IAF was adjusted up to give the best fit to removal grade. For scenario F17 the best result was achieved with IAF=0.51, which gave a removal grade of 83.48%, performance data is 83.50%. The temperature profile had a similar profile as  $E_M$ =Lin\*0.863, and had an ok fit to the performance temperature.

The results from these simulation indicates that there is small deviations between the equilibrium-based model in Aspen Plus and Aspen HYSYS. The  $E_M$ -profiles can easily be scaled with the  $E_M$ -factor to fit the removal grade of any scenario, in both Aspen plus and Aspen HYSYS, but the  $E_M$ -profile must be adjusted for the simulation tool.

The rate-based method proved to be able to adjust to removal grade for some scenarios, while other scenario was less adjustable, this is assumed to be because the simulation reaches equilibrium. For the scenarios where the rate-based simulation was able to predict the requested removal grade the temperature profile fit the performance data better, but never as good as the  $E_{M}$ -fitted profiles. Typically the temperature profile lays between the fitted  $E_{M}$ -profiles and the  $E_{M}$ -profile with constant Murphree efficiency of 0.1.

#### 6.5 Evaluation of Comparison between Aspen Plus and HYSYS

#### 6.5.1 Evaluation of Comparison for scenario H14

For equilibrium-based simulation in Aspen Plus and Aspen HYSYS the results were very similar. The average temperature for each  $E_M$ -profile was higher for the simulations in Aspen Plus than the simulations in Aspen HYSYS. For scenario H14 the average temperature for  $E_M$ =SF1 and  $E_M$ =SF2 was 1.3°C higher in Aspen Plus. The temperature were 2.4°C, 2.6°C and 2.9°C for  $E_M$ =Zhu,  $E_M$ =Lin and  $E_M$ =0.1 respectively. The rich loading is almost exactly the same for Aspen Plus and Aspen HYSYS, the small deviations are assumed to be because the removal grade is calculated with  $E_M$ -factor of three decimals. If the removal grade was calculated to an accurate 90% for all  $E_M$ -profiles the deviations between rich loading in Aspen Plus and Aspen HYSYS is assumed to be 0.0004, because this is the deviation between  $E_M$ =Zhu (HYSYS) and  $E_M$ =Lin (Plus) which both have an accurate removal grade of 90.00%.

Scenario H14 is one of the scenarios where rate-based couldn't predict accurate removal grade. With highest predicted removal grade =88.82%, the rate-based model predicted rich loading of 0.4894, which is closer to performance data than equilibrium-based model, by 0.0030. The temperature on the other hand, deviates a lot from performance temperature.

For scenario H14 the best fit for temperature profile was  $E_M$ =SF1 and  $E_M$ =SF2 in HYSYS.

#### 6.5.2 Evaluation of Comparison for scenario 2B5

For scenario 2B5 the temperature deviation between Aspen Plus and Aspen HYSYS less visible than for Scenario H14. For scenario 2B5 the average temperature for  $E_M$ =SF1 was 0.07 °C higher in Aspen Plus. The temperature were 0,05°C, 0.2°C, 0.4°C and 1.1°C for  $E_M$ =SF2,  $E_M$ =Zhu,  $E_M$ =Lin and  $E_M$ =0.1 respectively. The rich loading is higher in Aspen Plus than in Aspen HYSYS. If the removal grade was calculated to an accurate 87.30% for all  $E_M$ -profiles the deviations between rich loading in Aspen Plus and Aspen HYSYS is assumed to be 0.0250, because this is the deviation between  $E_M$ =SF1 (HYSYS) and  $E_M$ =0.1 (Plus) which both have an accurate removal grade of 87.30%.

Scenario 2B5 is the other scenario where rate-based couldn't predict accurate removal grade. With the highest predicted removal grade =86.14%, the rate-based model predicted rich loading of 0.4857, which is between equilibrium-based model in Aspen HYSYS and Aspen Plus, where Aspen Plus is closest to performance data (0.5000). The temperature profile deviates a lot from performance temperature.

For scenario 2B5 the best fit for temperature profile was E<sub>M</sub>=Lin in Plus and HYSYS.

#### 6.5.3 Evaluation of Comparison for scenario 6w

For scenario 6w the average temperature for  $E_M$ =SF1,  $E_M$ =SF2 and  $E_M$ =Zhu was 0.06 °C higher in Aspen Plus. The temperature were 1.1°C higher in Aspen Plus for  $E_M$ =0.1 and 0.06 °C lower in Aspen Plus for  $E_M$ =Lin. If the removal grade had been calculated to an accurate 79.00% for all  $E_M$ -profiles the deviations between rich loading in Aspen Plus and Aspen HYSYS is assumed to be 0.0007, because this is the deviation between  $E_M$ =SF2 &  $E_M$  =Lin (Plus) and  $E_M$  =Lin &  $E_M$  =0.1 (HYSYS) which have an removal grade of 79.04 and 79.03%.

For Scenario 6w the rate-based model was able to estimate removal grade to 79.04% and rich loading to be 0.4870. From performance data the rich loading is 0.4600 which is between equilibrium-based (0.4418) and rate-based (0.4870), where Aspen HYSYS is closest to performance data. The temperature profile lays between the fitted  $E_{M-}$  profiles and  $E_{M-}$ 0.1

For scenario 6w the best fit for temperature profile was  $E_M=SF2$  and  $E_M=Lin$  in Plus.

#### 6.5.4 Evaluation of Comparison for scenario Goal1

For scenario Goal1 the average temperature for  $E_M$ =SF1,  $E_M$ =SF2 and  $E_M$ =Zhu was 1.9 °C higher in Aspen Plus. The temperature were 2.0 °C and 2.1 °C for  $E_M$ =Lin and  $E_M$ =0.1 respectively. If the removal grade had been calculated to an accurate 90.10% for all  $E_M$ -profiles the deviations between rich loading in Aspen Plus and Aspen HYSYS is assumed to be 0.0004, because this is the deviation between  $E_M$ =Lin in Plus and HYSYS.

For Scenario Goal1 the rate-based model was able to estimate removal grade to 90.11% and rich loading to be 0.4870. From performance data the rich loading is 0.5000, all models have very similar values for rich loading but Aspen HYSYS is closest to performance data, followed by equilibrium-based in Aspen Plus, and rate-based last. The rate-base temperature profile lays is very close to  $E_M$ =Lin (Plus).

For scenario Goal1 the best fit for temperature profile was  $E_M$ =SF1,  $E_M$ =SF2 and  $E_M$ =Zhu in HYSYS.

#### 6.5.5 Evaluation of Comparison for scenario F17

For scenario F17 the average temperature for each  $E_M$ -profile was higher for the simulations in Aspen HYSYS than the simulations in Aspen Plus. The average temperature for  $E_M$ =SF1 and  $E_M$ =SF2 was 0.6°C higher in Aspen HYSYS. The temperature were 0.5°C, 0.4°C and 0.3°C for  $E_M$ =Zhu,  $E_M$ =Lin and  $E_M$ =0.1 respectively. If the removal grade had been calculated to an accurate 83.50% for all  $E_M$ -profiles the deviations between rich loading in Aspen Plus and Aspen HYSYS is assumed to be 0.0500, because this is the deviation between  $E_M$ =SF2 (HYSYS) and  $E_M$ =0.1 (Plus) which both have an accurate removal grade of 83.50%.

For Scenario F17 the rate-based model was able to estimate removal grade to 83.48% and rich loading to be 0.4836. From performance data the rich loading is 0.4800. For this scenario Aspen Plus rate-based and equilibrium-based model is very similar and closest to performance data, while equilibrium-based in HYSYS is off by 0.0400. The rate-base temperature profile lays is very close to  $E_M$ =Lin (HYSYS).

For scenario F17 the best fit for temperature profile was  $E_M=SF1$  and  $E_M=SF2$  in HYSYS.

By the results from these simulation it looks like there is very small deviations between the equilibrium-based model in Aspen Plus and Aspen HYSYS. The temperature profiles seem to have higher average temperatures in Aspen Plus, even though this is not accurate for all E<sub>M</sub>-profiles in all scenarios.

The overall best fit for temperature profile have been for equilibrium-based model in Aspen HYSYS, with  $E_M$ -profiles  $E_M$ =SF1,  $E_M$ =SF2 and  $E_M$ =Lin. Lin have had the best fit for scenario 2B5 and 6w, but like mentioned earlier, these scenarios have four sets of measurements. And if data set A had been removed the average line is assumed to fit  $E_M$ =SF1 and  $E_M$ =SF2.

The overall best fit for rich loading have been alternately equally good for equilibrium-based model in Aspen HYSYS and Aspen Plus.

When all factors are added up the best predictions for all parameters where achieved by equilibrium-based model in Aspen HYSYS.

## 6.6 Evaluation of simulation with default Murphree efficiencies in Aspen HYSYS

The default  $E_M$ -profiles predicted by Aspen HYSYS was compared to the estimated  $E_M$ -profile,  $E_M$ =SF1, for all scenarios. Since the only adjustable variable in these simulations was the number of stages, it was harder to achieve the exact removal grade, compared with estimating the  $E_M$ -profile by calculation where the results can be just as accurate as requested depending on the amount of decimals used for the  $E_M$ -factor.

#### 6.6.1 Evaluation of scenario H14 with default Murphree efficiencies

For scenario H14 the removal grade from both the default simulation (89.64%) and  $E_M$ =SF1 (90.12%) was close to performance data (90.00%). The rich loading was higher for both default (0.0120) and SF1 (0.0130). The best fit for the temperature profile was for  $E_M$ =SF1. The only stages where the default is close to performance data is stage 1, 6 and 24.

#### 6.6.2 Evaluation of scenario 2B5 with default Murphree efficiencies

For scenario 2B5 the removal grade from both the default simulation (86.80%) and  $E_M$ =SF1 (87.30%) was close to performance data (87.30%). The rich loading was lower for both default (-0.0380) and SF1 (-0.0370). The best fit for the temperature profile was for  $E_M$ =SF1. The only stages the default is close to performance data is 6, 7 and 8.

#### 6.6.3 Evaluation of scenario 6w with default Murphree efficiencies

For scenario 6w the removal grade from both the default simulation (79.80%) and  $E_M$ =SF1 (79.00%) was close to performance data (79.00%). The rich loading was lower for both default (-0.0150) and SF1 (-0.0170). The best fit for the temperature profile was for  $E_M$ =SF1. The only stages the default is near performance data is 8, 9 and 10.

#### 6.6.4 Evaluation of scenario Goal1 with default Murphree efficiencies

For scenario Goal1 the removal grade from both the default simulation (90.39%) and  $E_M$ =SF1 (90.10%) was close to performance data (90.10%). The rich loading was lower for both default (-0.0120) and SF1 (-0.0090). The best fit for the temperature profile was for  $E_M$ =SF1. The only stages the default is near performance data is 6 and 24.

#### 6.6.5 Evaluation of scenario F17 with default Murphree efficiencies

For scenario F17 the removal grade from both the default simulation (82.80%) and  $E_M$ =SF1 (83.51%) was close to performance data (83.50%). The rich loading was lower for both default (-0.0470) and SF1 (-0.0450). The best fit for the temperature profile was for  $E_M$ =SF1. The only stages the default is near performance data is 7 and 8.

The trend for the simulation of all scenarios is that the simulated temperature profile with default E<sub>M</sub>-profile provides a bad fit to the temperature profile for performance data. The rich loading is very similar for default and estimated efficiency, and the removal grade is easier to adjust correctly with estimated efficiency.

When the default  $E_M$ -profile is compared with the estimated  $E_M$ -profile, one can see that the estimated profile decreases linearly with varying slope for the different sections in the packed column. While the default efficiency decreases with a polynomial profile for all stages.

The amount of stages required to achieve the requested removal grade seem to increase with the  $E_M$ -factor. This is presented below in table 6.1.

Scenario	H14	Goal1	2B5	F17	6w
E <sub>M</sub> -Factor for SF1	1.000	0.920	0.778	0.671	0.591
stages	14	13	10	8	8

Table 6.1: Correolation between E<sub>M</sub>-factor and amount of stages

#### 6.7 Evaluation of comparison of different amine packages

The results from the simulations of all scenarios shows that the amine package named Li-Mather always will give a lower removal grade than Kent-Eisenberg, and Acid Gas always will give a higher removal grade than Kent-Eisenberg.

#### 6.7.1 Evaluation of scenario H14 with different amine packages

For scenario H14, L-M gives an average removal grade 0.45% lower than K-E for all simulated  $E_{M}$ 's, while A-G gives an average removal grade 1.92% higher than K-E.

For scenario H14, L-M have an average rich loading 0.0013 lower than K-E for all simulated  $E_{M}$ 's, while A-G gives an average rich loading 0.0045 higher than K-E.

#### 6.7.2 Evaluation of scenario 2B5 with different amine packages

For scenario 2B5, L-M gives an average removal grade 0.62% lower than K-E for all simulated  $E_{M}$ 's, while A-G gives a removal grade 0.59% higher than K-E.

For scenario 2B5, L-M have an average rich loading 0.0019 lower than K-E for all simulated  $E_{M}$ 's, while A-G gives an average rich loading 0.0009 higher than K-E.

#### 6.7.3 Evaluation of scenario 6w with different amine packages

For scenario 6w L-M gives an average removal grade 0.39% lower than K-E for all simulated E<sub>M</sub>'s, while A-G gives an average removal grade 0.49% higher than K-E.

For scenario 6w, L-M have an average rich loading 0.0018 lower than K-E for all simulated  $E_{M}$ 's, while A-G gives an average rich loading 0.0006 higher than K-E.

#### 6.7.4 Evaluation of scenario Goal1 with different amine packages

For scenario goal1 L-M gives an average removal grade 0.32% lower than K-E for all simulated  $E_{M}$ 's, while A-G gives an average removal grade 1.19% higher than K-E.

For scenario goal1, L-M have an average rich loading 0.0012 lower than K-E for all simulated  $E_{M^*S}$ , while A-G gives an average rich loading 0.0002 higher than K-E.

#### 6.7.5 Evaluation of scenario F17 with different amine packages

For scenario F17, L-M gives a removal grade 0.59% lower than K-E, while A-G gives a removal grade 0.34% higher than K-E.

For scenario F17, L-M have an average rich loading 0.0016 lower than K-E for all simulated  $E_{M^*S}$ , while A-G gives an average rich loading 0.0003 higher than K-E.

Overall the average removal grade for Li-Mather is 0.47% lower than Kent-Eisenberg, and Acid-Gas is 0.91% higher than Kent-Eisenberg.

The overall average rich loading is also lowest for Li-Mather, which is 0.0016 lower than Kent-Eisenberg, while Acid-Gas is 0.0013 higher than Kent-Eisenberg.

It is also visible from the graphs in figure 4.63-4.67 that the temperature profiles of Kent-Eisenberg and Li-Mather are very similar while Acid-Gas keeps a temperature of about 2 °C higher than K-E and L-M, but the deviation decreases for the lowest stages where all the amine packages finishes with about the same temperature.

## 6.8 Comparison between results from this work and results from earlier work

Scenario H14, 2B5, 6w and Goal1 was used in the paper by  $\emptyset$ i, Sætre and Hamborg (2018) [34]. From this paper it was found that an equilibrium-based model with  $E_M$ =Zhu gave good predictions to Scenario H14 and Goal1, but not for scenario 2B5 and 6w. They found scenario 2B5 and 6w to be well predicted with a linear decreasing  $E_M$ -profile with  $E_M$ =0.192 at top stage and  $E_M$ =0.008 at bottom stage.

These results are consistent with the results from this report, except that we have a different performance removal grade for scenario H14 and 6w. Øi, Sætre and Hamborg used performance removal grades of 88.50% for both Scenario H14 and 6w. I found the removal grade for scenario H14 to be about 90.00% from Hamborg et al., (2014) [7] and from appendix D in Sætre (2016) [28] I found removal grade for scenario 6w to be 79.00%.

It is naturally that Scenario H14 and Goal1 would fit the same  $E_M$ -profile as they have almost the same removal grade of 90.00% and 90.10% respectively. This is consistent with the results from the simulations in this report where the  $E_M$ -factor used for the  $E_M$ -profiles in scenario Goal1 was close to 1 e.g. small scaling factor, and very similar  $E_M$ -profiles for Scenario H14 and Goal1. It is also naturally that 2B5 and 6w would get good predictions with the same  $E_M$ -profile if the removal grades for Scenario 2B5 and 6w was 87.30% and 88.50% as these

removal grades are fairly close to each other. But this was not the case in this report where the removal grades used for scenario 2B5 and 6w was 87.30% and 79.00%.

From figure 2 in Øi, Sætre and Hamborg, for scenario H14, they got a god temperature profile with the equilibrium-based model in Aspen HYSYS, and an ok temperature profile with the equilibrium-based model in Aspen Plus. The temperature profile achieved with the rate-based model in Aspen Plus deviated from the performance data but the deviation was less than 6 °C. Compared with the results for scenario H14 in this theses, the temperature profiles from the equilibrium-based model in Aspen Plus and Aspen HYSYS was consistent with their results. But the temperature profile from the rate-based model in Aspen Plus did not fit the performance data, and deviated with as much as 11.2 °C. The rate-based simulation in this thesis achieved removal grade closer to performance data than Øi, Sætre and Hamborg, but it reached equilibrium and was not able to achieve performance removal grade

From figure 3 in Øi, Sætre and Hamborg, for scenario 6w, they got a god temperature profile for all simulations. For rate based simulation they used IAF=0.55 to achieve a removal grade of 86.10%. In this thesis the rate-based simulation used IAF=0.29 to achieve a removal grade of 79.00%. When the results are compared the temperature profile for their rate-based model had a better fit to performance data, but not to the removal grade if the correct removal grade is 79.00%.

From figure 4 in Øi, Sætre and Hamborg, for scenario 2B5, they got a god temperature profile for all simulations, and a good fit to removal grade for equilibrium-based simulations in Aspen Plus and Aspen HYSYS. The results from this thesis achieved equally as good temperature profile and removal grade for the equilibrium-based simulations, but the temperature profile for the rate-based simulation deviated from the performance data. The rate-based simulation in this thesis achieved removal grade closer to performance data than Øi, Sætre and Hamborg, but it reached equilibrium and was not able to achieve performance removal grade.

From figure 5 in Øi, Sætre and Hamborg, for scenario Goal1, they got an ok temperature profile for all simulations, but none of them achieved a removal grade close to performance data. For the rate-based simulation Øi et al., used IAF=0.55, and in this thesis the IAF=0.51. In this thesis all of the simulation tools were able to achieve the requested removal grade. The temperature profile from equilibrium-based model in Aspen HYSYS fit well for the performance data. The temperature profile from equilibrium-based model in Aspen Plus was a little too high but had an ok fit, and temperature profile from rate-based model in Aspen Plus was even higher.

With all these results in mind one can conclude that the  $E_M$ -factor have been a necessary tool to easily achieve the right removal grade, and might even be easier to estimate than the IAF used in rate-based simulation. The  $E_M$ -factor will always increase linearly with the removal grade, but this does not always seem to be the case with the interfacial area factor.

 $\emptyset$ i, Sætre and Hamborg concluded that the equilibrium-based and rate-based model perform equally well in both fitting performance data and in predicting performance at changed conditions. With the new developed  $E_M$ -factor the equilibrium-based model can predict reliable performance data at changed conditions. From the simulations in this report the equilibrium-based model, with estimated Murphree efficiency and  $E_M$ -factor, predicts more reliable performance data than the rate-based model with estimated interfacial area factor. The reason why the equilibrium-based model with estimated  $E_M$ -profiles gives a better prediction than rate-based model, is that many parameters can be fitted.

#### 6.9 Further work

The estimated  $E_M$ -profiles SF1 and SF2 gave a god fit to the performance data, but there is room for improvement. Several fittings of  $E_M$  profiles should be made, based on the method in sub-chapter 3.2.1, to get an even better fit for temperature profile. The new estimated  $E_M$ -sets should be tested on several scenarios with different removal grades, with the new developed  $E_M$ -factor in sub-chapter 3.2.2.

It would also be interesting to test the calculation for estimating  $E_M$ -factor in equation 5.1, on different scenarios, and see if there is connections with experimental data and  $E_M$ -factor based on linearity of removal grade.

Another interesting topic might be to use the methods developed in this thesis to estimate a Murphree efficiency profile with another amine package. In this thesis, the removal grade have always been estimated to fit with Kent Eisenberg as amine package. It might be interesting to try to fit the removal grade with the amine packages Li Mather or Acid Gas in Aspen HYSYS, or the equilibrium-based model Electrolyte-NRTL in Aspen Plus, and see if this gives an even better fit with the temperature profile.

It would also be interesting to compare an equilibrium-based model and a rate-based model. Results from this work reveals that there is definitely possibilities to fit parameters in equilibrium-based model. In this work the only parameter that was varied in the rate-based model was the interfacial area factor. In the rate-based tool in Aspen Plus, there are several parameters that may be adjusted. In principle any rate-based parameters could be used as variables to fit performance data, but this may lead to a model with doubtful predictability. One possibility is to divide the absorption column into 2 or 3 sections with different IAF in each section.

The fact that the best fit of  $E_M$ -profiles are the ones with decreasing Murphree efficiency from the top stage to the bottom stage indicates that the simulation is approaching equilibrium. The temperature profile flattens out on the lowest stages, and the  $E_M$ -profile produces a temperature profile that fits the performance data better, when the Murphree efficiencies are close to zero on the lowest stages. It would be interesting to do the simulations with an 18 m packing height and see if the results is consistent with the results from the simulation with 24 m.

It would also be interesting to simulate the entire process with both the absorption and the desorption column.

## 7 Conclusion

The  $CO_2$  capture from exhaust gas is an important topic to limit man-made greenhouse gas emissions. One mature method to capture  $CO_2$  is to absorb it in an aqueous amine solution. An important step in the research to improve the technology is to create simulation tools that is able to predict the performance of the absorber. There have been developed many calculation models for process simulation, Aspen HYSYS and Aspen Plus are common tools for simulating the capture of  $CO_2$  in to amine solutions.

In this thesis the amine based CO<sub>2</sub> capture process at TCM where CO<sub>2</sub> from flue gas is absorbed into 30wt% MEA solution, have been simulated in Aspen HYSYS and Aspen Plus. The main purpose of the simulation have been to fit the removal grade, temperature profile and rich loading to the performance data. The performance data used in this paper is five different scenarios obtained from test-campaigns at TCM in 2013 and 2015. These scenarios have been simulated in earlier master theses from USN, and some of the results are verified in this thesis.

The rate-based model in Aspen Plus and the equilibrium-based model in Aspen Plus and Aspen HYSYS have been compared. The conclusion is that the equilibrium-based model is easier to adjust to fit the requested parameters. The equilibrium-based model predicts sufficient results in both Aspen HYSYS and Aspen Plus, but the results from this thesis proved that the most reliable predictions was achieved in Aspen HYSYS. The result might have been the opposite if the  $E_M$ -profile was created for the equilibrium-based model in Aspen Plus, and scaled with an  $E_M$ -factor to fit the removal grade in Aspen HYSYS.

An  $E_M$ -factor was developed in this thesis, this factor made it possible to achieve the requested removal grade, with an accuracy depending on the amount of decimals used in the  $E_M$ -factor. Two methods of estimating the  $E_M$ -factor have been proposed. The first is a try and fail method that can be combined with e.g. the bisection-method to converge towards the right answer. The second method is to estimate the  $E_M$ -factor based on experimental data. Assuming there is some linearity between the gas/amine-ratio and the deviation from the linearity of  $E_M$ -factor and removal grade. By the linear interpolation equations in chapter 5 the required  $E_M$ -factor to achieve the requested removal grade can be calculated. With the interfacial area factor, used to estimate the removal grade in the rate-based model, the calibration is less predictable, because the factor does not always seem to be linear with the result.

Some earlier papers have stated that the equilibrium-based model and the rate-based model perform equally well in fitting performance data and in predicting performance at changed conditions. Some state that the rate-based model is more reliable than the equilibrium-based model. From the results in this thesis the equilibrium-based model have proven to predict reliable results, and can easily be adjusted to predict reliable results even when the conditions are changed.

The results from this study show that it is possible to fit a rate-based model by adjusting the interfacial area factor, and to fit an equilibrium-based model by adjusting the Murphree efficiency for each stage. In this work the equilibrium and rate-based models both predicts reliable results for removal grade and rich loading, but the equilibrium-based model provides more reliable results than the rate-based model in predicting temperature profile. Which is natural as many parameters have been estimated. In addition, with the new developed E<sub>M</sub>-factor the equilibrium-based model is able to predict reliable performance at changed conditions.

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### Appendix A – Task description



Faculty of Technology, Natural Sciences and Maritime Sciences, Campus Porsgrunn

#### FMH606 Master's Thesis

Title: Process simulation of CO2 absorption at TCM Mongstad

USN supervisor: Lars Erik Øi

External partner: CO<sub>2</sub> Technology Centre Mongstad (TCM)

#### Task background:

Technology Centre Mongstad (TCM) is the world's largest facility for testing and improving CO<sub>2</sub> capture, and was started in 2006 when the Norwegian government and Statoil (now Equinor) made an agreement to establish the world's largest full scale CO2 capture and storage project. To be able to predict process behaviour, plan campaigns and verify results it is necessary to have good and robust simulation models.

There have been performed several projects at Telemark University College/ University of Southeastern Norway on process simulation of amine based CO2 capture processes. Most of the simulations have been performed with the program Aspen HYSYS, but the process has also been simulated using Aspen Plus. In Master Thesis projects from 2014, 2015, 2016 and 2017 both programs have been used to simulate the monoethanol amine (MEA) based CO2 capture process at TCM.

#### Task description:

The aim of the project is to develop simulation models for amine based CO<sub>2</sub> capture.

- 1. A literature search on process simulation of amine based CO2 capture by absorption
- 2. Perform Aspen HYSYS and/or Aspen Plus simulations of the MEA based CO2 capture process at TCM
- 3. Compare process simulations with performance data and design data

Develop the simulation models further and make suggestions for improvements

Student category: EET or PT

#### **Practical arrangements:**

The work will be carried out mainly in Porsgrunn. A visit and possibly some work at TCM Mongstad is a possibility. The aim is to base the work on open available data, so that the thesis can be open. Some information from TCM Mongstad must however be treated confidentially.

#### Supervision:

As a general rule, the student is entitled to 15-20 hours of supervision. This includes necessary time for the supervisor to prepare for supervision meetings (reading material to be discussed. etc).

Signatures:

Supervisor (date and signature):

Student (write clearly in all capitalized letters):

Student (date and signature):

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## Appendix B - TCM data for scenario H14

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#### Appendix A. Amine plant process information

Table 8 provides the amine plant main process information averaged over the base-case test time period. Process fluctuations, generally attributed to fluctuations in the  $CO_2$  content of the CHP flue gas, cannot be derived from the given values.

Table 8. Typical amine plant process information during Base-Case testing

Process parameter	Units	Value
Operating capacity	%	80
CHP flue gas supply rate	$\mathrm{Sm}^3/\mathrm{hr}$	46970
CHP flue gas supply temperature	°C	25.0
CHP flue gas supply pressure	barg	0.063
CHP flue gas supply CO2 concentration (wet)	vol%	3.7
CHP flue gas supply O2 concentration (wet)	vol%	13.6
Depleted flue gas temperature	°C	24.7
Lean MEA concentration	wt%	30
Lean CO <sub>2</sub> loading	mol CO <sub>2</sub> / mol MEA	0.23
Lean amine supply flow rate	kg/hr	54900
Lean amine supply temperature	°C	36.5
Lean amine density	$kg/m^3$	1067
Active absorber packing height	m	24
Temperature, upper absorber packing - 6	°C	45.4
Temperature, upper absorber packing - 5	°C	51.1
Temperature, upper absorber packing - 4	°C	51.2
Temperature, upper absorber packing - 3	°C	50.3
Temperature, upper absorber packing - 2	°C	49.6
Temperature, upper absorber packing - 1	°C	48.5
Temperature, middle absorber packing - 6	°C	46.7
Temperature, middle absorber packing - 5	°C	45.2
Temperature, middle absorber packing - 4	°C	43.5
Temperature, middle absorber packing - 3	°C	41.7
Temperature, middle absorber packing – 2	°C	40.6
Temperature, middle absorber packing – 1	°C	39.0
Temperature, lower absorber packing - 12	°C	38.4
Temperature, lower absorber packing - 11	°C	39.1
Temperature, lower absorber packing – 10	°C	35.0
Temperature, lower absorber packing – 9	°C	33.7
Temperature, lower absorber packing - 8	°C	32.2
Temperature, lower absorber packing - 7	°C	30.4
Temperature, lower absorber packing – 6	°C	29.8
Temperature, lower absorber packing - 5	°C	29.3
Temperature, lower absorber packing – 4	°C	28.1
Temperature, lower absorber packing – 3	°C	28.4
Temperature, lower absorber packing – 2	°C	27.6
Temperature, lower absorber packing - 1	°C	27.2

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Rich solution return temperature	°C	27.7
Temperature above upper absorber packing	°C	38.1
Wash water 1 supply flow rate	kg/hr	55000
Wash water 1 inlet temperature	°C	28.4
Wash water 1 withdrawal temperature	°C	43.9
Temperature above Wash Water 1	°C	36.2
Wash water 2 supply flow rate	kg/hr	62000
Wash water 2 inlet temperature	°C	23.5
Wash water 2 withdrawal temperature	°C	35.0
Temperature above Wash Water 2	°C	24.7
Rich CO <sub>2</sub> loading	mol CO <sub>2</sub> / mol MEA	0.48
Rich solution supply flow rate	kg/hr	57200
Rich solution supply temperature	°C	108.6
Lean solution return temperature	°C	119.1
Rich amine density	kg/m <sup>3</sup>	1114
Reboiler steam flow rate	kg/hr	4800
Reboiler steam temperature	°C	169
Reboiler steam pressure	barg	4.42
Reboiler condensate temperature	°C	118.8
Reboiler condensate pressure	barg	4.11
Stripper overhead pressure	barg	0.90
Stripper overhead temperature	°C	99.8
Stripper overhead reflux flow rate	kg/hr	1370
Stripper overhead reflux temperature	°C	23.3
Stripper sump temperature	°C	119.3
Reboiler solution temperature	°C	122.3
Lean vapour compressor system	-	off
Product CO <sub>2</sub> flow rate	kg/hr	2670
Product CO <sub>2</sub> discharge temperature	°C	17.7
Product CO <sub>2</sub> discharge pressure	barg	0.023

## Appendix C – TCM data for scenario 2B5

This data is provided to USN from TCM for scenario 2B5, the data table below is collected from appendix J in Sætre, 2016 [28].

	TCM DATA for Scenario 2B5								
Unit									
Flue gas	composition	/ absorber inlet	t -	CO2	mol%	0,0357			
0.1	,		-	H2O	mol%	0,0370			
				O2	mol%	0,1460			
				N2	mol%	0,7720			
				Ar	mol%	0,0090			
Flue gas	inlet flow			Sm3/h		46981,61			
				mol/h		1986,40			
Flue gas	inlet tempera	ature		°C		28,20			
	inlet pressure			kPa		106,30			
	vent flowrate			kg/h		49485,00			
Lean sol	vent loading			mol/mol		0,20			
Lean sol	ven temperat	ure		°C		36,80			
MEA wt	% (lean, CO2 fı			wt%		31,60			
Rich solv	vent flowrate			kg/h		52064,00			
Rich solv	vent loading			mol/mol		0,50			
Rich solv	vent temperat	ure		°C		32,20			
CO2 reco	overy			%		87,20			
			Loading pr	ofile					
Height			24	18	12	0			
Loading	Loading 0,2					0,5			
		Te	mperature	profile					
C	Column			Temperatures					
Stage	Height [m]	Plant data A	Plant data B	Plant data C	Plant data D	Average			
1	23,5	44,93	45,71	49,28	48,47	47,10			
2	23					48,44			
3	22					49,79			
4	21	0,00	51,44	50,16	51,81	51,14			
5	20					50,36			
6	18,5	49,90		-					
7	17,5	48,74	48,51	45,81	48,62				
8	17					47,24			
9	16					46,56			
10	15					45,88			
11	14	46,48	45,94	42,80	45,58	45,20			
12	12,5	42,15	41,68	39,51	41,18	41,13			
13	11,5	42,41	41,80	40,54	38,68	40,86			
14	11					39,94			
15	9,5	43,10	39,04	47,11	37,56	41,70			
16	9				2- 22	38,20			
17	8	41,54	35,96	35,64	35,98	37,28			
18	7,5	41,55	37,47	33,93	34,21	36,79			
19	6	40,53	34,40	33,41	33,38	35,43			
20	4,5	37,74	33,37	31,82	32,45	33,84			
21	4	27.00	22.42	22.24	24.40	33,56			
22	3	37,06	32,49	32,04	31,49	33,27			
23	1,5	33,39	31,12	31,03	31,37	31,73			
24	0,5	31,84	30,92	30,56	30,65	30,99			

## Appendix D - TCM data for scenario 6w

This data is provided to USN from TCM for scenario 6w, the data table below is collected from appendix D in Sætre, 2016 [28].

TCM DATA for Scenario 6w										
Unit										
Flue gas	composition,	/ absorber inle	t	CO2	vol%	3,5700				
				H2O	vol%	3,0000				
				O2	vol%	13,6000				
				N2	vol%	79,8300				
				Ar	vol%	0,0000				
Flue gas	inlet flow			Sm3/h	-	46602,00				
Flue gas	inlet tempera	nture		°C		25,00				
	inlet pressure	9		kPa		106,30				
	vent flowrate			kg/h		54915,00				
	vent loading			mol/mol	0,25					
	ven temperat			°C	36,90					
	% (lean, CO2 fi	ree)		wt%		30,40				
	vent flowrate			kg/h		52064,00				
	vent loading			mol/mol		0,46				
Rich solv	vent temperat	ure		°C						
CO2 reco	overy			%		79,00				
			Loading pr	ofile						
Height			24	18	12	0				
Loading			0,25	0,36	0,44	0,49				
		Te	mperature	profile						
С	olumn		-	Temperatures						
Stage	Height [m]	Plant data A	Plant data B	Plant data C	Plant data D	Average				
1	23,5	43,4	44,5	48,6	47,7	46,81				
2	23					47,47				
3	22					48,13				
4	21	46,8	50,6	49,2	50,8	48,81				
5	20					47,63				
6	18,5	49,2	47,3	49	· · · · · · · · · · · · · · · · · · ·	46,45				
7	17,5	47,8	47,2	45,1	47,5	44,00				
8	17					42,97				
9	16					41,93				
10	15					40,90				
11	14	45,3	44,4	41,6		39,87				
12	12,5	40,4	40			34,72				
13	11,5	39,7	39,2	38,8	37,8	34,40				
14	11					33,58				
15	9,5	39,7	36,6	44,7	37	35,10				
16	9					31,94				
17	8	37,8	33,8			31,12				
18	7,5	37,8	33,8	31,9		30,74				
19	6	36,8	31	30,7		29,86				
20	4,5	34	29,8	29,2	29,8	28,78				
21	4	22.2	30	30.0	30.4	28,72				
22	3	33,2	29			28,68				
23	1,5	29,8	27,6			27,60				
24	0,5	28,2	27,2	26,9	27	27,31				

## Appendix E - TCM data for scenario Goal1

This data is provided to USN from TCM for scenario Goal1, the data table below is collected from appendix K in Sætre, 2016 [28].

TCM DATA for Scenario Goal1										
Unit										
Flue gas	composition /	absorber inle	t	CO2	mol%	0,0362				
	•			H2O	mol%	0,0310				
				O2 mol%		0,1430				
				N2	mol%	0,7810				
				Ar	mol%	0,0090				
Flue gas	inlet flow			Sm3/h		46868,00				
Flue gas	inlet tempera	iture		°C	25,00					
	inlet pressure	<u> </u>		kPa	106,30					
Lean sol	vent flowrate			kg/h		44391,00				
Lean sol	vent loading			mol/mol		0,20				
	ven temperati			°C		36,50				
	% (lean, CO2 fr	ree)		wt%		32,40				
	vent flowrate			kg/h	47502,00					
	vent loading			mol/mol		0,50				
	vent temperat	ure		°C		28,60				
CO2 reco	overy			%		90,10				
			Loading pr	ofile						
Height			24	18	12	0				
Loading			0,2			0,5				
		Te	mperature	profile						
С	olumn			Temperatures						
Stage	Height [m]	Plant data A	Plant data B	Plant data C	Plant data D	Average				
1	23,5	45,66	46,50	47,79		_				
2	23	,	10,00	,	,	47,47				
3	22					48,13				
4	21	0,00	49,46	47,20	49,77	48,81				
5	20	ĺ	,	,	,	47,63				
6	18,5	47,01	44,30	47,01	47,50					
7	17,5	45,12	44,93	40,81	45,15					
8	17					42,97				
9	16					41,93				
10	15					40,90				
11	14	41,49	40,85	36,49	40,63	39,87				
12	12,5	35,63	35,26	33,06	34,94	34,72				
13	11,5	35,28	35,02	34,36	32,94	34,40				
14	11					33,58				
15	9,5	35,58	32,62	40,42	31,79	35,10				
16	9					31,94				
17	8	33,97	30,13	30,06	30,34					
18	7,5	34,11	30,89	28,86	29,11	30,74				
19	6	33,52	28,96	28,42	28,54					
20	4,5	31,31	28,37	27,58	27,88	28,78				
21	4					28,72				
22	3	30,80	0,00	27,78	27,46	28,68				
23	1,5	28,58	27,19			27,60				
24	0,5	28,02	27,23	26,94						

## **Appendix F – TCM data for scenario F17**

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#### Appendix C. Amine plant 2015 baseline testing results

Table 12 presents the process data for the TCM amine plant averaged for the period C3-4 of baseline testing in 2015 (when flow rates were measured). During that period the plant was running at nearly stable conditions and the process parameters fluctuations were insignificant.

Table 12. Averaged process data for the test period C3-4 of baseline testing in September 2015.							
Operating capacity	%	100					
CHP flue gas supply rate	Sm <sup>3</sup> /h	59 430					
CHP flue gas supply temperature	°C	29.8					
CHP flue gas supply pressure	barg	0.01					
CHP flue gas supply CO <sub>2</sub> concentration (dry)	vol%	3.7					
CHP flue gas supply $O_2$ concentration (wet)	vol%	14.6					
CHP flue gas supply water content	vol%	3.7					
Depleted flue gas temperature	°C	30.4					
Lean MEA concentration (CO <sub>2</sub> free)	wt%	31					
Lean MEA concentration (incl CO <sub>2</sub> )	wt%	30					
Lean CO <sub>2</sub> loading	mol CO <sub>2</sub> /mol MEA	0.20					
Lean amine supply flow rate	kg/h	57 434					
Lean amine supply temperature	$^{\circ}\mathrm{C}$	37.0					
Lean amine density	kg/m <sup>3</sup>	1 073					
Rich solution return temperature	°C	33.2					
Temperature above upper absorber packing	°C	39.7					
Wash water 1 (lower) supply flow rate	kg/h	55 005					
Wash water 1 inlet temperature	$^{\circ}\mathrm{C}$	30.4					
Wash water 1 withdrawal temperature	°C	44.9					
Temperature above Wash Water 1	°C	38.0					
Wash water 2 (upper) supply flow rate	kg/h	54 997					
Wash water 2 inlet temperature	°C	30.4					
Wash water 2 withdrawal temperature	°C	37.3					
Temperature above Wash Water 2	°C	30.4					

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Rich solution supply flow rate Rich solution supply temperature Rich solution supply temperature Rich amine density Rich amine density Reboiler steam flow rate Reboiler steam flow rate Reboiler steam temperature Reboiler steam temperature Reboiler steam temperature Reboiler steam pressure Reboiler condensate temperature Reboiler condensate temperature Reboiler condensate pressure Reboiler solution temperature Reboiler solution tem	Rich CO <sub>2</sub> loading	mol CO <sub>2</sub> /mol MEA	0.48
Rich solution supply temperature         °C         110.7           Lean solution return temperature         °C         121.3           Rich amine density         kg/m³         1 125           Reboiler steam flow rate         kg/h         5 398           Reboiler steam temperature         °C         156           Reboiler steam pressure         barg         2.04           Reboiler condensate temperature         °C         132.8           Reboiler condensate temperature         barg         1.96           Stripper overhead pressure         barg         0.91           Stripper overhead pressure         barg         0.91           Stripper overhead reflux flow rate         kg/h         1 227           Stripper overhead reflux temperature         °C         17.64           Stripper overhead reflux temperature         °C         121.0           Reboiler solution temperature         °C         122.1           Reboiler solution temperature         °C         125.1           Lean vapour compressor system         -         off           Product CO2 flow rate         kg/h         3 325           Product CO2 discharge temperature         °C         17.9           Product CO2 discharge pressure         barg	Rich solution supply flow rate	k⊈/h	60 775
Lean solution return temperature         °C         121.3           Rich amine density         kg/m³         1 125           Reboiler steam flow rate         kg/h         5 398           Reboiler steam temperature         °C         156           Reboiler steam pressure         barg         2.04           Reboiler condensate temperature         °C         132.8           Reboiler condensate pressure         barg         1.96           Stripper overhead pressure         barg         0.91           Stripper overhead reflux flow rate         kg/h         1 227           Stripper overhead reflux flow rate         kg/h         1 227           Stripper overhead reflux temperature         °C         17.64           Stripper sump temperature         °C         121.0           Reboiler solution temperature         °C         125.1           Lean vapour compressor system         -         off           Product CO2 flow rate         kg/h         3 325           Product CO2 discharge temperature         °C         17.9           Product CO2 discharge pressure         barg         0.017           Product CO2 water content         vol%         1.3           Active absorber packing height         m         24		-	110.7
Reboiler steam flow rate kg/h 5 398 Reboiler steam flow rate c		°C	121.3
Reboiler steam flow rate kg/h 5 398 Reboiler steam temperature °C 156 Reboiler steam pressure barg 2.04 Reboiler condensate temperature °C 132.8 Reboiler condensate temperature °C 132.8 Reboiler condensate pressure barg 1.96 Stripper overhead pressure barg 0.91 Stripper overhead temperature °C 96.1  Stripper overhead temperature °C 17.64 Stripper overhead reflux flow rate kg/h 1 227 Stripper overhead reflux temperature °C 17.64 Stripper sump temperature °C 121.0 Reboiler solution temperature °C 125.1 Lean vapour compressor system - off Product CO <sub>2</sub> flow rate kg/h 3 325 Product CO <sub>2</sub> discharge temperature °C 17.9 Product CO <sub>2</sub> discharge temperature °C 17.9 Product CO <sub>2</sub> discharge pressure barg 0.017 Product CO <sub>2</sub> water content vol% 1.3  Active absorber packing height m 24 Temperature, upper absorber packing - 6 °C 47.4 Temperature, upper absorber packing - 5 °C 51.7 Temperature, upper absorber packing - 3 °C 50.5 Temperature, upper absorber packing - 1 °C 49.9 Temperature, upper absorber packing - 1 °C 49.9 Temperature, middle absorber packing - 5 °C 46.0 Temperature, middle absorber packing - 5 °C 46.0 Temperature, middle absorber packing - 1 °C 44.4 Temperature, middle absorber packing - 2 °C 42.2 Temperature, middle absorber packing - 1 °C 40.9	•	$kg/m^3$	1 125
Reboiler steam temperature barg 2.04 Reboiler condensate temperature °C 132.8 Reboiler condensate temperature °C 132.8 Reboiler condensate pressure barg 1.96 Stripper overhead pressure barg 0.91 Stripper overhead temperature °C 96.1  Stripper overhead temperature °C 17.64 Stripper overhead reflux flow rate kg/h 1 227 Stripper sump temperature °C 17.64 Stripper sump temperature °C 121.0 Reboiler solution temperature °C 125.1 Lean vapour compressor system - off Product CO <sub>2</sub> discharge temperature °C 17.9 Product CO <sub>2</sub> discharge temperature °C 17.9 Product CO <sub>2</sub> discharge pressure barg 0.017 Product CO <sub>2</sub> water content vol% 1.3  Active absorber packing height m 24 Temperature, upper absorber packing – 5 °C 51.7 Temperature, upper absorber packing – 5 °C 51.7 Temperature, upper absorber packing – 3 °C 50.5 Temperature, upper absorber packing – 1 °C 48.9 Temperature, upper absorber packing – 1 °C 48.9 Temperature, upper absorber packing – 5 °C 46.0 Temperature, middle absorber packing – 1 °C 40.9	•		5 398
Reboiler steam pressure Reboiler condensate temperature Reboiler condensate temperature Reboiler condensate pressure Stripper overhead pressure Stripper overhead temperature  Stripper overhead temperature  Stripper overhead temperature  Stripper overhead reflux flow rate Stripper overhead reflux temperature  Stripper overhead reflux temperature  C Stripper sump temperature  C C C C C C C C C C C C C C C C C C			156
Reboiler condensate temperature  Reboiler condensate pressure  Barg  1.96  Stripper overhead pressure  Stripper overhead temperature  °C  96.1  Stripper overhead temperature  °C  96.1  Stripper overhead temperature  °C  Stripper overhead reflux flow rate  Stripper overhead reflux temperature  °C  17.64  Stripper sump temperature  °C  121.0  Reboiler solution temperature  °C  125.1  Lean vapour compressor system  - off  Product CO2 flow rate  kg/h  3 325  Product CO2 discharge temperature  °C  17.9  Product CO2 discharge pressure  barg  0.017  Product CO2 water content  vol%  1.3  Active absorber packing height  m  24  Temperature, upper absorber packing – 6  °C  47.4  Temperature, upper absorber packing – 3  °C  50.5  Temperature, upper absorber packing – 2  °C  49.9  Temperature, upper absorber packing – 6  °C  48.9  Temperature, upper absorber packing – 6  °C  49.9  Temperature, upper absorber packing – 6  °C  49.9  Temperature, upper absorber packing – 6  °C  49.9  Temperature, middle absorber packing – 6  °C  44.4  Temperature, middle absorber packing – 6  °C  44.4  Temperature, middle absorber packing – 3  °C  46.0  Temperature, middle absorber packing – 3  °C  44.4  Temperature, middle absorber packing – 3  °C  44.4  Temperature, middle absorber packing – 3  °C  44.4  Temperature, middle absorber packing – 3  °C  45.2  Temperature, middle absorber packing – 1  °C  40.9  Temperature, middle absorber packing – 1  °C  40.9  Temperature, middle absorber packing – 1  °C  40.9  Temperature, niver absorber packing – 1  °C  40.6  Temperature, lower absorber packing – 1  °C  40.6  Temperature, lower absorber packing – 1  °C  41.6  Temperature, lower absorber packing – 1  °C  41.6	<u>-</u>	barg	2.04
Reboiler condensate pressure barg 0.91 Stripper overhead pressure barg 0.91 Stripper overhead temperature °C 96.1  Stripper overhead reflux flow rate kg/h 1 227 Stripper overhead reflux temperature °C 17.64 Stripper sump temperature °C 121.0 Reboiler solution temperature °C 125.1 Lean vapour compressor system - off Product CO2 flow rate kg/h 3 325 Product CO2 discharge temperature °C 17.9 Product CO2 discharge pressure barg 0.017 Product CO2 water content vol% 1.3  Active absorber packing height m 24 Temperature, upper absorber packing - 6 °C 47.4 Temperature, upper absorber packing - 8 °C 51.6 Temperature, upper absorber packing - 9 °C 50.5 Temperature, upper absorber packing - 1 °C 48.9 Temperature, middle absorber packing - 5 °C 46.0 Temperature, middle absorber packing - 5 °C 44.4 Temperature, middle absorber packing - 5 °C 44.4 Temperature, middle absorber packing - 6 °C 47.2 Temperature, middle absorber packing - 7 °C 44.9 Temperature, middle absorber packing - 8 °C 45.1 Temperature, middle absorber packing - 9 °C 44.4 Temperature, middle absorber packing - 9 °C 44.4 Temperature, middle absorber packing - 1 °C 44.9 Temperature, middle absorber packing - 1 °C 44.9 Temperature, middle absorber packing - 1 °C 40.9 Temperature, middle absorber packing - 1 °C 40.9 Temperature, lower absorber packing - 1 °C 40.6 Temperature, lower absorber packing - 1 °C 40.6 Temperature, lower absorber packing - 1 °C 41.6 Temperature, lower absorber packing - 10 °C 41.6	•		132.8
Stripper overhead pressure barg 0.91  Stripper overhead temperature °C 96.1  Stripper overhead reflux flow rate kg/h 1.227  Stripper overhead reflux temperature °C 17.64  Stripper sump temperature °C 121.0  Reboiler solution temperature °C 125.1  Lean vapour compressor system - off  Product CO2 flow rate kg/h 3.325  Product CO2 discharge temperature °C 17.9  Product CO2 discharge pressure barg 0.017  Product CO2 water content vol% 1.3  Active absorber packing height m 24  Temperature, upper absorber packing - 5 °C 51.7  Temperature, upper absorber packing - 4 °C 51.6  Temperature, upper absorber packing - 2 °C 49.9  Temperature, upper absorber packing - 1 °C 48.9  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 5 °C 44.4  Temperature, middle absorber packing - 5 °C 44.4  Temperature, middle absorber packing - 6 °C 47.2  Temperature, middle absorber packing - 6 °C 47.2  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 6 °C 44.4  Temperature, middle absorber packing - 7 °C 44.4  Temperature, middle absorber packing - 9 °C 42.2  Temperature, middle absorber packing - 1 °C 44.4  Temperature, middle absorber packing - 1 °C 40.9  Temperature, middle absorber packing - 1 °C 40.9  Temperature, lower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 41.6  Temperature, lower absorber packing - 10 °C 41.6	•	bar⊈	1.96
Stripper overhead temperature °C 96.1  Stripper overhead reflux flow rate kg/h 1 227  Stripper overhead reflux temperature °C 17.64  Stripper sump temperature °C 121.0  Reboiler solution temperature °C 125.1  Lean vapour compressor system - off  Product CO2 flow rate kg/h 3 325  Product CO2 discharge temperature °C 17.9  Product CO2 discharge pressure barg 0.017  Product CO2 water content vol% 1.3  Active absorber packing height m 24  Temperature, upper absorber packing - 6 °C 47.4  Temperature, upper absorber packing - 4 °C 51.6  Temperature, upper absorber packing - 3 °C 50.5  Temperature, upper absorber packing - 1 °C 48.9  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 5 °C 44.4  Temperature, middle absorber packing - 6 °C 47.2  Temperature, middle absorber packing - 7 °C 44.4  Temperature, middle absorber packing - 9 °C 44.2  Temperature, middle absorber packing - 9 °C 44.4  Temperature, middle absorber packing - 9 °C 44.2  Temperature, middle absorber packing - 1 °C 44.4  Temperature, middle absorber packing - 1 °C 44.6  Temperature, middle absorber packing - 1 °C 44.4  Temperature, middle absorber packing - 1 °C 44.6  Temperature, middle absorber packing - 1 °C 40.9  Temperature, bower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 41.6  Temperature, lower absorber packing - 10 °C 37.4	•		0.91
Stripper overhead reflux flow rate kg/h 1 227  Stripper overhead reflux temperature °C 17.64  Stripper sump temperature °C 121.0  Reboiler solution temperature °C 125.1  Lean vapour compressor system - off  Product CO2 flow rate kg/h 3 325  Product CO2 discharge temperature °C 17.9  Product CO2 discharge pressure barg 0.017  Product CO2 water content vol% 1.3  Active absorber packing height m 24  Temperature, upper absorber packing - 6 °C 47.4  Temperature, upper absorber packing - 5 °C 51.7  Temperature, upper absorber packing - 3 °C 50.5  Temperature, upper absorber packing - 1 °C 48.9  Temperature, upper absorber packing - 6 °C 47.2  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 3 °C 43.1  Temperature, middle absorber packing - 3 °C 43.1  Temperature, middle absorber packing - 3 °C 43.1  Temperature, middle absorber packing - 3 °C 42.2  Temperature, middle absorber packing - 1 °C 44.4  Temperature, middle absorber packing - 3 °C 43.1  Temperature, middle absorber packing - 1 °C 40.9  Temperature, middle absorber packing - 1 °C 40.9  Temperature, middle absorber packing - 1 °C 40.9  Temperature, middle absorber packing - 1 °C 40.6  Temperature, middle absorber packing - 1 °C 40.6  Temperature, bower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 41.6  Temperature, lower absorber packing - 10 °C 37.4	•	2	96.1
Stripper overhead reflux temperature  Stripper sump temperature  C Stripper sumper sumper sumper sump sump sump sump sump sump sump sump			
Stripper sump temperature	Stripper overhead reflux flow rate	kg/h	1 227
Reboiler solution temperature  C C D D D D D D D D D D D D D D D D D	Stripper overhead reflux temperature	°C	17.64
Lean vapour compressor system       -       off         Product CO₂ flow rate       kg/h       3 325         Product CO₂ discharge temperature       °C       17.9         Product CO₂ discharge pressure       barg       0.017         Product CO₂ water content       vol%       1.3         Active absorber packing height       m       24         Temperature, upper absorber packing − 6       °C       47.4         Temperature, upper absorber packing − 5       °C       51.7         Temperature, upper absorber packing − 4       °C       51.6         Temperature, upper absorber packing − 3       °C       50.5         Temperature, upper absorber packing − 2       °C       49.9         Temperature, upper absorber packing − 1       °C       48.9         Temperature, middle absorber packing − 6       °C       47.2         Temperature, middle absorber packing − 5       °C       46.0         Temperature, middle absorber packing − 3       °C       43.1         Temperature, middle absorber packing − 2       °C       42.2         Temperature, middle absorber packing − 1       °C       40.9         Temperature, lower absorber packing − 1       °C       40.6         Temperature, lower absorber packing − 10       °	Stripper sump temperature	°C	121.0
Product CO <sub>2</sub> flow rate kg/h 3 325  Product CO <sub>2</sub> discharge temperature °C 17.9  Product CO <sub>2</sub> discharge pressure barg 0.017  Product CO <sub>2</sub> water content vol% 1.3  Active absorber packing height m 24  Temperature, upper absorber packing - 6 °C 47.4  Temperature, upper absorber packing - 5 °C 51.7  Temperature, upper absorber packing - 4 °C 51.6  Temperature, upper absorber packing - 3 °C 50.5  Temperature, upper absorber packing - 2 °C 49.9  Temperature, upper absorber packing - 1 °C 48.9  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 4 °C 44.4  Temperature, middle absorber packing - 5 °C 46.0  Temperature, middle absorber packing - 2 °C 44.4  Temperature, middle absorber packing - 3 °C 43.1  Temperature, middle absorber packing - 2 °C 40.9  Temperature, middle absorber packing - 1 °C 40.9  Temperature, middle absorber packing - 1 °C 40.9  Temperature, bower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 1 °C 40.6  Temperature, lower absorber packing - 10 °C 37.4	Reboiler solution temperature	$^{\circ}\mathrm{C}$	125.1
Product CO <sub>2</sub> discharge temperature  Product CO <sub>2</sub> discharge pressure  barg  0.017  Product CO <sub>2</sub> water content  vol%  1.3  Active absorber packing height  Temperature, upper absorber packing – 6  C  Temperature, upper absorber packing – 5  Temperature, upper absorber packing – 4  Temperature, upper absorber packing – 3  C  Temperature, upper absorber packing – 2  Temperature, upper absorber packing – 1  Temperature, upper absorber packing – 1  C  Temperature, middle absorber packing – 6  C  Temperature, middle absorber packing – 6  Temperature, middle absorber packing – 4  Temperature, middle absorber packing – 3  C  Temperature, middle absorber packing – 3  Temperature, middle absorber packing – 2  Temperature, middle absorber packing – 2  Temperature, middle absorber packing – 1  Temperature, middle absorber packing – 1  C  40.9  Temperature, lower absorber packing – 12  C  41.6  Temperature, lower absorber packing – 10  C  37.4	Lean vapour compressor system	-	off
Product CO <sub>2</sub> discharge pressure barg 0.017 Product CO <sub>2</sub> water content vol% 1.3  Active absorber packing height m 24 Temperature, upper absorber packing – 6 °C 47.4 Temperature, upper absorber packing – 5 °C 51.7 Temperature, upper absorber packing – 4 °C 51.6 Temperature, upper absorber packing – 3 °C 50.5 Temperature, upper absorber packing – 2 °C 49.9 Temperature, upper absorber packing – 1 °C 48.9 Temperature, middle absorber packing – 6 °C 47.2 Temperature, middle absorber packing – 5 °C 46.0 Temperature, middle absorber packing – 4 °C 44.4 Temperature, middle absorber packing – 3 °C 43.1 Temperature, middle absorber packing – 2 °C 42.2 Temperature, middle absorber packing – 1 °C 40.9 Temperature, middle absorber packing – 1 °C 40.9 Temperature, middle absorber packing – 1 °C 40.6 Temperature, lower absorber packing – 1 °C 40.6 Temperature, lower absorber packing – 1 °C 41.6	Product CO <sub>2</sub> flow rate	kg/h	3 325
Product CO <sub>2</sub> water content vol% 1.3  Active absorber packing height m 24  Temperature, upper absorber packing – 6 °C 47.4  Temperature, upper absorber packing – 5 °C 51.7  Temperature, upper absorber packing – 4 °C 51.6  Temperature, upper absorber packing – 3 °C 50.5  Temperature, upper absorber packing – 2 °C 49.9  Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Product CO <sub>2</sub> discharge temperature	°C	17.9
Active absorber packing height m 24  Temperature, upper absorber packing – 6 °C 47.4  Temperature, upper absorber packing – 5 °C 51.7  Temperature, upper absorber packing – 4 °C 51.6  Temperature, upper absorber packing – 3 °C 50.5  Temperature, upper absorber packing – 2 °C 49.9  Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 11 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Product CO <sub>2</sub> discharge pressure	barg	0.017
Temperature, upper absorber packing – 6 °C 47.4  Temperature, upper absorber packing – 5 °C 51.7  Temperature, upper absorber packing – 4 °C 51.6  Temperature, upper absorber packing – 3 °C 50.5  Temperature, upper absorber packing – 2 °C 49.9  Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 11 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Product CO <sub>2</sub> water content	vol%	1.3
Temperature, upper absorber packing – 6 °C 47.4  Temperature, upper absorber packing – 5 °C 51.7  Temperature, upper absorber packing – 4 °C 51.6  Temperature, upper absorber packing – 3 °C 50.5  Temperature, upper absorber packing – 2 °C 49.9  Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 11 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4			
Temperature, upper absorber packing – 5  Temperature, upper absorber packing – 4  Temperature, upper absorber packing – 3  Temperature, upper absorber packing – 2  Temperature, upper absorber packing – 2  Temperature, upper absorber packing – 1  Temperature, middle absorber packing – 6  Temperature, middle absorber packing – 6  Temperature, middle absorber packing – 5  Temperature, middle absorber packing – 5  Temperature, middle absorber packing – 4  Temperature, middle absorber packing – 3  Temperature, middle absorber packing – 3  Temperature, middle absorber packing – 2  Temperature, middle absorber packing – 1  Temperature, middle absorber packing – 1  Temperature, lower absorber packing – 12  Temperature, lower absorber packing – 11  Temperature, lower absorber packing – 10  Temperature, lower absorber packing – 10  Soc	Active absorber packing height	m	24
Temperature, upper absorber packing – 4  C C Temperature, upper absorber packing – 3 C Temperature, upper absorber packing – 2 C Temperature, upper absorber packing – 1 C Temperature, upper absorber packing – 1 C Temperature, middle absorber packing – 6 C Temperature, middle absorber packing – 5 C Temperature, middle absorber packing – 5 C Temperature, middle absorber packing – 4 C Temperature, middle absorber packing – 3 C Temperature, middle absorber packing – 3 C Temperature, middle absorber packing – 2 C Temperature, middle absorber packing – 2 C Temperature, middle absorber packing – 1 C Temperature, lower absorber packing – 12 C Temperature, lower absorber packing – 11 C Temperature, lower absorber packing – 11 C Temperature, lower absorber packing – 10 C 37.4	Temperature, upper absorber packing – 6	°C	47.4
Temperature, upper absorber packing – 3 °C 49.9  Temperature, upper absorber packing – 2 °C 49.9  Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, upper absorber packing $-5$	°C	51.7
Temperature, upper absorber packing – 2 °C 49.9  Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, upper absorber packing $-4$	°C	51.6
Temperature, upper absorber packing – 1 °C 48.9  Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, upper absorber packing $-3$	°C	50.5
Temperature, middle absorber packing – 6 °C 47.2  Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, upper absorber packing $-2$	°C	49.9
Temperature, middle absorber packing – 5 °C 46.0  Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, upper absorber packing – 1	°C	48.9
Temperature, middle absorber packing – 4 °C 44.4  Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, middle absorber packing $-6$	°C	47.2
Temperature, middle absorber packing – 3 °C 43.1  Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, middle absorber packing $-5$	°C	46.0
Temperature, middle absorber packing – 2 °C 42.2  Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, middle absorber packing $-4$	°C	44.4
Temperature, middle absorber packing – 1 °C 40.9  Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, middle absorber packing $-3$	°C	43.1
Temperature, lower absorber packing – 12 °C 40.6  Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, middle absorber packing $-2$	°C	42.2
Temperature, lower absorber packing – 11 °C 41.6  Temperature, lower absorber packing – 10 °C 37.4	Temperature, middle absorber packing $-1$	$^{\circ}\mathrm{C}$	40.9
Temperature, lower absorber packing – 10 °C 37.4	Temperature, lower absorber packing – 12	°C	40.6
F	Temperature, lower absorber packing – 11	°C	41.6
Temperature, lower absorber packing – 9 °C 37.1	Temperature, lower absorber packing $-10$	°C	37.4
	Temperature, lower absorber packing – 9	°C	37.1

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Temperature, lower absorber packing – 8	°C	35.9
Temperature, lower absorber packing $-7$	°C	34.3
Temperature, lower absorber packing $-6$	°C	34.1
Temperature, lower absorber packing $-5$	°C	33.8
Temperature, lower absorber packing $-4$	°C	32.9
Temperature, lower absorber packing $-3$	°C	33.2
Temperature, lower absorber packing $-2$	°C	32.5
Temperature, lower absorber packing $-1$	°C	32.4
Stripping section packing height	m	8
Temperature, stripper packing – 7	°C	102.7
Temperature, stripper packing – 6	°C	103.1
Temperature, stripper packing – 5	°C	104.5
Temperature, stripper packing – 4	°C	107.7
Temperature, stripper packing – 3	°C	112.1
Temperature, stripper packing $-2$	°C	114.7
Temperature, stripper packing – 1	$^{\circ}\mathrm{C}$	119.4

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## **Appendix G – Data from verification (HYSYS)**

#### Scenario H14

				Temperature	•	
Stage	EM	Scenario		Sætre	Røsvik	Fagerheim
		H14	Zhu (2015)	(2016)	(2018)	(2019)
Remo	val grade	90%	89.4%	89.3%	89.3%	88.42%
Ric	h loading	0.48	0.487	0.478	-	0.4885
1	0.100	45,4	44,29	46,6	44,52	45,20
2	0.100	51,1	47,45	50	47,72	48,50
3	0.100	51,2	48,58	51	48,82	49,56
4	0.100	50,3	48,92	51,2	49,1	49,79
5	0.100	49,6	48,93	51,1	49,07	49,70
6	0.100	48,5	48,81	50,9	48,89	49,48
7	0.100	46,7	48,62	50,6	48,64	49,19
8	0.100	45,2	48,38	50,3	48,32	48,85
9	0.100	43,5	48,09	49,9	48	48,46
10	0.100	41,7	47,75	49,5	47,68	48,03
11	0.100	40,6	47,37	49	47,31	47,54
12	0.100	39	46,92	48,5	46,86	46,98
13	0.100	38,4	46,42	47,9	46,3	46,36
14	0.100	39,1	45,84	47,3	45,6	45,65
15	0.100	35	45,19	46,5	44,81	44,84
16	0.100	33,7	44,41	45,6	43,94	43,93
17	0.100	32,2	43,5	44,6	42,77	42,88
18	0.100	30,4	42,44	43,5	41,47	41,69
19	0.100	29,8	41,21	42,1	40,13	40,32
20	0.100	29,3	39,79	40,5	38,73	38,71
21	0.100	28,1	38,06	38,6	37,1	36,86
22	0.100	28,4	35,97	36,4	35,13	34,71
23	0.100	27,6	33,41	33,7	32,72	32,26
24	0.100	27,2	30,26	30,4	29,84	29,48

Table G.1: Temperature profiles for Scenario H14 with  $E_{\text{M}} = 0.1$ 

		Temperature				
Stage	EM	Scenario		Sætre	Røsvik	Fagerheim
		H14	Zhu (2015)	(2016)	(2018)	(2019)
Remo	val grade	90%	89.39%	89.4%	89.3%	88.57%
Ric	h loading	0.48	0.4789	0.4784	-	0.4890
1	0.2300	45,4	45,48	47,7	45,66	46,14
2	0.2192	51,1	48,7	51,1	49,02	49,41
3	0.2085	51,2	49,56	51,8	49,94	50,16
4	0.1977	50,3	49,5	51,6	49,89	49,95
5	0.1869	49,6	49,03	50,9	49,44	49,34
6	0.1800	48,5	48,32	50,1	48,77	48,49
7	0.1762	46,7	47,41	49,1	47,94	47,44
8	0.1546	45,2	46,29	48	46,98	46,16
9	0.1438	43,5	45,04	46,6	45,88	44,74
10	0.1331	41,7	43,66	45	44,64	43,18
11	0.1223	40,6	42,18	43,2	43,25	41,45
12	0.1115	39	40,53	41,2	41,72	39,61
13	0.1007	38,4	38,77	39,1	39,99	37,73
14	0.0900	39,1	36,91	36,9	38,12	35,87
15	0.0100	35	34,98	34,7	36,17	34,09
16	0.0100	33,7	33,59	33,3	34,23	32,80
17	0.0100	32,2	32,51	32,2	32,85	31,79
18	0.0100	30,4	31,64	31,4	31,82	30,96
19	0.0100	29,8	30,91	30,7	30,99	30,23
20	0.0100	29,3	30,22	30	30,3	29,56
21	0.0100	28,1	29,56	29,3	29,65	28,93
22	0.0100	28,4	28,85	28,7	28,99	28,31
23	0.0100	27,6	28,08	28	28,26	27,67
24	0.0100	27,2	27,22	27,3	27,38	27,00

Table G.2: Temperature profiles for Scenario H14 with  $E_{\text{M}} = Zhu$ 

#### Scenario 2B5

		Temperature			
Stage	EM	Scenario	Sætre	Fagerheim	
J		H14	(2016)	(2019)	
Remo	val grade	87,2%	86.9%	89,97%	
Ric	h loading	0.5	0,4893	0.4715	
1	0.100	47,10	45,8	45,80	
2	0.100	48,44	48,8	48,86	
3	0.100	49,79	49,6	49,74	
4	0.100	51,14	49,7	49,89	
5	0.100	50,36	49,6	49,79	
6	0.100	49,59	49,3	49,58	
7	0.100	47,92	49	49,33	
8	0.100	47,24	48,6	49,04	
9	0.100	46,56	48,2	48,70	
10	0.100	45,88	47,7	48,33	
11	0.100	45,20	47,2	47,91	
12	0.100	41,13	46,6	47,43	
13	0.100	40,86	45,9	46,90	
14	0.100	39,94	45,2	46,30	
15	0.100	41,70	44,3	45,62	
16	0.100	38,20	43,4	44,84	
17	0.100	37,28	42,3	43,95	
18	0.100	36,79	41,1	42,93	
19	0.100	35,43	39,8	41,76	
20	0.100	33,84	38,2	40,42	
21	0.100	33,56	36,6	38,88	
22	0.100	33,27	34,9	37,06	
23	0.100	31,73	33,3	34,95	
24	0.100	30,99	31,8	32,51	

			Temperature	)
Stage	EM	Scenario	Sætre	Fagerheim
		H14	(2016)	(2019)
Remo	val grade	87,2%	87,2%	90,2%
Ric	h loading	0.5	0.4901	0,4722
1	0.2300	47,10	46,20	46,63
2	0.2192	48,44	49,10	49,67
3	0.2085	49,79	49,60	50,29
4	0.1977	51,14	49,20	50,08
5	0.1869	50,36	48,50	49,54
6	0.1800	49,59	47,50	48,80
7	0.1762	47,92	46,40	47,89
8	0.1546	47,24	45,00	46,78
9	0.1438	46,56	43,50	45,55
10	0.1331	45,88	41,70	44,18
11	0.1223	45,20	39,90	42,67
12	0.1115	41,13	38,10	41,04
13	0.1007	40,86	36,40	39,26
14	0.0900	39,94	34,90	37,41
15	0.0100	41,70	33,70	35,55
16	0.0100	38,20	32,90	34,34
17	0.0100	37,28	32,30	33,50
18	0.0100	36,79	31,90	32,86
19	0.0100	35,43	31,60	32,33
20	0.0100	33,84	31,30	31,86
21	0.0100	33,56	31,10	31,43
22	0.0100	33,27	30,90	31,02
23	0.0100	31,73	30,70	30,62
24	0.0100	30,99	30,50	30,21

Table G.3: T-profiles for scenario 2B5 with  $E_M = 0.1$ 

Table G.4: T- profiles for scenario 2B5 with  $E_{\text{M}} = Zhu$ 

#### Scenario 6w

		Temperature			
Stage	EM	Scenario	Sætre	Fagerheim	
		H14	(2016)	(2019)	
Remo	val grade	79,0%	87,0%	89,72%	
Ric	h loading	0,46	0,4920	0.4721	
1	0.100	46,05	45,00	45,04	
2	0.100	47,15	48,10	48,21	
3	0.100	48,25	49,10	49,27	
4	0.100	49,35	49,30	49,52	
5	0.100	49,01	49,20	49,46	
6	0.100	48,68	48,90	49,27	
7	0.100	46,90	48,60	49,02	
8	0.100	46,14	48,30	48,72	
9	0.100	45,38	47,90	48,38	
10	0.100	44,61	47,40	48,00	
11	0.100	43,85	46,90	47,56	
12	0.100	39,45	46,30	47,07	
13	0.100	38,88	45,60	46,52	
14	0.100	38,00	44,90	45,89	
15	0.100	39,50	44,00	45,17	
16	0.100	36,27	43,00	44,36	
17	0.100	35,40	42,00	43,43	
18	0.100	34,13	40,70	42,35	
19	0.100	32,55	39,30	41,11	
20	0.100	30,70	37,60	39,67	
21	0.100	30,38	35,80	37,98	
22	0.100	30,05	33,70	35,91	
23	0.100	28,35	31,50	33,41	
24	0.100	27,33	29,10	30,33	

Table G.5: T-profiles for scenario 6w with  $E_M = 0.1$ 

			Temperature	2
Stage	EM	Scenario	Sætre	Fagerheim
		H14	(2016)	(2019)
Remo	val grade	79,0%	86,9%	89,6%
Ric	h loading	0,46	0.4910	0,4721
1	0.2300	46,05	45,80	46,24
2	0.2192	47,15	48,80	49,48
3	0.2085	48,25	49,50	50,29
4	0.1977	49,35	49,30	50,17
5	0.1869	49,01	48,60	49,67
6	0.1800	48,68	47,70	48,95
7	0.1762	46,90	46,60	48,05
8	0.1546	46,14	45,20	46,95
9	0.1438	45,38	43,80	45,71
10	0.1331	44,61	42,10	44,34
11	0.1223	43,85	40,30	42,82
12	0.1115	39,45	38,50	41,16
13	0.1007	38,88	36,60	39,33
14	0.0900	38,00	34,90	37,39
15	0.0100	39,50	33,40	35,37
16	0.0100	36,27	32,20	33,93
17	0.0100	35,40	31,30	32,81
18	0.0100	34,13	30,60	31,89
19	0.0100	32,55	29,90	31,08
20	0.0100	30,70	29,30	30,32
21	0.0100	30,38	28,70	29,59
22	0.0100	30,05	28,20	28,86
23	0.0100	28,35	27,60	28,11
24	0.0100	27,33	27,00	27,30

Table G.6: T- profiles for scenario 6w with  $E_M = Zhu$ 

#### Scenario Goal1

		Temperature			
Stage	EM	Scenario	Sætre	Fagerheim	
		H14	(2016)	(2019)	
Remo	val grade	90,1%	86,1%	89,82%	
Ric	h loading	0.5	0.5	0.4863	
1	0.100	46,81	45,1	44,03	
2	0.100	47,47	47,9	46,46	
3	0.100	48,13	48,6	47,16	
4	0.100	48,81	48,7	47,30	
5	0.100	47,63	48,5	47,24	
6	0.100	46,45	48,2	47,10	
7	0.100	44,00	47,8	46,92	
8	0.100	42,97	47,4	46,69	
9	0.100	41,93	46,9	46,42	
10	0.100	40,90	46,4	46,10	
11	0.100	39,87	45,8	45,73	
12	0.100	34,72	45,1	45,29	
13	0.100	34,40	44,3	44,78	
14	0.100	33,58	43,4	44,19	
15	0.100	35,10	42,5	43,51	
16	0.100	31,94	41,4	42,72	
17	0.100	31,12	40,1	41,80	
18	0.100	30,74	38,7	40,72	
19	0.100	29,86	37,1	39,48	
20	0.100	28,78	35,3	38,04	
21	0.100	28,72	33,5	36,33	
22	0.100	28,68	31,7	34,35	
23	0.100	27,60	30,1	32,07	
24	0.100	27,31	28,5	29,55	

Table G.7: T- profiles for scenario Goal 1 with  $E_{\text{M}}=0.1$ 

			Temperature	9
Stage	EM	Scenario	Sætre	Fagerheim
		H14	(2016)	(2019)
Remo	val grade	90,1%	86,2%	90,20%
Ric	h loading	0.5	0.5	0.4876
1	0.2300	46,81	45,50	44,83
2	0.2192	47,47	48,10	47,22
3	0.2085	48,13	48,50	47,64
4	0.1977	48,81	48,00	47,38
5	0.1869	47,63	47,10	46,83
6	0.1800	46,45	45,90	46,09
7	0.1762	44,00	44,60	45,16
8	0.1546	42,97	43,00	44,00
9	0.1438	41,93	41,20	42,68
10	0.1331	40,90	39,20	41,20
11	0.1223	39,87	37,10	39,56
12	0.1115	34,72	35,10	37,74
13	0.1007	34,40	33,40	35,80
14	0.0900	33,58	32,00	33,82
15	0.0100	35,10	30,80	31,91
16	0.0100	31,94	30,00	30,70
17	0.0100	31,12	29,40	29,86
18	0.0100	30,74	29,00	29,26
19	0.0100	29,86	28,60	28,79
20	0.0100	28,78	28,30	28,41
21	0.0100	28,72	28,00	28,07
22	0.0100	28,68	27,80	27,77
23	0.0100	27,60	27,50	27,48
24	0.0100	27,31	27,30	27,20

Table G.8: T-profiles for scenario Goal1 with  $E_{\text{M}} = Zhu$ 

#### Scenario F17

		Temperature			
Stage	EM	Scenario	Røsvik	Fagerheim	
0		H14	(2018)	(2019)	
Remo	val grade	83.5%	86.6%	91.88%	
Ric	ch loading	0.48	-	0.3554	
1	0.100	47,40	45,84	45,72	
2	0.100	51,70	48,57	48,82	
3	0.100	51,60	49,26	49,77	
4	0.100	50,50	49,31	49,96	
5	0.100	49,90	49,14	49,88	
6	0.100	48,90	48,88	49,70	
7	0.100	47,20	48,58	49,47	
8	0.100	46,00	48,24	49,19	
9	0.100	44,40	47,85	48,89	
10	0.100	43,10	47,42	48,54	
11	0.100	42,20	46,95	48,14	
12	0.100	40,90	46,42	47,70	
13	0.100	40,60	45,84	47,20	
14	0.100	41,60	45,20	46,63	
15	0.100	37,40	44,51	45,98	
16	0.100	37,10	43,77	45,24	
17	0.100	35,90	42,92	44,39	
18	0.100	34,30	41,89	43,43	
19	0.100	34,10	40,41	42,32	
20	0.100	33,80	38,92	41,03	
21	0.100	32,90	37,22	39,53	
22	0.100	33,20	35,01	37,76	
23	0.100	32,50	32,80	35,62	
24	0.100	32,40	30,98	33,00	

			Temperature	•
Stage	EM	Scenario	Røsvik	Fagerheim
		H14	(2018)	(2019)
Remo	val grade	83.5%	87.90%	90.57%
Ric	h loading	0.48	-	0.4552
1	0.2300	47,40	46,04	47,09
2	0.2192	51,70	48,40	50,39
3	0.2085	51,60	48,63	51,16
4	0.1977	50,50	48,14	51,03
5	0.1869	49,90	47,34	50,56
6	0.1800	48,90	46,30	49,88
7	0.1762	47,20	45,02	49,04
8	0.1546	46,00	43,46	48,01
9	0.1438	44,40	41,52	46,86
10	0.1331	43,10	39,20	45,57
11	0.1223	42,20	36,55	44,14
12	0.1115	40,90	33,81	42,56
13	0.1007	40,60	31,24	40,85
14	0.0900	41,60	29,05	38,98
15	0.0100	37,40	27,48	36,99
16	0.0100	37,10	26,70	35,69
17	0.0100	35,90	26,53	34,75
18	0.0100	34,30	26,71	34,01
19	0.0100	34,10	27,09	33,39
20	0.0100	33,80	27,59	32,83
21	0.0100	32,90	28,11	32,31
22	0.0100	33,20	28,63	31,79
23	0.0100	32,50	29,13	31,28
24	0.0100	32,40	29,59	30,75

Table G.9: T-profiles for scenario F17 with  $E_M = 0.1$ 

Table G.10: T-profiles for scenario F17 with  $E_{\text{M}} = Zhu$ 

-		Tomporatura			
			Temperature		
Stage	EM	Scenario	Røsvik	Fagerheim	
		H14	(2018)	(2019)	
Remo	Removal grade		85.6%	89.2%	
Ric	h loading	0.48	-	0.4514	
1	0,17	47,40	45,6	46,92	
2	0,17	51,70	47,83	50,24	
3	0,17	51,60	48,19	51,09	
4	0,17	50,50	47,89	51,07	
5	0,17	49,90	47,3	50,70	
6	0,16	48,90	46,5	50,15	
7	0,15	47,20	45,55	49,48	
8	0,14	46,00	44,45	48,70	
9	0,13	44,40	43,2	47,82	
10	0,12	43,10	41,83	46,85	
11	0,11	42,20	40,35	45,78	
12	0,1	40,90	38,75	44,63	
13	0,09	40,60	37,11	43,41	
14	0,08	41,60	35,54	42,13	
15	0,07	37,40	34,19	40,82	
16	0,06	37,10	33,17	39,49	
17	0,05	35,90	32,52	38,11	
18	0,04	34,30	32,14	36,77	
19	0,03	34,10	31,91	35,48	
20	0,02	33,80	31,76	34,29	
21	0,01	32,90	31,59	33,23	
22	0,01	33,20	31,37	32,36	
23	0,01	32,50	31,05	31,60	
24	0,01	32,40	30,64	30,88	

Table G.11: Temperature profiles for scenario F17 with  $E_{\text{M}} = \text{Lin}$ 

### Appendix H – Data from verification (Plus)

#### Scenario H14

		Temperature			
Stage	EM	Scenario H14	Sætre (2016)	Røsvik (2018)	Fagerheim (2019)
Dama	ual arada	90%	, ,	•	. ,
	val grade		88.43%	88.4%	88.40%
	h loading	0.48	0,488	- 4C CE	0.4880
1	0.100	45,4	46,6	46,65	46,60
2	0.100	51,1	50	50,12	50,05
3	0.100	51,2	51	51,12	51,03
4	0.100	50,3	51,2	51,28	51,19
5	0.100	49,6	51,1	51,17	51,08
6	0.100	48,5	50,9	50,95	50,86
7	0.100	46,7	50,6	50,67	50,58
8	0.100	45,2	50,3	50,35	50,26
9	0.100	43,5	49,9	49,99	49,90
10	0.100	41,7	49,5	49,59	49,50
11	0.100	40,6	49	49,13	49,04
12	0.100	39	48,5	48,61	48,52
13	0.100	38,4	47,9	48,02	47,93
14	0.100	39,1	47,3	47,35	47,26
15	0.100	35	46,5	46,59	46,50
16	0.100	33,7	45,6	45,71	45,63
17	0.100	32,2	44,6	44,71	44,62
18	0.100	30,4	43,5	43,54	43,45
19	0.100	29,8	42,1	42,17	42,08
20	0.100	29,3	40,5	40,57	40,48
21	0.100	28,1	38,6	38,67	38,58
22	0.100	28,4	36,4	36,41	36,33
23	0.100	27,6	33,7	33,72	33,64
24	0.100	27,2	30,4	30,5	30,43

Table H.1: Temperature profiles for Scenario H14 with  $E_M = 0.1$ 

		Temperature				
Stage	EM	Scenario	Sætre	Røsvik	Fagerheim	
		H14	(2016)	(2018)	(2019)	
Remo	val grade	90%	88.43	89.0%	88.39%	
Ric	h loading	0.48	0.4880	-	0.4880	
1	0.2300	45,4	47,7	47,83	47,69	
2	0.2192	51,1	51,1	51,31	51,11	
3	0.2085	51,2	51,8	52,03	51,79	
4	0.1977	50,3	51,6	51,82	51,54	
5	0.1869	49,6	50,9	51,27	50,94	
6	0.1800	48,5	50,1	50,51	50,12	
7	0.1762	46,7	49,1	49,58	49,11	
8	0.1546	45,2	48	48,48	47,93	
9	0.1438	43,5	46,6	47,21	46,54	
10	0.1331	41,7	45	45,74	44,95	
11	0.1223	40,6	43,2	44,09	43,14	
12	0.1115	39	41,2	42,26	41,15	
13	0.1007	38,4	39,1	40,28	39,01	
14	0.0900	39,1	36,9	38,22	36,82	
15	0.0100	35	34,7	36,16	34,68	
16	0.0100	33,7	33,3	34,13	33,27	
17	0.0100	32,2	32,2	32,74	32,22	
18	0.0100	30,4	31,4	31,71	31,39	
19	0.0100	29,8	30,7	30,85	30,66	
20	0.0100	29,3	30	30,11	29,98	
21	0.0100	28,1	29,3	29,42	29,33	
22	0.0100	28,4	28,7	28,74	28,68	
23	0.0100	27,6	28	28,05	28,00	
24	0.0100	27,2	27,3	27,33	27,28	

Sætre Røsvik Fagerheim **Fagerheim** (2016) (2018)(2019)[0.55] (2019)[0.65] 88.50% 88.70% 88.38% 88.73% 0.4881 0.4891 0.4883 47,30 47,73 48,82 50,46 51,30 53,39 51,93 52,45 52,10 51,41 52,21 52,34 52,00 51,45 52,11 52,17 51,80 50,63 51,95 51,97 49,93 51,78 51,70 51,75 51,50 48,99 51,59 51,51 51,20 47,92 51,38 51,25 51,00 46,66 51,16 50,96 45,20 50,70 50,92 50,65 50,40 43,56 50,65 50,30 50,10 41,73 50,37 49,93 49,80 39,75 50,07 49,52 49,50 37,68 49,74 49,07 49,10 35,61 49,39 48,59 49,01 48,70 48,07 33,63 48,20 31,86 48,60 47,51 47,80 30,36 48,17 46,91 47,30 29,16 47,70 46,26 46,70 47,21 45,58 28,23 46,20 27,50 46,69 44,85 45,60 26,94 46,14 44,07 44,90 45,55 26,50 43,26 44,30 26,07 44,93 42,40 44,28 43,60 41,51 42,90 43,60 40,58 42,11 42,88 39,63 41,30 42,14 38,65 41,36 40,50 37,66 39,70 40,57 36,67 39,74 38,80 35,69 38,00 38,90 34,73 38,04 37,10 33,81 36,20 37,17 32,93 35,30 36,29 32,10 34,50 35,42 31,34 34,56 33,60 30,64 32,80 33,72 30,00 32,00 32,89 29,43 31,30 32,10 28,93 30,60 31,35 28,47 30,63 29,90 28,07 29,30 29,96 27,71 29,33 27,39 28,80 28,20 28,75 27,11 27,70 28,21 26,85 27,30 27,71 26,62 26,80 27,24 26,42 26,30 26,82 26,24 26,43 26,09

Table H.3: Temperature profiles for scenario H14 with Rate-base model

Table H.2: Temperature profiles for Scenario H14 with  $E_M = Zhu$ 

#### Scenario 2B5

		Temperature		
Stage	EM	Scenario	Sætre	Fagerheim
J		H14	(2016)	(2019)
Remo	val grade	87,2%	87.2%	87.2%
Ric	h loading	0.5	0.4900	0.4887
1	0.100	47,10	47,20	47,19
2	0.100	48,44	50,30	50,33
3	0.100	49,79	51,10	51,10
4	0.100	51,14	51,20	51,17
5	0.100	50,36	51,00	51,01
6	0.100	49,59	50,80	50,76
7	0.100	47,92	50,50	50,47
8	0.100	47,24	50,10	50,13
9	0.100	46,56	49,80	49,75
10	0.100	45,88	49,30	49,33
11	0.100	45,20	48,90	48,85
12	0.100	41,13	48,30	48,31
13	0.100	40,86	47,70	47,70
14	0.100	39,94	47,00	47,01
15	0.100	41,70	46,20	46,22
16	0.100	38,20	45,20	45,33
17	0.100	37,28	44,30	44,30
18	0.100	36,79	43,10	43,12
19	0.100	35,43	41,70	41,77
20	0.100	33,84	40,20	40,22
21	0.100	33,56	38,40	38,47
22	0.100	33,27	36,50	36,54
23	0.100	31,73	34,50	34,50
24	0.100	30,99	32,40	32,41

Table H.4: Temperature profiles for Scenario 2B5 with  $E_{\text{\scriptsize M}}=0.1$ 

		Temperature		
Stage	EM	Scenario	Sætre	Fagerheim
		H14	(2016)	(2019)
	val grade	87,3%	0,87	88.39%
Ric	h loading	0.5	0.4901	0.4880
1	0.2300	47,10	47,80	47,69
2	0.2192	48,44	50,80	51,11
3	0.2085	49,79	51,20	51,79
4	0.1977	51,14	50,90	51,54
5	0.1869	50,36	50,20	50,94
6	0.1800	49,59	49,30	50,12
7	0.1762	47,92	48,20	49,11
8	0.1546	47,24	46,90	47,93
9	0.1438	46,56	45,50	46,54
10	0.1331	45,88	43,80	44,95
11	0.1223	45,20	41,90	43,14
12	0.1115	41,13	40,00	41,15
13	0.1007	40,86	38,00	39,01
14	0.0900	39,94	36,20	36,82
15	0.0100	41,70	34,60	34,68
16	0.0100	38,20	33,70	33,27
17	0.0100	37,28	33,00	32,22
18	0.0100	36,79	32,50	31,39
19	0.0100	35,43	32,20	30,66
20	0.0100	33,84	31,80	29,98
21	0.0100	33,56	31,50	29,33
22	0.0100	33,27	31,20	28,68
23	0.0100	31,73	30,90	28,00
24	0.0100	30,99	30,70	27,28

Table H.5: Temperature profiles for Scenario 2B5 with  $E_{\text{\scriptsize M}}=Zhu$ 

Sætre	Fagerheim	Fagerheim
(2016)	(2019)[0.5	(2019)[0.6
86.00%	86.02%	86.12%
0.4900	0.4854	0.4856
48,35	49,35	50,75
51,20	51,54	51,72
51,40	51,54	51,49
51,30	51,37	51,26
51,00	51,17	51,01
50,86	50,96	50,74
50,60	50,73	50,44
50,30	50,47	50,11
50,00 49,75	50,20 49,91	49,75 49,36
49,40	49,59	48,93
49,00	49,25	48,47
48,66	48,89	47,97
48,25	48,50	47,44
47,80	48,08	46,86
47,33	47,63	46,24
46,83	47,16	45,58
46,30	46,65	44,88
45,70	46,12	44,13
45,13	45,56	43,35
44,50	44,96	42,53
43,85 43,20	44,34 43,69	41,68 40,79
42,44	43,03	39,89
41,70	42,30	38,97
40,94	41,57	38,04
40,16	40,82	37,12
39,36	40,05	36,22
38,56	39,27	35,35
37,76	38,48	34,54
36,96	37,69	33,78
36,18	36,91	33,10
35,43	36,14	32,50
34,71 34,00	35,40 34,69	31,99 31,55
33,40	34,03	31,19
32,84	33,40	30,90
32,30	32,84	30,66
31,88	32,34	30,47
31,50	31,90	30,32
31,17	31,51	30,20
30,89	31,18	30,11
30,66	30,90	30,04
30,47	30,67	29,99
30,30	30,47	29,94
30,16	30,31	29,91
30,03	30,18	29,89
29,89 29,70	30,08 30,00	29,88 29,87
29,70 29,45	29,94	29,87
43,43	23,34	23,00

Table H.6: Temperature profiles for scenario 2B5 with Rate-base model

#### Scenario 6w

		Temperature		
Stage	EM	Scenario	Sætre	Fagerheim
		H14	(2016)	(2019)
Remo	val grade	79,0%	87.20%	89.49%
Ric	h loading	0,46	0,4910	0.4707
1	0.100	46,05	46,50	46,31
2	0.100	47,15	49,80	49,63
3	0.100	48,25	50,70	50,62
4	0.100	49,35	50,90	50,80
5	0.100	49,01	50,70	50,72
6	0.100	48,68	50,50	50,53
7	0.100	46,90	50,20	50,28
8	0.100	46,14	49,90	49,99
9	0.100	45,38	49,50	49,67
10	0.100	44,61	49,10	49,30
11	0.100	43,85	48,60	48,89
12	0.100	39,45	48,00	48,42
13	0.100	38,88	47,40	47,89
14	0.100	38,00	46,70	47,29
15	0.100	39,50	45,90	46,60
16	0.100	36,27	45,00	45,81
17	0.100	35,40	43,90	44,90
18	0.100	34,13	42,70	43,84
19	0.100	32,55	41,30	42,61
20	0.100	30,70	39,70	41,15
21	0.100	30,38	37,80	39,40
22	0.100	30,05	35,60	37,28
23	0.100	28,35	33,10	34,64
24	0.100	27,33	30,20	31,27

Table H.7: Temperature profiles for Scenario 6w with  $E_{\text{M}} = 0.1$ 

			Temperature	•
Stage	EM	Scenario	Sætre	Fagerheim
Juage	LIVI	H14	(2016)	(2019)
Remo	val grade	79,0%	86.90%	89.68%
	h loading	0,46	0.4900	0,4702
1	0.2300	46,05	47,40	47,62
2	0.2192	47,15	50,60	51,00
3	0.2085	48,25	51,20	51,73
4	0.1977	49,35	51,00	51,57
5	0.1869	49,01	50,30	51,06
6	0.1800	48,68	49,40	50,36
7	0.1762	46,90	48,30	49,49
8	0.1546	46,14	47,10	48,46
9	0.1438	45,38	45,60	47,26
10	0.1331	44,61	43,90	45,87
11	0.1223	43,85	42,10	44,28
12	0.1115	39,45	40,10	42,46
13	0.1007	38,88	38,00	40,41
14	0.0900	38,00	36,00	38,15
15	0.0100	39,50	34,20	35,76
16	0.0100	36,27	32,90	34,21
17	0.0100	35,40	31,90	33,08
18	0.0100	34,13	31,20	32,17
19	0.0100	32,55	30,50	31,38
20	0.0100	30,70	29,90	30,65
21	0.0100	30,38	29,30	29,94
22	0.0100	30,05	28,70	29,21
23	0.0100	28,35	28,10	28,45
24	0.0100	27,33	27,50	27,64

Table H.8: Temperature profiles for Scenario 6w with  $E_{\text{M}} = Zhu$ 

Sætre	Fagerheim	Fagerheim
(2016)	(2019)[0.5	(2019)[0.6
86.10%	93.53%	95.19%
0.4880	0.4819	0.4865
47,57	48,92	50,86
50,90	52,02	52,86
51,40	52,38	52,85
51,33	52,35	52,78
51,15	52,27	52,71
50,94	52,18	52,63
50,70	52,08	52,54
50,40	51,97	52,44
50,20	51,85	52,32
49,90	51,72	52,20
49,62	51,58	52,06
49,29	51,43	51,91
48,94	51,26	51,74
48,60	51,08	51,56
48,20	50,88	51,35
47,70 47,30	50,67 50,43	51,13 50,88
46,80	50,43	50,61
46,30	49,91	50,31
45,70	49,62	49,99
45,12	49,31	49,63
44,51	48,97	49,25
43,86	48,60	48,83
43,19	48,21	48,38
42,49	47,79	47,89
41,76	47,35	47,36
41,00	46,87	46,79
40,22	46,36	46,18
39,40	45,82	45,53
38,60	45,25	44,84
37,78	44,64	44,10
36,90	44,00	43,32
36,12 35,29	43,32	42,50 41,63
34,48	42,61 41,86	40,73
33,70	41,08	39,79
32,90	40,26	38,82
32,20	39,41	37,83
31,50	38,52	36,81
30,80	37,61	35,79
30,20	36,67	34,77
29,70	35,70	33,75
29,13	34,72	32,76
28,64	33,72	31,80
28,19	32,71	30,87
27,77	31,69	29,98
27,37	30,67	29,14
26,99	29,65	28,36
26,60	28,63	27,62
26,17	27,63	26,94

Table H.9: Temperature profiles for scenario 6w with Rate-base model

#### Scenario Goal1

		Temperature		
Stage	EM	Scenario	Sætre	Fagerheim
		H14	(2016)	(2019)
Remo	val grade	90,1%	82.7%	89,63%
Ric	h loading	0.5	0.5000	0.4854
1	0.100	46,81	46,30	47,22
2	0.100	47,47	49,00	49,99
3	0.100	48,13	49,60	50,37
4	0.100	48,81	49,50	50,03
5	0.100	47,63	49,20	49,41
6	0.100	46,45	48,80	48,62
7	0.100	44,00	48,30	47,65
8	0.100	42,97	47,80	46,45
9	0.100	41,93	47,30	45,10
10	0.100	40,90	46,60	43,57
11	0.100	39,87	45,90	41,84
12	0.100	34,72	45,00	39,91
13	0.100	34,40	44,10	37,80
14	0.100	33,58	42,90	35,59
15	0.100	35,10	41,70	33,36
16	0.100	31,94	40,20	32,03
17	0.100	31,12	38,60	31,15
18	0.100	30,74	36,80	30,48
19	0.100	29,86	35,00	29,93
20	0.100	28,78	33,30	29,43
21	0.100	28,72	31,70	28,95
22	0.100	28,68	30,30	28,48
23	0.100	27,60	29,20	28,00
24	0.100	27,31	28,10	27,52

Table H.10: Temperature profiles for Scenario Goal1 with  $E_{\mbox{\scriptsize M}}=0.1$ 

		Temperature		
Stage	EM	Scenario	Sætre	Fagerheim
Juge	LIVI	H14	(2016)	(2019)
Remo	val grade	90,1%	82.7%	89.82%
Ric	h loading	0.5	0.5000	0,4860
1	0.2300	46,81	45,50	46,39
2	0.2192	47,47	49,00	49,23
3	0.2085	48,13	49,00	49,90
4	0.1977	48,81	48,20	49,93
5	0.1869	47,63	47,00	49,78
6	0.1800	46,45	45,50	49,56
7	0.1762	44,00	43,80	49,29
8	0.1546	42,97	41,70	48,98
9	0.1438	41,93	39,40	48,64
10	0.1331	40,90	37,00	48,25
11	0.1223	39,87	35,00	47,82
12	0.1115	34,72	33,20	47,33
13	0.1007	34,40	31,80	46,77
14	0.0900	33,58	30,70	46,13
15	0.0100	35,10	29,80	45,41
16	0.0100	31,94	29,20	44,58
17	0.0100	31,12	28,80	43,62
18	0.0100	30,74	28,50	42,52
19	0.0100	29,86	28,30	41,22
20	0.0100	28,78	28,00	39,71
21	0.0100	28,72	27,90	37,91
22	0.0100	28,68	27,70	35,77
23	0.0100	27,60	27,50	33,23
24	0.0100	27,31	27,40	30,29

Table H.11: Temperature profiles for Scenario Goal1 with  $E_{\text{M}} = Zhu$ 

Sætre	Fagerheim	Fagerheim
(2016)	(2019)[0.5	(2019)[0.6
78.90%	90.21%	90.40%
0.4900	0.4877	0.4880
46,70	49,51	50,90
49,00	51,05	51,11
49,00	50,96	50,93
48,70	50,82	50,75
48,30	50,66	50,56
47,90	50,49	50,34
47,50	50,30	50,09
47,10	50,10	49,82
46,60	49,88	49,52
46,10	49,63	49,20
45,60	49,37	48,83
45,00	49,08	48,43
44,40	48,77	48,00
43,80	48,43	47,52
43,10 42,40	48,06 47,67	47,00 46,44
41,70	47,07	45,83
40,90	46,79	45,17
40,10	46,30	44,47
39,20	45,78	43,72
38,40	45,22	42,91
37,50	44,63	42,06
36,60	44,01	41,16
35,70	43,35	40,22
34,80	42,65	39,24
33,90	41,92	38,22
33,00	41,15	37,17
32,20	40,35	36,11
31,40	39,52	35,04
30,70	38,67	33,98
30,00	37,79	32,94
29,40	36,89	31,96
28,90	35,98	31,04
28,40 28,10	35,06 34,15	30,21 29,48
27,80	33,26	28,86
27,50	32,39	28,34
27,30	31,57	27,92
27,20	30,79	27,58
27,00	30,08	27,32
26,90	29,44	27,12
26,80	28,87	26,96
26,80	28,39	26,84
26,70	27,97	26,75
26,70	27,63	26,69
26,60	27,34	26,64
26,60	27,11	26,60
26,50	26,93	26,58
26,40	26,78	26,56
26,20	26,68	26,57

Table H.12: Temperature profiles for scenario Goal1 with Rate-base model

#### Scenario F17

			Temperature	nre
Stage	EM	Scenario	Røsvik	Fagerheim
)		H14	(2018)	(2019)
Removal	90	83.5%	86.65%	88.40%
Rich	h Ioading	0.48		0.4880
1	0.100	47,40	47,34	46,60
2	0.100	51,70	50,12	50,05
33	0.100	51,60	50,69	51,03
4	0.100	50,50	20,66	51,19
2	0.100	49,90	50,45	51,08
9	0.100	48,90	50,17	50,86
7	0.100	47,20	49,85	50,58
8	0.100	46,00	49,48	50,26
6	0.100	44,40	49,06	49,90
10	0.100	43,10	48,60	49,50
11	0.100	42,20	48,07	49,04
12	0.100	40,90	47,47	48,52
13	0.100	40,60	46,79	47,93
14	0.100	41,60	46,02	47,26
15	0.100	37,40	45,14	46,50
16	0.100	37,10	44,14	45,63
17	0.100	35,90	42,98	44,62
18	0.100	34,30	41,66	43,45
19	0.100	34,10	40,15	42,08
20	0.100	33,80	38,47	40,48
21	0.100	32,90	36,66	38,58
22	0.100	33,20	34,86	36,33
23	0.100	32,50	33,20	33,64
24	0.100	32,40	31,74	30,43

Table H.13: Temperature profiles for Scenario F17 with  $E_{\text{M}}\,{=}\,0.1$ 

			Temperature	ure
Stage	EM	Scenario	Røsvik	Fagerheim
)		H14	(2018)	(2019)
Removal	val grade	83.5%	87,20%	88.39%
	Rich loading	0.48		0.4880
1	0.2300	47,40	47,72	47,69
7	0.2192	51,70	50,32	51,11
က	0.2085	51,60	50,55	51,79
4	0.1977	50,50	50,07	51,54
2	0.1869	49,90	49,28	50,94
9	0.1800	48,90	48,29	50,12
7	0.1762	47,20	47,09	49,11
∞	0.1546	46,00	45,67	47,93
6	0.1438	44,40	44,01	46,54
10	0.1331	43,10	42,13	44,95
11	0.1223	42,20	40,10	43,14
12	0.1115	40,90	38,06	41,15
13	0.1007	40,60	36,22	39,01
14	0.0900	41,60	34,70	36,82
15	0.0100	37,40	33,48	_
16	0.0100	37,10	32,53	33,27
17	0.0100	35,90	31,98	32,22
18	0.0100	34,30	31,63	31,39
19	0.0100	34,10	31,38	30,66
	0.0100	33,80	31,18	29,98
21	0.0100	32,90	31,02	29,33
	0.0100	33,20	30,88	28,68
23	0.0100	32,50	30,75	28,00
24	0.0100	32,40	30,63	27,28

Table H.14: Temperature profiles for Scenario F17 with  $E_{\text{M}} = Zhu\,$ 

			<b>Femperature</b>	ure
Stage	EM	Scenario	Røsvik	Fagerheim
0		H14	(2018)	(2019)
Removal	val grade	83.5%	86.30%	86.24%
Rich	h loading	0.48		0.4929
1	0,17	47,40	47,58	41,974
2	0,17	51,70	50,26	50,/865
3	0,17	51,60	50,63	51,1983
4	0,17	50,50	50,33	20,9067
2	0,17	49,90	49,77	50,3442
9	0,16	48,90	49,03	49,5992
7	0,15	47,20	48,16	48,7174
8	0,14	46,00	47,15	47,7061
6	0,13	44,40	46,02	46,5651
10	0,12	43,10	44,76	45,2953
11	0,11	42,20	43,38	43,9039
12	0,1	40,90	41,89	42,4088
13	60'0	40,60	40,34	40,844
14	0,08	41,60	38,77	3,7
15	0,07	37,40	37,25	/'/
16	90'0	37,10	35,86	oʻ
17	0,05	'n,	34,64	35,1054
18	0,04	34,30	33,61	34,0635
19	0,03	34,10	32,76	33,2072
70	0,02	33,80	32,09	32,5233
21	0,01	32,90	31,58	31,9987
	0,01	33,20	31,22	_
23	0,01	32,50	30,94	υĴ
	0,01	32,40	30,71	31,105

Table H.15: Temperature profiles for Scenario F17 with  $E_{\text{M}} = Lin$ 

Røsvik	Fagerheim	Fagerheim
(2018)	(2019)[0.5	(2019)[0.6
88.50%	83.76%	83.94%
0.4883	0.4846	0.4852
47,13	49,38	50,75
51,27	51,23	51,37
49,74	51,18	51,14
49,63	51,00	50,91
48,97	50,81	50,67
48,38	50,60	50,40
47,66	50,37	50,11
46,87	50,13	49,80
45,98	49,86	49,46
44,99	49,59	49,10
43,91	49,29	48,71
42,73	48,97	48,29
41,46	48,64	47,84
40,12 38,72	48,28	47,36 46,85
36,72 37,30	47,90 47,50	46,30
35,89	47,30	45,73
34,55	46,63	45,12
33,32	46,16	44,49
32,27	45,67	43,82
31,43	45,16	43,12
30,81	44,62	42,39
30,37	44,06	41,64
30,08	43,48	40,86
	42,87	40,07
	42,25	39,26
	41,60	38,44
	40,95	37,62
	40,27	36,81
	39,58	36,02
	38,89	35,25
	38,19	34,52
	37,49	33,84
	36,79	33,22
	36,11	32,67
	35,45	32,19
	34,80	31,78
	34,19	31,44
	33,62	31,16
	33,09	30,95
	32,61	30,78
	32,18	30,65
	31,80	30,55
	31,48	30,48
	31,21	30,42
	30,98	30,38
	30,79	30,36
	30,64	30,34
	30,52	30,33
	30,42	30,33

Table H.16: Temperature profiles for scenario F17 with Rate-base model

## Appendix I – Data from simulation with estimated Murphree efficiency (HYSYS)

#### Scenario H14

Scenario H14	io H14	SF1 (90,1	,12%)	SF2 (89,94%)	()34%)		Zhu *1.106 (90.00%)	0.00%)	* uil	Lin *1.159 (90,00%)	(%0	0.1	0.1 *1.101 (90.01%)	1%)
		Removal grade	90,12	Removal grad	89,94	Removal grade	grade	06	Removal grade	rade	06	Removal grade	grade	10,06
		Rich loading	0,4936	Rich loading	0,4931	Rich loading	ng	0,4933	Rich loading	Jg.	0,4885	Rich loading	ng	0,4427
Height (m)	Step	EM	_	EM	T	EM	EM Ma	_	EM	EM 1		EM	EM	_
24	1	0,245	46,43423	0,24	46,411369	0,23	0,25	46,15531546	0,17	0,19703	45,19928	0,1	0,1101	46,31302
23	2	0,2425	49,80819	0,235	49,783948	0,2192	0,24	49,4357382	0,17	0,19703	48,50233	0,1	0,1101	49,33061
22	ю	0,24	50,59425	0,23	50,581542	0,2085	0,23	50,1848433	0,17	0,19703	49,56453	0,1	0,1101	50,01751
21	4	0,2375	50,3917	0,225	50,407563	0,1977	0,22	49,98058266	0,17	0,19703	49,78902	0,1	0,1101	49,90349
20	2	0,235	49,72219	0,22	49,792754	0,1869	0,21	49,36624789	0,17	0,19703	49,69899	0,1	0,1101	49,47054
19	9	0,2325	48,7175	0,215	48,885781	0,18	0,20	48,5158092	0,16	0,18544	49,47788	0,1	0,1101	48,85475
18	7	0,23	47,37409	0,23	47,704211	0,1762	0,19	47,46149473	0,15	0,17385	49,18967	0,1	0,1101	48,11853
17	∞	0,2	45,64572	0,2	46,103334	0,1546	0,17	46,18145711	0,14	0,16226	48,85018	0,1	0,1101	47,28099
16	6	0,17	43,69197	0,17	44,254003	0,1438	0,16	44,76568279	0,13	0,15067	48,46368	0,1	0,1101	46,34905
15	10	0,14	41,60845	0,14	42,262455	0,1331	0,15	43,21078415	0,12	0,13908	48,02784	0,1	0,1101	45,32775
14	11	0,11	39,57541	0,11	40,275671	0,1223	0,14	41,49319485	0,11	0,12749	47,53463	0,1	0,1101	44,22469
13	12	0,08	37,7206	0,08	38,424106	0,1115	0,12	39,66731114	0,1	0,1159	46,98238	0,1	0,1101	43,04981
12	13	0,05	36,11771	0,055	36,799821	0,1007	0,11	37,78956234	60'0	0,10431	46,35338	0,1	0,1101	41,81853
11	14	0,0475	34,79678	0,0525	35,427972	60'0	0,10	35,93070121	80′0	0,09272	45,64306	0,1	0,1101	40,54881
10	15	0,045	33,64282	0,05	34,202939	0,01	0,01	34,15152262	0,07	0,08113	44,83812	0,1	0,1101	39,26551
6	16	0,0425	32,5978	0,0475	33,079114	0,01	0,01	32,85558966	90'0	0,06954	43,92198	0,1	0,1101	37,93476
8	17	0,04	31,63047	0,045	32,030922	0,01	0,01	31,84359623	0,05	0,05795	42,87751	0,1	0,1101	36,63035
7	18	0,0375	30,71945	0,0425	31,045598	0,01	0,01	31,00376577	0,04	0,04636	41,68521	0,1	0,1101	35,37716
9	19	0,035	29,85226	0,04	30,106005	0,01	0,01	30,26902753	0,03	0,03477	40,32256	0,1	0,1101	34,2037
2	20	0,0001	29,01557	0,0001	29,199105	0,01	0,01	29,59664412	0,02	0,02318	38,71654	0,1	0,1101	33,14101
4	21	0,0001	28,32445	0,0001	28,455056	0,01	0,01	28,95771203	0,01	0,01159	36,85763	0,1	0,1101	32,22497
ю	22	0,0001	27,72883	0,0001	27,819038	0,01	0,01	28,33151258	0,01	0,01159	34,71193	0,1	0,1101	31,49707
2	23	0,0001	27,20374	0,0001	27,259634	0,01	0,01	27,68963246	0,01	0,01159	32,25969	0,1	0,1101	30,87855
1	24	0,0001	26,72995	0,0001	26,756237	0,01	0,01	27,01435771	0,01	0,01159	29,48468	0,1	0,1101	30,31713
Calculated efficiency	ency	94,83380484	84 %	94,56295847 %	%	92,4054	94,5707405 %	%	90,95945	94,5822 %	%	92,02336	94,59836 %	%
simulated efficiency	ency	90,12	12 %	89,94	%	06	% 06	%	06	6	%	90,01	90,01 %	%
difference		4,713804836		4,62295847	)	0 2,40538	4,57074049		0 0,959447	4,582202		0 2,013356	4,588361	

Table I.1: Data from simulation of scenario H14 in Aspen HYSYS (Kent-Eisenberg)

#### Scenario 2B5

	SF1*0,778		(82,30%)	SF2*0,79		(87,31%)	Zhu*0,88		(82,29%)	Lin*0,935		(87,32%)	0.1*0,886		(82,29%)
Rem	Removal grade	rade	87,3	Removal grade	rade	87,31	Removal grade	rade	87,29	Removal grade	rade	87,32	Removal grade	grade	87,29
Ric	Rich loading	Jg	0,4635	Rich loading	ng l	0,4635	Rich loading	lg l	0,4634	Rich loading	g,	0,4635	Rich loading	ng	0,4634
E	EM (H14)	EM*0,778	T	EM(H14)	EM*0,79	T	EM(H14)	EM*0,88	Т	EM	EM*0,935	T	EM	EM*0,886	T
	0,245	0,1906	46,44101	0,24	0,1896	46,45285	0,23	0,20263	46,36482	0,17	0,1590	46,31302	0,1	9880′0	45,55251
	0,2425	0,1887	49,4237	0,235	0,1857	49,4429	0,2192	0,193115	49,30871	0,17	0,1590	49,33061	0,1	0,0886	48,54922
	0,24	0,1867	50,01988	0,23	0,1817	50,05084	0,2085	0,183689	49,88009	0,17	0,1590	50,01751	0,1	0,0886	49,40882
	0,2375	0,1848	49,77749	0,225	0,1778	49,83095	0,1977	0,174174	49,6286	0,17	0,1590	49,90349	0,1	0,0886	49,53891
	0,235	0,1828	49,17348	0,22	0,1738	49,26648	0,1869	0,164659	49,04514	0,17	0,1590	49,47054	0,1	0,0886	49,4152
	0,2325	0,1809	48,33231	0,215	0,1699	48,49098	0,18	0,15858	48,27815	0,16	0,1496	48,85475	0,1	0,0886	49, 19119
	0,23	0,1789	47,26312	0,23	0,1817	47,52709	0,1762	0,155232	47,35258	0,15	0,1403	48,11853	0,1	0,0886	48,91454
	0,2	0,1556	45,93161	0,2	0,1580	46,26198	0,1546	0,136203	46,24646	0,14	0,1309	47,28099	0,1	0,0886	48,5983
	0,17	0,1323	44,44316	0,17	0,1343	44,82589	0,1438	0,126688	45,03704	0,13	0,1216	46,34905	0,1	0,0886	48,24397
	0,14	0,1089	42,87605	0,14	0,1106	43,30419	0,1331	0,117261	43,70836	0,12	0,1122	45,32775	0,1	0,0886	47,84895
	0,11	0,0856	41,30946	0,11	0,0869	41,77883	0,1223	0,107746	42,26122	0,11	0,1029	44,22469	0,1	0,0886	47,40872
	0,08	0,0622	39,82779	0,08	0,0632	40,3344	0,1115	0,098232	40,70858	0,1	0,0935	43,04981	0,1	0,0886	46,91777
	0,05	0,0389	38,46205	0,055	0,0435	39,01699	0,1007	0,088717	39,03163	60'0	0,0841	41,81853	0,1	0,0886	46,36922
	0,0475	0,0370	37,3481	0,0525	0,0415	37,90777	60'0	0,07929	37,27153	80′0	0,0748	40,54881	0,1	0,0886	45, 75536
	0,045	0,0350	36,3421	0,05	0,0395	36,87716	0,01	0,00881	35,45702	0,07	0,0655	39,26551	0,1	0,0886	45,06664
_	0,0425	0,0331	35,37985	0,0475	0,0375	35,86871	0,01	0,00881	34,28323	90′0	0,0561	37,93476	0,1	0,0886	44, 29154
	0,04	0,0311	34,43302	0,045	0,0356	34,85999	0,01	0,00881	33,45555	0,05	0,0468	36,63035	0,1	0,0886	43,41663
	0,0375	0,0292	33,48937	0,0425	0,0336	33,84153	0,01	0,00881	32,82256	0,04	0,0374	35,37716	0,1	0,0886	42,42652
	0,035	0,0272	32,54433	0,04	0,0316	32,81053	0,01	0,00881	32,30053	0,03	0,0281	34,2037	0,1	0,0886	41,30311
	0,0001	0,0001	31,59555	0,0001	0,0001	31,76481	0,01	0,00881	31,84156	0,02	0,0187	33,14101	0,1	0,0886	40,02391
	0,0001	0,0001	30,9512	0,0001	0,0001	31,05818	0,01	0,00881	31,41722	0,01	0,0094	32,22497	0,1	0,0886	38,56275
	0,0001	0,0001	30,50387	0,0001	0,0001	30,56884	0,01	0,00881	31,01064	0,01	0,0094	31,49707	0,1	0,0886	36,84885
	0,0001	0,0001	30,18842	0,0001	0,0001	30,22393	0,01	0,00881	30,60989	0,01	0,0094	30,87855	0,1	0,0886	34,85052
	0,0001	0,0001	29,95775	0,0001	0,0001	29,97253	0,01	0,00881	30,6743	0,01	0,0094	30,31713	0,1	0,0886	32,50742
								•							
	94,8338	89,4175		94,5630	89,4306		92,4054	89,4033		90,9594	89,3142		92,0234	89,2101	
	90,12	87,3		89,94	87,31		88,28	87,29		88,91	87,32		89,97	87,29	
	4,713805	2,117526		4,622958	2,120555		4,125385	2,113253		2,049447	2,049447   1,9941963		2,053356	1,920121	

Table I.2: Data from simulation of scenario 2B5 in Aspen HYSYS (Kent-Eisenberg)

#### Scenario 6w

0,1										ш	
49,33061		46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469	46,31302 49,33061 50,01751 49,90349 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469 43,04981 41,81853 40,54881	46,31302 49,33061 50,01751 49,90349 49,47054 48,11853 47,28099 46,34905 45,32775 44,22469 43,04981 41,81853 40,54881 39,26551	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469 43,04981 41,81853 40,54881 37,93476 36,63035 35,37716	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469 43,04981 41,81853 40,54881 39,26551 37,93476 36,63035 35,37716 34,2037 33,14101	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469 43,04981 41,81853 40,54881 37,93476 37,93476 36,63035 35,37716 37,93476 36,22497 31,49707	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469 43,04881 39,26551 37,93476 36,63035 35,37716 34,2037 33,14101 32,22497 31,49707 30,87855 30,31713	46,31302 49,33061 50,01751 49,90349 49,47054 48,85475 48,11853 47,28099 46,34905 45,32775 44,22469 43,04981 41,81853 40,54881 39,26551 37,93476 36,63035 35,37716 33,14101 32,22497 31,49707 30,87855
0,1590	0,1590 0,1590 0,1590 0,1590 0,1496	0,1590 0,1590 0,1590 0,1590 0,1496 0,1403 0,1309	0,1590 0,1590 0,1590 0,1590 0,1496 0,1403 0,1309 0,1216	0,1590 0,1590 0,1590 0,1496 0,1408 0,1309 0,1216 0,1029 0,00335	0,1590 0,1590 0,1590 0,1590 0,1496 0,1403 0,1309 0,1216 0,1029 0,0935 0,0935	0,1590 0,1590 0,1590 0,1590 0,1496 0,1403 0,1309 0,1216 0,1122 0,1029 0,0935 0,0935 0,0655	0,1590 0,1590 0,1590 0,1496 0,1403 0,1309 0,1029 0,0335 0,0935 0,0655 0,0655 0,0468 0,0561	0,1590 0,1590 0,1590 0,1496 0,1403 0,1029 0,1029 0,0935 0,0935 0,0655 0,0655 0,0468 0,0468 0,0187	0,1590 0,1590 0,1590 0,1496 0,1403 0,1309 0,1216 0,1029 0,0935 0,0935 0,0655 0,0655 0,0468 0,0374 0,0374 0,0374 0,0187 0,0094	0,1590 0,1590 0,1590 0,1496 0,1403 0,1309 0,1029 0,0935 0,0935 0,00551 0,0054 0,0094 0,0094 0,0094 0,0094	0,1590 0,1590 0,1590 0,1590 0,1496 0,1309 0,1309 0,1029 0,0335 0,0337 0,034 0,0374 0,0374 0,0374 0,0374 0,0374 0,0374 0,0374 0,0374 0,0374 0,0374 0,0094 0,0094
000000	49,88009 49,6286 49,04514 48,27815	49,88009 49,6286 49,04514 48,27815 47,35258 46,24646	49,88009 49,6286 49,04514 48,27815 47,35258 46,24646 45,03704 43,70836	49, 88009 49, 6286 49, 04514 48, 27815 47, 35258 46, 24646 45, 03704 43, 70836 40, 70858	49, 88009 49, 6286 49, 04514 48, 27815 47, 35258 46, 24646 45, 03704 43, 70836 42, 26122 40, 70858 39, 03163	49, 88009 49, 6286 49, 04514 48, 27815 47, 35258 46, 24646 45, 03704 43, 70836 42, 26122 40, 70858 39, 03163 37, 27153 34, 28323	49, 88009 49, 6286 49, 04514 48, 27815 47, 35258 46, 24646 43, 70836 42, 26122 40, 70858 39, 03163 37, 27153 35, 45702 34, 28323 33, 42555	49, 88009 49, 6286 49, 04514 48, 27815 47, 35258 46, 24646 45, 03704 43, 70858 39, 03163 37, 27153 33, 45555 32, 30053 31, 84156	49,88009 49,6286 49,04514 48,27815 47,35258 46,24646 45,03704 43,70858 39,03163 37,27153 35,45702 34,28323 33,45555 32,80053 31,84156 31,01064	49,88009 49,6286 49,04514 48,27815 47,35258 46,24646 45,03704 43,70836 40,70858 39,03163 37,27153 35,45702 34,28323 33,45555 32,82256 32,30053 31,84156 31,41722 31,01064 30,60989	49,88009 49,6286 49,04514 48,27815 47,35258 46,24646 43,70836 42,26122 40,70858 39,03163 37,27153 33,45555 32,82256 31,84156 31,84156 31,41722 31,6064 30,60989
	0,1977 0,174174 0,1869 0,164659 0,18 0,15858										
_	0,1817 50,05084 0,1778 49,83095 0,1738 49,26648 0,1699 48,49098										
					1 1						
0,1007											
	0,2375 0,18 0,235 0,18 0,2325 0,18	<del>- 11</del>									
0 5	4 72 0	4 10 0 1 8 1	4 7 9 7 8 6 0 1	4 6 6 7 10 10 11 12 12 12 12 12 12 12 12 12 12 12 12	4	4 6 6 7 7 9 8 8 8 11 11 11 11 11 11 11 11 11 11 11	4 6 6 7 7 10 11 11 11 11 11 11 11 11 11 11 11 11	4	4 6 6 7 7 8 8 7 11 11 11 11 11 11 11 11 11 11 11 11 1	4	20 5 18 7 17 8 16 9 15 10 14 11 11 14 10 15 9 16 8 17 7 18 6 19 6 19 7 22 7 23 1 24

Table I.3: Data from simulation of scenario 6w in Aspen HYSYS (Kent-Eisenberg)

### Scenario Goal1

Scenario Goal1	SF1*0,854		(90,11%)	SF2*0,886		(%60'06)	2hu*0,966		(%60'06)	Lin*1,029		(90,10%)	0.1*0,974		(%60'06)
	Removal grad	ape	90,11	Removal grade	rade	60'06	Removal grade	rade	60'06	Removal grade	grade	90,1	Removal grade	grade	60'06
	Rich loading	h.c	0,4207	Rich loading	Jg.	0,4207	Rich loading	Jg.	0,4207	Rich loading	ng	0,4207	Rich loading	ng	0,4207
Height (m) Step	EM (H14) E	EM*0,778	T	EM(H14)	EM*0,79	T	EM(H14)	EM*0,88	T	EM	EM*0,935	T	EM	EM*0,886	T
24 1	0,245	0,1906	46,44101	0,24	0,1896	46,45285	0,23	0,20263	46,36482	0,17	0,1590	46,31302	0,1	9880′0	45,55251
23 2	0,2425	0,1887	49,4237	0,235	0,1857	49,4429	0,2192	0,193115	49,30871	0,17	0,1590	49,33061	0,1	0,0886	48,54922
22 3	0,24	0,1867	50,01988	0,23	0,1817	50,05084	0,2085	0,183689	49,88009	0,17	0,1590	50,01751	0,1	0,0886	49,40882
21 4	0,2375	0,1848	49,77749	0,225	0,1778	49,83095	0,1977	0,174174	49,6286	0,17	0,1590	49,90349	0,1	0,0886	49,53891
20 5	0,235	0,1828	49,17348	0,22	0,1738	49, 26648	0,1869	0,164659	49,04514	0,17	0,1590	49,47054	0,1	0,0886	49,4152
19 6	0,2325	0,1809	48,33231	0,215	0,1699	48,49098	0,18	0,15858	48,27815	0,16	0,1496	48,85475	0,1	0,0886	49,19119
18 7	0,23	0,1789	47,26312	0,23	0,1817	47,52709	0,1762	0,155232	47,35258	0,15	0,1403	48,11853	0,1	0,0886	48,91454
17 8	0,2	0,1556	45,93161	0,2	0,1580	46,26198	0,1546	0,136203	46,24646	0,14	0,1309	47,28099	0,1	0,0886	48,5983
16 9	0,17	0,1323	44,44316	0,17	0,1343	44,82589	0,1438	0,126688	45,03704	0,13	0,1216	46,34905	0,1	0,0886	48,24397
15 10	0,14	0,1089	42,87605	0,14	0,1106	43,30419	0,1331	0,117261	43,70836	0,12	0,1122	45,32775	0,1	0,0886	47,84895
14 11	0,11	0,0856	41,30946	0,11	6980'0	41,77883	0,1223	0,107746	42,26122	0,11	0,1029	44,22469	0,1	0,0886	47,40872
13 12	0,08	0,0622	39,82779	0,08	0,0632	40,3344	0,1115	0,098232	40,70858	0,1	0,0935	43,04981	0,1	0,0886	46,91777
12 13	0,05	0,0389	38,46205	0,055	0,0435	39,01699	0,1007	0,088717	39,03163	60'0	0,0841	41,81853	0,1	0,0886	46,36922
11 14	0,0475	0,0370	37,3481	0,0525	0,0415	37,90777	0,09	0,07929	37,27153	0,08	0,0748	40,54881	0,1	0,0886	45,75536
10 15	0,045	0,0350	36,3421	0,05	0,0395	36,87716	0,01	0,00881	35,45702	0,07	0,0655	39,26551	0,1	0,0886	45,06664
9 16	0,0425	0,0331	35,37985	0,0475	0,0375	35,86871	0,01	0,00881	34,28323	90'0	0,0561	37,93476	0,1	0,0886	44,29154
8 17	0,04	0,0311	34,43302	0,045	0,0356	34,85999	0,01	0,00881	33,45555	0,05	0,0468	36,63035	0,1	0,0886	43,41663
7 18	0,0375	0,0292	33,48937	0,0425	0,0336	33,84153	0,01	0,00881	32,82256	0,04	0,0374	35,37716	0,1	0,0886	42,42652
6 19	0,035	0,0272	32,54433	0,04	0,0316	32,81053	0,01	0,00881	32,30053	0,03	0,0281	34,2037	0,1	0,0886	41,30311
5 20	0,0001	0,0001	31,59555	0,0001	0,0001	31, 76481	0,01	0,00881	31,84156	0,02	0,0187	33,14101	0,1	0,0886	40,02391
4 21	0,0001	0,0001	30,9512	0,0001	0,0001	31,05818	0,01	0,00881	31,41722	0,01	0,0094	32,22497	0,1	0,0886	38,56275
3 22	0,0001	0,0001	30,50387	0,0001	0,0001	30,56884	0,01	0,00881	31,01064	0,01	0,0094	31,49707	0,1	0,0886	36,84885
2 23	0,0001	0,0001	30,18842	0,0001	0,0001	30,22393	0,01	0,00881	30,60989	0,01	0,0094	30,87855	0,1	0,0886	34,85052
1 24	0,0001	0,0001	29,95775	0,0001	0,0001	29,97253	0,01	0,00881	30,6743	0,01	0,0094	30,31713	0,1	0,0886	32,50742
Calculated efficiency	94,8338	0,000,0	#	94,5630	91,6593		92,4054	94,1292		90,9594	91,6139		92,0234	94,0620	
simulated efficiency	90,3	90,11	#	\$ 90,02	90,09		90,2	90,09		89,91	90,1		89,97	60'06	
difference	4,533805	-90,11	#	4,542958	1,569294		2,205385	4,03917		1,049447	1,513906		2,053356	3,971972	

Table I.4: Data from simulation of scenario Goal1 in Aspen HYSYS (Kent-Eisenberg)

### Scenario F17

Scenario F17	SF1	SF1*0,671 (83,51%)	1%)	SF2*0,68	0,68 (83,50%)	(%0)	Zhu	Zhu*0,76 (83,54%)	54%)	Lin*(	Lin*0,81 (83,51%)	51%)	0.1*0	0.1*0,761 (83,49%)	(%6
	Removal grade	grade	83,51	Removal grade	ade	83,5	Removal grade	rade	83,54	Removal grade	grade	83,51	Removal grade	ade	83,49
	Rich loading	ng	0,4354	Rich loading	2	0,4353	Rich loading	Jg.	0,4354	Rich loading	ng	0,4353	Rich loading	00	0,4353
Height (m) Step	EM (H14)	EM*0,671	T	EM(H14)	EM*0,68	T	EM(H14)	EM*0,76	T	EM	EM*0,81	Т	EM	EM*0,761	T
24 1	0,245	0,1644	46,56386	0,24	0,1632	46,535464	0,23	0,1748	46,455015	0,17	0,13685	46,412	0,1	0,0761	45,88199
23 2	0,2425	0,1627	49,69863	0,235	0,1598	49,664709	0,2192	0,166592	49,541338	0,17	0,13685	49,58039	0,1	0,0761	49,10222
22 3	0,24	0,1610	50,38244	0,23	0,1564	50,354819	0,2085	0,15846	50,19734	0,17	0,13685	50,35815	0,1	0,0761	50,09258
21 4	0,2375	0,1594	50,17242	0,225	0,1530	50,162358	0,1977	0,150252	49,977286	0,17	0,13685	50,27677	0,1	0,0761	50,28837
20 5	0,235	0,1577	49,58039	0,22	0,1496	49,604363	0,1869	0,142044	49,404879	0,17	0,13685	49,85083	0,1	0,0761	50,19976
19 6	0,2325	0,1560	48,75399	0,215	0,1462	48,836643	0,18	0,1368	48,649504	0,16	0,1288	49,23669	0,1	0,0761	49,99853
18 7	0,23	0,1543	47,71706	0,23	0,1564	47,895007	0,1762	0,133912	47,748128	0,15	0,12075	48,50725	0,1	0,0761	49,74036
17 8	0,2	0,1342	46,44547	0,2	0,1360	46,684662	0,1546	0,117496	46,686465	0,14	0,1127	47,68652	0,1	0,0761	49,44154
16 9	0,17	0,1141	45,03606	0,17	0,1156	45,326555	0,1438	0,109288	45,53804	0,13	0,10465	46,78343	0,1	0,0761	49,10508
15 10	0,14	0,0939	43,5555	0,14	0,0952	43,895712	0,1331	0,101156	44,285826	0,12	9960′0	45,80341	0,1	0,0761	48,72899
14 11	0,11	0,0738	42,06904	0,11	0,0748	42,45902	0,1223	0,092948	42,926887	0,11	0,08855	44,75239	0,1	0,0761	48,30878
13 12	0,08	0,0537	40,6472	0,08	0,0544	41,087216	0,1115	0,08474	41,461972	0,1	0,0805	43,63769	0,1	0,0761	47,83926
12 13	0,05	0,0336	39,36715	0,055	0,0374	39,856939	0,1007	0,076532	39,897602	60'0	0,07245	42,46943	0,1	0,0761	47,31309
11 14	0,0475	0,0319	38,31365	0,0525	0,0357	38,814125	60'0	0,0684	38,212142	0,08	0,0644	41,25999	0,1	0,0761	46,72341
10 15	0,045	0,0302	37,31795	0,05	0,0340	37,847421	0,01	0,0076	36,409475	0,07	0,05635	40,02409	0,1	0,0761	46,05962
9 16	0,0425	0,0285	36,36103	0,0475	0,0323	36,853094	0,01	0,0076	35,202827	90'0	0,0483	38,77978	0,1	0,0761	45,30973
8 17	0,04	0,0268	35,40799	0,045	0,0306	35,850149	0,01	0,0076	34,325948	0,05	0,04025	37,51217	0,1	0,0761	44,45984
7 18	0,0375	0,0252	34,43906	0,0425	0,0289	34,817489	0,01	0,0076	33,639361	0,04	0,0322	36,26933	0,1	0,0761	43,49247
6 19	0,035	0,0235	33,44131	0,04	0,0272	33,740492	0,01	0,0076	33,063529	0,03	0,02415	35,07892	0,1	0,0761	42,38661
5 20	0,0001	0,0001	32,40377	0,0001	0,0001	32,605354	0,01	0,0076	32,551638	0,02	0,0161	33,97429	0,1	0,0761	41,1158
4 21	0,0001	0,0001	31,6643	0,0001	0,0001	31,799405	0,01	0,0076	32,072696	0,01	0,00805	32,99398	0,1	0,0761	39,64469
3 22	0,0001	0,0001	31,12427	0,0001	0,0001	31,211752	0,01	0,0076	31,608348	0,01	0,00805	32,18628	0,1	0,0761	37,92874
2 23	0,0001	0,0001	30,72278	0,0001	0,0001	30,774157	0,01	0,0076	31,145663	0,01	0,00805	31,4781	0,1	0,0761	35,85459
1 24	0,0001	0,0001	30,41848	0,0001	0,0001	30,441574	0,01	0,0076	30,6743	0,01	0,00805	30,82119	0,1	0,0761	33,33372
				•									•		
Calculated efficiency	94,8338	85,2487	#	94,5630	85,2151		92,4054	85,2513	#	90,9594	85,1453	#	92,0234	85,0377	
simulated efficiency	90,12	83,51	#	89,94	83,5		88,28	83,54	#	89,54	83,51	#	72,06	83,49	
difference	4,713805	1,7387035	#	4,6229585	1,71514		4,125385	1,711287	#	1,419447	1,63526	#	1,253356 1,5476706	1,5476706	

Table I.5: Data from simulation of scenario F17 in Aspen HYSYS (Kent-Eisenberg)

## Appendix J – Data from simulation with estimated Murphree efficiency (Plus)

#### Scenario H14

3%)	10,06	0,4427	_	46,8969	50,4122	51,4071	51,5771	51,4735	51,2654	51,0019	50,6949	50,344	49,9446	49,4897	48,9707	48,3768	47,6952	46,9099	46,0012	44,9447	43,7096	42,2579	40,5437	38,5169	36,1343	33,3737	30,2124	%	2 %			(IA	e base F=1)	ed
0.1 *1.100 (90.03%)	rade	ng	EM	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	0,1100	93,89957		3,869574		(88)		8,82 4894
0.1	Removal grade	Rich loading	EM	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	92,02336	90.01	0 2,013356			52,0	4007 0345
(%	06	0,4885		47,849	51,3963	52,2095	52,1283	51,7012	51,0667	50,2806	49,3527	48,2808	47,0622	45,6983	44,1985	42,5834	40,8878	39,1587	37,4479	35, 7994	34,2426	32,793	31,4618	30,2676	29,2551	28,3319	27,4366				_		51,7 51,4	1856 7759 4076
Lin *1.170 (90,00%)	ade	<b>D</b> 0	EM ⊢					0,1989	0,1872	0,1755	0,1638 4	0,1521 4	_	0,1287 4	0,117	0,1053 4		0,0819		0,0585		0,0351	0,0234	0,0117		_	0,0117	94, 20941 %	% 06				50,4 49,8	9679 4612 8871
Lin *1	Removal grade	Rich loading	EM	0,17	0,17	0,17	0,17	0,17	0,16	0,15	0,14	0,13	0,12	0,11	0,1		80'0	0,07	90'0	0,05	0,04	0,03	0,02	0,01	0,01	0,01	0,01	90.95945					48,4	2292 4911 6571
(%	6	0,4933		47,9127	51,3808	52,0643	51,8184	51,1961	50,3458	49,2756	47,9347	46,409	44,67	42,7273	40,636	38,4925	36,3987	34,3986	33,0556	32,0599	31,2532	30,5482	29,8941	29,2589	28,6209	27,9636	27,2706			0			45,7 44,5	7325 7046 5816 3554
Zhu*1.120 (90.05%)	ade	bū	EM	0,258	0,246	0,234	0,221	0,209	0,202	0,197	0,173	0,161	0,149	0,137	0,125	0,113	0,101	0,011	0,011	0,011	0,011	0,011	0,011	0,011	0,011	0,011	0,011	94.6178564 %	90.05 %	4,56785642			40,6 39,1	0418 6432 1879 6946
ďZ	Removal grade	Rich loading	EM	0,23	0,2192	0,2085	0,1977	0,1869	0,18	0,1762	0,1546	0,1438	0,1331	0,1223	0,1115	0,1007	60'0	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	92.4054		_			36,2 34,7	2078 7614 4075
(%	89,94	0,4931	-	48,0322	51,5426	52,2572	52,0406	51,436	50,5718	49,4525	47,8998	46,0646	44,0616	42,0229	40,0854	38,3669	36,9196	35,5924	34,3256	33,0944	31,8838	30,6799	29,4565	28,5511	27,8593	27,3175	26,8822	%	2 %				31 <sub>,</sub>	1762 ,101 1823
SF2*1.005 (89,98%	a		EM	0,241	0,236	0,231	0,226	0,221	0,216	0,231	0,201	0,171	0,141	0,111	0,080	0,055	0,053	0,050	0,048	0,045	0,043	0,040	000'0	000'0	000'0	0000	0,000	94.65050401	86.68	4,670504012			28,7 28,2	4207 7907 2788 8569
*SF2*	Removal grade	Rich loading	EM	0,24	0,235	0,23	0,225	0,22	0,215	0,23	0,2	0,17	0,14	0,11	0,08	0,055	0,0525	0,05	0,0475	0,045	0,0425	0,04	0,0001	0,0001	0,0001	0,0001	0,0001	94.56295847	89.94				27,5 27,2	5147 2299 9983
	90,12	0,4936		48,0479	51,5593	52,266	52,0289	51,3817	50,4389	49,1798	47,5244	45,5971	43,5139	41,416	39,4438	37,7052	36,2848	35,0123	33,8159	32,6626	31,5333	30,4128	29,2767	28,4308	27,782	27,2725	26,8625	~	8 %				26,6 26	8029 6439 ,508
(%50'06) 566.			EM	0,244	0,241	0,239	0,236	0,234	0,231	0,229	0,199	0,169	0,139	0,109	0,080	0,050	0,047	0,045	0,042	0,040	0,037	0,035	0,000	0,000	0,000	0,000	0,000	94 747378	90.05	4,6973783			26,3 26	3979 3024 5,226 1587
SF1*0.995	Removal grade	loading	EM	0,245	0,2425	0,24	0,2375	0,235	0,2325	0,23	0,2	0,17	0,14	0,11	80'0	0,05	0,0475	0,045	0,0425	0,04	0,0375	0,035	0,0001	0,0001	0,0001	0,0001	0,0001	94.83380484	90.12	4,713804836			26,1 26,0 26,0	1059 0584 0224
H14			Step	1	2	8	4	2	9	7	8	6	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	774	Vac				25,9 25,9 25,9	9892 9653 9424 9274
Scenario H14			Height (m)	24	23	22	21	20	19	18	17	16	15	14	13	12	11	10	6	∞	7	9	2	4	3	2	1	Calculated efficiency	simulated efficiency	difference		24	25,9 25,8	9122 9045 8984 9097 0003

Table J.1: Data from simulation of scenario H14 in Aspen Plus (eNRTL & Rate-based)

#### Scenario 6w

			_																														
79,07%)	79,07	0,4426	Г	45,2186	48,2375	49,1326	49,2594	49,1065	48,8409	48,5176	48,1533	47,7514	47,3102	46,8258	46,2932	45,7057	45,0558	44,3336	43,5276	42,6228	41,6	40,4342	39,0913	37,5233	35,6597	33,3904	30,5261					Rate based (IAF=0,29) (79,04%)	
	rade	80	EM*0,680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	0,0680	60 775	70.07	1,705271			),04 487
0.1*0,680	Removal grade	Rich loading	EM	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	1,500,00	89.77	2,303356		42,55 46,10	021
																																48,01	
	79,03	0,4427		046	102	941	573	733	8	228	509	957	599	466	586	003	786	025	981	448	90	808	244	584	528	999	365					48,93	
3%)		o,		46,3046	49,402	50,1041	49,9573	49,4733	48,8044	48,0228	47,1509	46,1957	45,1599	44,0466	42,8586	41,6003	40,2786	38,9025	37,486	36,0448	34,6002	33,1808	31,8244	30,584	29,528	28,566	27,6365					49,29 49,39	
(79,03%)			2 T	,			_	_			_				`		_			,	,	,	,									49,34	
7			EM*0,722	227	227	227	227	227	0,1155	0,1083	211	0,0939	0,0866	794	722	0,0650	0,0578	0,0505	0,0433	361	0,0289	217	144	272	272	272	272	01 000	79 03	2,055797		49,3	
22	age		M*(	0,1227	0,1227	0,1227	0,1227	0,1227	0,1	0,1	0,1011	0,0	0,0	0,0794	0,0722	0,0	0,0	0,0	0,0	0,0361	0,0	0,0217	0,0144	0,0072	0,0072	0,0072	0,0072	2	,	,05		49,08	
Lin*0,722	Removal grade	Rich loading	E																										+		-	48,91	
Lin	ova	loac		17	0,17	0,17	0,17	0,17	0,16	0,15	0,14	0,13	0,12	0,11	0,1	60'0	80′0	0,07	90'0	0,05	0,04	0,03	0,02	0,01	0,01	0,01	0,01	00 0000	88 91	2,049447		48,72	
	em	ich	EM	0,17	0	0	0	0	o,	0	0	0	0	0	O)	o,	o,	o,	o,	o,	o,	0,	oʻ	0,	0,	Ō,	o,	0	3	<b>18</b>		48,52	
			回																								_			7		48,31	
	78,92	0,4426		561	737	427	174	49,0107	48,1968	47,2386	46,1161	)24	43,5739	42,1173	219	38,7782	36,8723	542	427	292	31,4487	213	30,055	149	767	28,1224	338					48,09	
9	78	0,4		46,3661	49,3737	49,9427	49,6474	9,0	8,15	7,23	6,1	44,9024	3,57	2,1	40,5219	8,7,	6,87	34,7642	33,3427	32,292	1,4	30,7213	30,0	29,4149	28,7767	8,17	27,4338					47,85	599
(78,92%)			⊥	4	4	4	4	4	4	4	4	4	4	4	4	m	m	m	m		က	က		7	7	7	7					47,6	618
(78)			38	4	99	78	36	92	4	116	28	84	80	64	82	9/:	7	∞ ∞	ω <sub>ω</sub>	<sub>∞</sub>	<sub>∞</sub>	<sub>∞</sub>	<sub>∞</sub>	ω <sub>ω</sub>	∞ ∞	<sub>∞</sub>	∞ ∞	7	78 97	56		47,36	
0	e		EM*0,68	0,1564	0,149056	0,14178	0,134436	0,127092	0,1224	0,119816	0,105128	0,097784	0,090508	0,083164	0,07582	0,068476	0,0612	0,0068	0,0068	0,0068	0,0068	0,0068	0,0068	0,0068	0,0068	0,0068	0,0068	710110	7	2,26466		47,10	
89′(	rad	g	EM	0	0,1	0	0,1	0,1	0	0,1	0,1	0,0	0,0	0,0	o,	0,0	0	0	0	0	0	0	0	0	0	0	0	9	5	2,		46,82	
Zhu*0,680	Removal grade	Rich loading			2	ί	_	<u>و</u>		2	ب	∞	<del>,</del>	m	5	_												5	89.60	85	1	46,53	
7	JO T	h lo	EM(H14)	0,23	0,2192	0,2085	0,1977	0,1869	0,18	0,1762	0,1546	0,1438	0,1331	0,1223	0,1115	0,1007	60'0	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	אסט מסבע	8	2,805385		46,24	
	Rer	Ric	EM	)	0	0	0	0	Ŭ	0	0	0	0	0	0	0	_	_	_	J	_	_	_	_	_	_	$\Box$	6	2	2,8		45,92	
	3	9		4	<u>ق</u>	Ú	5	ᆫ	Ū.	7	6	5	m	Ū.	7	4	2	9	6	2	რ	2	m	9	ĸ	ξŨ	2					45,60	
	79,03	0,4426		46,4914	49,5559	50,1645	49,9005	49,2801	48,455	47,4587	46,1829	44,7505	43,2313	41,6865	40,187	38,8174	37,6382	36,5176	35,39	34,2182	32,9783	31,6462	30,1843	29,1106	28,2913	27,6473	27,1262					45,26 44,91	
3%		0		46,	49,	50,	49,	49,	4	47,	46,	4	43,	41,	4	38,	37,	36,	(,,	34,	32,	31,	30,	29,	28,	27,	27,					44,54	
79,03%)			2 T																										. <u>r</u>	)		44,16	
-			EM*0,612	69t	0,1438	0,1408	377	0,1346	0,1316	0,1408	0,1224	0,1040	357	0,0673	190	337	321	0,0306	291	0,0275	260	245	201	001	201	001	01	07 1677	79.03	2,1372		43,76	
17	de		*	0,1469	0,17	0,17	0,1377	0,13	0,13	0,17	0,17	0,10	0,0857	0,0	0,0490	0,0337	0,0321	0,0	0,0291	0,0	0,0260	0,0245	0,0001	0,0001	0,0001	0,0001	0,0001	7	֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓	2,13		43,35	
F2*0,612	Removal grade	loading																				-1							~		-	42,92	
SF2	oval	oac	EM(H14)	24	0,235	0,23	25	22	15	23	7	17	14	11	80'0	22	0,0525	0,05	0,0475	0,045	0,0425	0,04	0,0001	0,0001	0,0001	01	01	0633 10	89 88	2958		42,47	
	emo	Rich I	$\stackrel{>}{=}$	0,24	0,2	0,	0,225	0,22	0,2	0,23	0	0,	0	0,	0,0	0,055	0,0	ó	0,0	0,0	0,0	0,0	ο,α	0,0	0,0	0,0	0,0	2	] ~	4,682		42,00	
	œ	~	□																										_	4		41,52	223
	86	.26		59	81	29	118	37	59	8	88	126	8	83	98	26	8	43	29	4	21	693	.61	18	88	73	92					41,01	184
	78,98	0,4426		46,4959	49,5581	50,1567	49,8718	49,2137	48,3259	47,2284	45,8889	44,4026	42,8294	41,2283	39,6686	38,2356	37,0364	35,9243	34,8267	33,7044	32,5321	31,2893	29,9461	28,9518	28,1889	27,5873	27,0992					40,49	944
<b>%8</b> 6			⊥	4(	4	20	4	4	4	4	4	4	4	4	33	33	'n	3	ñ	æ	m	χ̈́	7	28	52	7	5					39,94	
(78,98%)			03		~	_	~	_	~	_	.0	10	_	~	~	~	.0	_	.0	_	.0	_	_		_		_	-	1 8	32		39,38	
			EM*0,603	0,1477	0,1462	0,1447	0,1432	0,1417	0,1402	0,1387	0,1206	0,1025	0,0844	0,0663	0,0482	0,0302	0,0286	0,0271	0,0256	0,0241	0,0226	0,0211	0,0001	0,0001	0,0001	0,0001	0,0001	110110	78 98	2,211092		38,7	
99,	grade	ρ0	*	0,	0	0	0	0	0	0,	0,	0	0	0,	0	0,	0	0,	0	0,	0	0	o,	0,	0,	0,	o)	2	7	2,2		38,17	
SF1*0,603	al gr	Rich loading	4) E						- 2														_	_	_	_		00	3 8	_	1	37,54	
SF	Removal	loa	EM (H14)	0,245	0,2425	0,24	0,2375	0,235	0,2325	0,23	0,2	0,17	0,14	0,11	0,08	0,05	0,0475	0,045	0,0425	0,04	0,0375	0,035	0,0001	0,0001	0,0001	0,0001	0,0001	0000 10	90.02	4,813805		36,8	
	∂eπ	₹ich	M.	0,	0,2	0	0,2	0	0,2	Ó	0	0	0	0	O	O	0,	O,	0,	0	0,	0	0,	0,	0,0	0	ŏ	9	5	4,81		36,18	
	_	-1	ш																												1	35,46	
			2																									2	2 2	2		34,70 33,92	
<b>%</b>			Step	1	7	3	4	2	9	7	∞	6	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24			2		33,92	
rio			,																									9	υ Ψ	 		32,24	
Scenario 6w		j	(m)																								$\Box$	+	to d	ince		31,34	
Sc			⊣eight (m	24	23	22	21	20	19	18	17	16	15	14	13	12	11	10	6	∞	7	9	2	4	3	7	П	Sacional peter policiones	simulated efficiency	difference		30,39	
			Hei																									5	i.	dif		29,40	
		•	_																													25, 10	

Table J.2: Data from simulation of scenario 6w in Aspen Plus (eNRTL & Rate-based)

### Scenario 2B5

	87,3	0,4891		108	592	51,1323	51,1932	51,0318	50,7857	50,4914	50,1558	49,7775	49,3514	48,8711	48,3286	47,7145	47,0175	242	45,3183	44,281	43,0905	238	611	38,3976	36,4626	34,4289	32,3765						ate base AF=1)
(%0	"	7,0		47,2108	50,3592	51,1	51,1	51,0	50,7	20,7	50,1	49,7	49,3	48,8	48,3	47,7	47,0	46,2242	45,3	4	43,0	41,7238	40,1611	38,3	36,4	34,7	32,3						36,14%)
(87,30%)			1800	8	<u>∞</u>	<u>∞</u>	∞	<u>∞</u>	<u></u>	<u>∞</u>	<u>∞</u>	<u>∞</u>	<u>∞</u>	∞	∞	<u>∞</u>	∞		71	87,3	21												
	de		EM*1,008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008	0,1008		89,2101	∞	1,910121		8 0,4
0.1*1,008	Removal grade	Rich loading	Ē			_			_	_			_		_		_		_	_				_	_					97			
0.1	Jove 1	loa		0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1		92,0234	89,97	2,053356		54,2
	Rer	Rich	EM																										92		2,0		50,8 51,2
	εί	)1		6			~	7	.0	~		~	0	6	.0	~		6	- 1	~	~	- 1	~	.0	6	~	~						50
	87,3	0,4891		47,7309	50,8287	51,4107	51,2118	50,7127	50,0246	49,1988	48,245	47,1643	45,9579	44,6329	43,2046	41,7012	40,1651	38,6479	37,2031	35,8748	34,6888	33,6571	32,7833	32,0726	31,5409	31,1078	30,7233						50,2
(%0		0	_	47,	50,	51,	51,	50,	50,	49,	8,	47,	45,	4,	43,	41,	40,	38,	37,	35,	34,	33,	32,	32,	31,	31,	30,						49,6
(87,30%)			4  T																									H	~	87,3	53		49,0
8)			EM*1,004	0,1707	0,1707	0,1707	0,1707	0,1707	0,1606	0,1506	0,1406	0,1305	0,1205	0,1104	0,1004	0,0904	0,0803	0,0703	0,0602	0,0502	0,0402	0,0301	0,0201	0,0100	0,0100	0,0100	0,0100		89,3142	87	2,0141963		48,3
9	ge		Λ*1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0′0	0′0	0,0	0,0		89)		,012		47,5
Lin*1,004	gra	ling	П																											1			46,6
Lin	val	oac			7	7	7	7	9	5	4	[]	7	П	1	9	8	7	9	35	4	33	75	ᅜ	ᅜ	7	ᅜ		594	88,91	3447		45,6
	Removal grade	Rich loading	5	0,17	0,17	0,17	0,17	0,17	0,16	0,15	0,14	0,13	0,12	0,11	0,1	0,09	0,08	0,07	90'0	0,05	9,0	0,03	0,02	0,01	0,01	0,01	0,01		90,9594	ω	2,049447		44,5
	R	Ŗ	EM																										J)		2,		43,3
	31	392		36	199	178	99	95	90	32	86	163	112	.59	72	178	10	160	25	83	178	89	47	95	161	157	325						42
()	87,31	0,4892		47,7536	50,7561	51,1978	50,8266	50,1294	49,2305	48,1332	46,7898	45,2963	43,6312	41,8159	39,9172	38,0378	36,2801	34,6891	33,7252	33,0783	32,5978	32,2068	31,8647	31,5495	31,2491	30,957	30,6625						40,7
(87,31%)		٦	_	4.	2	Ņ,	2	2	4	4	4	4	4	4	χ̈́	ñ	3	3,	m	m	'n	'n	ώ	ώ	ώ	,	3(						39,3
87,			- 80	4	<u>'¥</u>	8	32	35	4	ᆫ	37	Ū	55	8	35	9	2	∞	<u>∞</u>	<u>∞</u>	<u>∞</u>	<u>∞</u>	<u>∞</u>	∞	∞	<u>∞</u>	∞		က	31	23		37,9
	۵.		EM*1,008	0,23184	0,220954	0,210168	0,199282	0,188395	0,18144	0,17761	0,155837	0,14495	0,134165	0,123278	0,112392	0,101506	0,09072	0,01008	0,01008	0,01008	0,01008	0,01008	0,01008	0,01008	0,01008	0,01008	0,01008		89,4033	87,31	2,093253		36,5
8	age	ρ0	* Z	0,2	0,22	0,2	0,19	0,18	0,1	0,1	0,15	0,1	0,13	0,17	0,1	0,10	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0		89		2,06		35,1
Zhu*1,008	Removal grade	Rich loading			-			_		-		~	_			_													4	28			33,9
Zhı	Š	loa	EM(H14)	0,23	0,2192	0,2085	0,1977	0,1869	0,18	0,1762	0,1546	0,1438	0,1331	0,1223	0,1115	0,1007	0,09	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01		92,4054	88, 28	4,125385		32,9
	en.	ich G	)ME	0	0,	0,	ò	0,	0	0,	0,	0	0,	0	0	0,	0	0	0	0	0	0	0	0	0	0	0		92		4,12		32,0 31,3
					_		_			_	_	_				_			_					_			_				-		30,9
	87,29	0,4891		3146	50,8571	3375	047	3317	1268	927	.60E	941	1121	412	809	193	3136	456	7657	3545	082	227	1873	344	7211	30,5718	507						30,
(%	∞	0,7		47,8146	50,8	51,3379	51,0041	50,3317	49,4268	48,2927	46,7603	44,9941	43,1121	41,2412	39,5088	38,0193	36,8136	35,7459	34,7654	33,8545	33,0081	32,2227	31,4873	31,0344	30,7511	30,5	30,4507						30,3
(87,29%)			⊢	Ĺ								_																		_			30
8			6	90	15	2	25	8	35	8	8	8	93	8	2	35	73	23	28	33	83	00	77	5	5	77	덩		90	87,29	555		30,0
0	و پو		EM*0,9	0,2160	0,2115	0,2070	0,2025	0,1980	0,1935	0,2070	0,1800	0,1530	0,1260	0,0990	0,0720	0,0495	0,0473	0,0450	0,0428	0,0405	0,0383	0,0360	0,0001	0,0001	0,0001	0,0001	0,0001		89,4306	⊗ S	2,140555		29,9
SF2*0,900	oval grade	ng	EP	0	0	0	0	0	0	0	0	_		_	<u> </u>	_	_	_	_	_	0	<u> </u>	_			_	0						29,9
:5*(	val	loading	(4)	+	5	m	5	~	5	~		_	<+	1	Ω	55	52	10	75	ī.	25	8	71	77	77	71	77		630	89,94	2958		29,8
S	m O	h S	EM(H14)	0,24	0,235	0,23	0,225	0,22	0,215	0,23	0,2	0,1	0,14	0,1:	0,0	0,055	0,0525	0,05	0,0475	0,045	0,0425	O,Q	0,0001	0,0001	0,0001	0,0001	0,0001		94,56	8	522		29,8
	Remo	Rich	EP						Ů							_	0		0		0		0	0	0	0	0		റ്		4,62		29,8
	53	31		99	27	37	31	78	99	11	28	33	78	25	51	72	99	45	9	52	93	35	37	86	22	8	8						29,8
	87,29	0,4891		47,8166	50,857	51,3287	50,9731	50,2578	49,2769	48,0111	46,3928	44,5563	42,6178	40,7097	38,961	37,4672	36,2999	35,2945	34,3869	33,552	32,7793	32,0635	31,3937	30,98	30,7207	30,5564	30,4448						29,8
%6		0		47	5	51	50	50	49	48	46	4	42	40	33	37	36	35	34	C,	32	32	31		30	30	30						29,8
(87,29%)			17 T																										2	6	9		29,8
			EM*0,887	0,2173	0,2151	0,2129	0,2107	0,2084	0,2062	0,2040	0,1774	0,1508	0,1242	0,0976	0,0710	0,0444	0,0421	0,0399	0,0377	0,0355	0,0333	0,0310	0,0001	0,0001	0,0001	0,0001	0,0001		89,4175	87,29	127526		29,8
887	Removal grade	þΩ	*	0,2	0,2	0,2	0,2	0,2	0,2	0,2	0,1	0,1	0,1	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0	0,0		89,		2,12		29,8
SF1*0,887	l gr	Rich loading	()																										38	12			29,8
SF.	ova	loa	EM (H14)	0,245	0,2425	0,24	0,2375	0,235	0,2325	0,23	0,2	0,17	0,14	0,11	0,08	0,05	0,0475	0,045	0,0425	0,04	0,0375	0,035	0,0001	0,0001	0,0001	0,0001	0,0001		94,8338	90,12	713805		29,8
	tem.	ich	N	0,	0,2	0	0,2	0	0,2	0,	0	0	0	0	0	0	0,0	0,	0,0	0	0,0	0,	0,0	0,0	0,0	0,0	0,0		8		4,71		29,8 29,8
	LŒ	œ	ш																			[								-	7		29,8 29,8
	Ī																												ncy	ncy			29,8 29,8
<b>B</b> 2			Step	1	7	3	4	2	9	7	∞	6	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24		icie	efficiency			29,8
io 2			S																										eff	effi			29,8
Scenario 2B5			(m)																										ted		nce		29,8
Sce			Height (	24	23	22	21	20	19	18	17	16	15	14	13	12	11	10	6	∞	7	9	2	4	3	7	П		Calculated efficiency	simulated	difference		29,8
	ı		. <u></u>	`	•	•	•	•																					alc	ij	liff		29

Table J.3: Data from simulation of scenario 2B5 in Aspen Plus (eNRTL & Rate-based)

#### Scenario Goal1

						_																											
(%60'06)	60'06	0,4869	T	46,4696	49,3283	49,9963	50,036	49,8861	49,6646	49,4012	49,1008	48,7614	48,3781	47,9447	47,4537	46,8959	46,2602	45,5332	44,698	43,7337	42,6137	41,304	39,7612	37,931	35,7531	33,1843	30,2409					Rate bas [0,51] (90,11%	
	grade	ng	EM*1,025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	0,1025	<del>2</del> ,		3,971972			90,11 0,487
0.1*1,025	Removal grade	Rich loading	EM	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	0,1	92,0234	89,97	2,053356	•	50	3,8326
(90,12%)	90,12	0,4871		47,2302	50,0885	50,5911	50,4006	49,95	49,3323	48,5893	47,7263	46,7403	45,6289	44,3906	43,0297	41,5549	39,9842	38,3475	36,6851	35,0484	33,4895	32,0556	30,7877	29,7222	28,9109	28,2311	27,61					5 50	0,9133 50,791 0,6474 50,492
	rade	lg	EM*1,074	0,1826	0,1826	0,1826	0,1826	0,1826	0,1718	0,1611	0,1504	0,1396	0,1289	0,1181	0,1074	0,0967	0,0859	0,0752	0,0644	0,0537	0,0430	0,0322	0,0215	0,0107	0,0107	0,0107	0,0107	91,6139	90,12	1,493906		50 50	),3213 ),1374 ),9361
Lin*1,074	Removal grade	Rich loading	EM	0,17	0,17	0,17	0,17	0,17	0,16	0,15	0,14	0,13	0,12	0,11	0,1	60'0	80′0	0,07	90′0	0,05	0,04	0,03	0,02	0,01	0,01	0,01	0,01	90,9594	89,91	1,049447		49 49	9,7194 9,4832 9,2293
(90,12%)	90,12	0,4871		47,259	50,0396	50,4253	20,0908	49,4752	48,6833	47,712	46,5111	45,161	43,6207	41,8736	39,9227	37,7984	35,5781	33,3454	32,026	31,1435	30,4785	29,9229	29,421	28,9433	28,4733	28,002	27,5161					48	3,9537 18,658 3,3383 7,9964
	rade	gı	EM*1,015	0,23345	0,222488	0,211628	0,200666	0,189704	0,1827	0,178843	0,156919	0,145957	0,135097	0,124135	0,113173	0,102211	0,09135	0,01015	0,01015	0,01015	0,01015	0,01015	0,01015	0,01015	0,01015	0,01015	0,01015	94, 1292	90,12	4,00917		47 46	17,628 7,2352 5,8141
Zhu*1,015	Removal grade	Rich loading	EM	0,23	0,2192	0,2085	0,1977	0,1869	0,18	0,1762	0,1546	0,1438	0,1331	0,1223	0,1115	0,1007	60'0	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	0,01	92,4054	90,2	2,205385		45 45	5,3664 5,8887 5,3828 1,8453
(90,11%)	90,11	0,487		47,3587	50,179	50,5973	50,293	49,6955	48,8926	47,8791	46,4849	44,8462	43,046	41,1771	39,3561	37,7171	36,3452	35,0578	33,7933	32,5376	31,2943	30,0741	28,8722	28,1303	27,6611	27,3591	27,1549					44 43	1,2784 3,6791 43,05
	rade	lg l	EM*0,91	0,2184	0,2139	0,2093	0,2048	0,2002	0,1957	0,2093	0,1820	0,1547	0,1274	0,1001	0,0728	0,0501	0,0478	0,0455	0,0432	0,0410	0,0387	0,0364	0,0001	0,0001	0,0001	0,0001	0,0001	91,		1,549294		41 40	2,3886 1,6981 0,9765
SF2*0,910	Removal grade	Rich loading	EM(H14)	0,24	0,235	0,23	0,225	0,22	0,215	0,23	0,2	0,17	0,14	0,11	0,08	0,055	0,0525	0,05	0,0475	0,045	0,0425	0,04	0,0001	0,0001	0,0001	0,0001	0,0001	94		4,542958		39 38	0,2277 9,4508 8,6507 7,8277
(90,11%)	90,11	0,487		47,3613	50, 1803	50,591	50, 2682	49,6335	48,7625	47,6287	46,1536	44,4406	42,5662	40,6252	38,7375	37,0379	35,6728	34,4313	33,239	32,0723	30,9302	29,8158	28,721	28,0421	27,6113	27,3336	27,1449	#	#	#		36 36 3	5,9884 5,1351 35,276
	rade	lg	EM*0,896	0,2195	0,2173	0,2150	0,2128	0,2106	0,2083	0,2061	0,1792	0,1523	0,1254	9860'0	0,0717	0,0448	0,0426	0,0403	0,0381	0,0358	0,0336	0,0314	0,0001	0,0001	0,0001	0,0001	0,0001	91,6846	90,11	1,574602		33 32	1,4157 3,5646 2,7293 1,9218
SF1*0,896	Removal grade	Rich loading	EM (H14)	0,245	0,2425	0,24	0,2375	0,235	0,2325	0,23	0,2	0,17	0,14	0,11	80′0	0,05	0,0475	0,045	0,0425	0,04	0,0375	0,035	0,0001	0,0001	0,0001	0,0001	0,0001	94,8338	90,3	4,533805		31 30	1,9218 1,1494 0,4241 9,7521
Goal1			Step	1	2	က	4	2	9	7	∞	6	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	etticiency	tticiency			28 28	9,1424 3,5971 3,1199
Scenario Goal1			Height (m)	24	23	22	21	20	19	18	17	16	15	14	13	12	11	10	6	∞	7	9	2	4	m	2	1	Calculated efficiency	simulated efficiency	difference		27 27	7,7076 7,3593 7,0694 26,837

Table J.4: Data from simulation of scenario Goal1 in Aspen Plus (eNRTL & Rate-based)

### Scenario F17

Scenal	Scenario F17	SF1	SF1*0,772 (83,51%)	1%)	SF2*(	SF2*0,732 (83,49%)	(%6	*n4Z	Zhu*0,818 (83,49%)	(%6	Lin*	Lin*0,863 (83,	(83,51%)	0.	0.1*1,1 (83,50%)	(%
		Removal grade	grade	83,51	Removal grade	ade.	83,49	Removal grade	rade	83,49	Removal grade	grade	83,51	Removal grade	grade	83,5
		Rich loading	ng	0,4837	Rich loading	ρ <u>0</u>	0,4836	Rich loading	Jg Br	0,4836	Rich loading	ng	0,4837	Rich loading	ing	0,4836
Height (m)	Step	EM (H14)	EM*0,772	T	EM(H14)	EM*0,732 T		EM(H14)	EM*0,818 T		EM	EM*0,863	T	EM	EM*1,1	
24	1	0,245	0,1891	47,6719	0,24	0,1757	47,6682	0,23	0,18814	47,6049	0,17	0,14671	47,5929	0,1	0,11	47,0789
23	2	0,2425	0,1872	50,3556	0,235	0,1720	50,3538	0,2192	0,179306	50,2486	0,17	0,14671	50,3387	0,1	0,11	49,8924
22	8	0,24	0,1853	50,6487	0,23	0,1684	50,6564	0,2085	0,170553	50,5122	0,17	0,14671	50,7421	0,1	0,11	50,5008
21	4	0,2375	0,1834	50,2124	0,225	0,1647	50,2418	0,1977	0,161719	50,0637	0,17	0,14671	50,4554	0,1	0,11	50,4844
20	2	0,235	0,1814	49,4706	0,22	0,1610	49,541	0,1869	0,152884	49,3447	0,17	0,14671	49,9107	0,1	0,11	50,2808
19	9	0,2325	0,1795	48,508	0,215	0,1574	48,6488	0,18	0,14724	48,4653	0,16	0,13808	49,2043	0,1	0,11	50,0065
18	7	0,23	0,1776	47,3125	0,23	0,1684	47,571	0,1762	0,144132	47,4301	0,15	0,12945	48,3859	0,1	0,11	49,6909
17	∞	0,2	0,1544	45,8303	0,2	0,1464	46,1598	0,1546	0,126463	46,2005	0,14	0,12082	47,4674	0,1	0,11	49,3391
16	6	0,17	0,1312	44,1826	0,17	0,1244	44,571	0,1438	0,117628	44,8658	0,13	0,11219	46,4524	0,1	0,11	48,9499
15	10	0,14	0,1081	42,4548	0,14	0,1025	42,8968	0,1331	0,108876	43,4004	0,12	0,10356	45,3434	0,1	0,11	48,5192
14	11	0,11	0,0849	40,7378	0,11	0,0805	41,2268	0,1223	0,100041	41,8031	0,11	0,09493	44,1459	0,1	0,11	48,0422
13	12	0,08	0,0618	39,1342	0,08	0,0586	39,661	0,1115	0,091207	40,0967	0,1	0,0863	42,8709	0,1	0,11	47,5128
12	13	0,05	0,0386	37,742	0,055	0,0403	38,2994	0,1007	0,082373	38,3273	60'0	0,07767	41,5344	0,1	0,11	46,9239
11	14	0,0475	0,0367	36,6599	0,0525	0,0384	37,1957	60'0	0,07362	36,5674	0,08	0,06904	40,16	0,1	0,11	46,2671
10	15	0,045	0,0347	35,7099	0,05	9980'0	36, 1962	0,01	0,00818	34,8755	0,07	0,06041	38,7809	0,1	0,11	45,5324
6	16	0,0425	0,0328	34,8276	0,0475	0,0348	35,247	0,01	0,00818	33,9248	90'0	0,05178	37,4349	0,1	0,11	44,7079
∞	17	0,04	0,0309	33,9921	0,045	0,0329	34,3341	0,01	0,00818	33,3226	0,05	0,04315	36,1619	0,1	0,11	43,7793
7	18	0,0375	0,0290	33,1994	0,0425	0,0311	33,4596	0,01	0,00818	32,89	0,04	0,03452	34,9979	0,1	0,11	42,7296
9	19	0,035	0,0270	32,451	0,04	0,0293	32,6286	0,01	0,00818	32,5415	0,03	0,02589	33,9723	0,1	0,11	41,5387
Ŋ	20	0,0001	0,0001	31,7397	0,0001	0,0001	31,8351	0,01	0,00818	32,2351	0,02	0,01726	33,1047	0,1	0,11	40,1844
4	21	0,0001	0,0001	31,3422	0,0001	0,0001	31,3931	0,01	0,00818	31,9497	0,01	0,00863	32,4115	0,1	0,11	38,6449
ю	22	0,0001	0,0001	31,1167	0,0001	0,0001	31,1429	0,01	0,00818	31,6747	0,01	0,00863	31,9168	0,1	0,11	36,9079
2	23	0,0001	0,0001	30,9873	0,0001	0,0001	30,9996	0,01	0,00818	31,4047	0,01	0,00863	31,5235	0,1	0,11	34,9886
1	24	0,0001	0,0001	30,9098	0,0001	0,0001	30,9142	0,01	0,00818	31,1345	0,01	0,00863	31,1807	0,1	0,11	32,9464
	t oio idi	0000		4	07 100	0F 24F4		02 4054	01 2113	4	701000	05 1452			77.00.10	
calculated efficiency	Hicericy	94,0330	7,00		4,	1017,00		92,4054	CLC2,C0	# =	30,	,co		176	7 70,000	
simulated etriciency	midency	90,12	_			83,49		82,28	83,49	#					_	
difference		4,713805	1,7387035	#	4,6229585	1,72514		4,125385	1,761287	#	1,419447	1,63526		# 1,253356	1,5376706	
																Rate ba
31,2 30,9 30,7 30,5	32,3 31,9 31,5	34, 33,8 33,2 32,7	36, 35,6 34,9	38,8 38,2 37,5 36,9	40,8 40,1 39,5	43,1 42,6 42,0 41,4	44,7 44,2 43,7	46,2 45,7 45,2	47,8 47,4 47,0 46,6	48,8 48,5 48,1	49,6 49,4 49,1	50,3 50,1 49,9	50,9 50,8 50,6	48,7 51,0 51,1		sed (83.4
776 457	448 337 698	975	256 192 988	212 618	086 748 311	226 341	941 808 467	152 614	547 617	385 208 838	904 227	986 777	802 001	303	3,48 836	8%)

Table J.5: Data from simulation of scenario F17 in Aspen Plus (eNRTL & Rate-based)

## Appendix K – Comparison of Rate-based and Equilibrium-stage in HYSYS and Plus

#### Scenario H14

			C	omparis	on HYS	YS and	Plus - So	cenario	H14			
	SI	F1	SI	-2	Zł	าน	L	in	0	.1	Rate-b	ased
	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	Plu	S
EM-Factor	1.0	0.995	1.0	1.005	1.106	1.120	1.159	1.170	1.101	1.100	IAF :	= 1
Removal grade[9	90,12	90,05	89,94	89,98	90	90,05	90,01	90	90,01	90,03	8882,0	00%
Rich loading	0,4936	0,4929	0,4931	0,4929	0,4932	0,4929	0,4933	0,4928	0,4932	0,4928	0,48	94
Temp-profile	46,43	48,05	46,41	48,03	45,59	47,91	45,53	47,85	44,79	46,90	54,401	29,4
	49,81	51,56	49,78	51,54	48,58	51,38	48,60	51,40	47,82	50,41	52,035	28,8
	50,59	52,27	50,58	52,26	49,21	52,06	49,37	52,21	48,75	51,41	52,186	28,3
	50,39	52,03	50,41	52,04	48,96	51,82	49,30	52,13	48,93	51,58	51,776	27,9
	49,72	51,38	49,79	51,44	48,32	51,20	48,86	51,70	48,83	51,47	51,408	27,5
	48,72	50,44	48,89	50,57	47,43	50,35	48,20	51,07	48,61	51,27	50,968	27,2
	47,37	49,18	47,70	49,45	46,32	49,28	47,37	50,28	48,33	51,00	50,461	27
	45,65	47,52	46,10	47,90	44,94	47,93	46,40	49,35	48,00	50,69	49,887	26,8
	43,69	45,60	44,25	46,06	43,40	46,41	45,29	48,28	47,62	50,34	49,229	26,6
	41,61	43,51	42,26	44,06	41,69	44,67	44,04	47,06	47,19	49,94	48,491	26,5
	39,58	41,42	40,28	42,02	39,80	42,73	42,67	45,70	46,70	49,49	47,657	26,4
	37,72	39,44	38,42	40,09	37,84	40,64	41,20	44,20	46,13	48,97	46,733	26,3
	36,12	37,71	36,80	38,37	35,92	38,49	39,61	42,58	45,49	48,38	45,705	26,2
	34,80	36,28	35,43	36,92	34,12	36,40	37,98	40,89	44,76	47,70	44,582	26,2
	33,64	35,01	34,20	35,59	32,50	34,40	36,35	39,16	43,92	46,91	43,355	26,1
	32,60	33,82	33,08	34,33	31,32	33,06	34,79	37,45	42,96	46,00	42,042	26,1
	31,63	32,66	32,03	33,09	30,39	32,06	33,34	35,80	41,85	44,94	40,643	26
	30,72	31,53	31,05	31,88	29,63	31,25	32,00	34,24	40,58	43,71	39,188	26
	29,85	30,41	30,11	30,68	28,97	30,55	30,79	32,79	39,13	42,26	37,695	
	29,02	29,28	29,20	29,46	28,38	29,89	29,70	31,46	37,40	40,54	36,208	25,9
	28,32	28,43	28,46	28,55	27,81	29,26	28,73	30,27	35,42	38,52	34,761	25,9
	27,73	27,78	27,82	27,86	27,26	28,62	27,87	29,26	33,21	36,13	33,408	
	27,20	27,27	27,26	27,32	26,70	27,96	27,08	28,33	30,82	33,37	32,176	25,9
	26,73	26,86	26,76	26,88	26,14	27,27	26,31	27,44	28,29	30,21	31,101	25,9
											30,182	25,9
											29,421	24,7

Table K.1: Comparison of Rate-based (Aspen Plus) and Equilibrium (Aspen Plus & HYSYS) for Scenario H14

#### Scenario 2B5

				Compa	arison H	YSYS ar	d Plus	- Scenar	io 2B5			
	SI	F1	SI	F2	Zł	ıu	L	in	0	.1	Rate-	based
	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	PI	us
EM-Factor	0,778	0,887	0,79	0,9	0,88	1,008	0,935	1,005	0,886	1,008	IAF	= 1
Removal grade[%]	87,3	87,29	87,31	87,29	87,29	87,31	87,32	87,3	87,29	87,3	86	,14
Rich loading	0,4635	0,48909	0,4635	0,48909	0,4634	0,48916	0,4635	0,489123	0,4634	0,4891	0,4	857
Temp-profile	46,44	47,82	46,45	47,81	46,36	47,75	46,31	47,73	45,55	47,21	54,27	30,32
	49,42	50,86	49,44	50,86	49,31	50,76	49,33	50,83	48,55	50,36	50,86	30,14
	50,02	51,33	50,05	51,34	49,88	51,20	50,02	51,41	49,41	51,13	51,25	30,03
	49,78	50,97	49,83	51,00	49,63	50,83	49,90	51,21	49,54	51,19	50,66	29,95
	49,17	50,26	49,27	50,33	49,05	50,13	49,47	50,71	49,42	51,03	50,21	29,90
	48,33	49,28	48,49	49,43	48,28	49,23	48,85	50,02	49,19	50,79	49,66	29,86
	47,26	48,01	47,53	48,29	47,35	48,13	48,12	49,20	48,91	50,49	49,03	29,84
	45,93	46,39	46,26	46,76	46,25	46,79	47,28	48,25	48,60	50,16	48,31	29,83
	44,44	44,56	44,83	44,99	45,04	45,30	46,35	47,16	48,24	49,78	47,51	29,82
	42,88	42,62	43,30	43,11	43,71	43,63	45,33	45,96	47,85	49,35	46,61	29,81
	41,31	40,71	41,78	41,24	42,26	41,82	44,22	44,63	47,41	48,87	45,62	29,81
	39,83	38,96	40,33	39,51	40,71	39,92	43,05	43,20	46,92	48,33	44,53	29,81
	38,46	37,47	39,02	38,02	39,03	38,04	41,82	41,70	46,37	47,71	43,35	29,81
	37,35	36,30	37,91	36,81	37,27	36,28	40,55	40,17	45,76	47,02	42,08	29,81
	36,34	35,29	36,88	35,75	35,46	34,69	39,27	38,65	45,07	46,22	40,73	29,81
	35,38	34,39	35,87	34,77	34,28	33,73	37,93	37,20	44,29	45,32	39,33	29,81
	34,43	33,55	34,86	33,85	33,46	33,08	36,63	35,87	43,42	44,28	37,91	29,81
	33,49	32,78	33,84	33,01	32,82	32,60	35,38	34,69	42,43	43,09	36,51	29,81
	32,54	32,06	32,81	32,22	32,30	32,21	34,20	33,66	41,30	41,72	35,17	29,82
	31,60	31,39	31,76	31,49	31,84	31,86	33,14	32,78	40,02	40,16	33,96	29,82
	30,95	30,98	31,06	31,03	31,42	31,55	32,22	32,07	38,56	38,40	32,91	29,82
	30,50	30,72	30,57	30,75	31,01	31,25	31,50	31,54	36,85	36,46	32,06	29,82
	30,19	30,56	30,22	30,57	30,61	30,96	30,88	31,11	34,85	34,43	31,40	29,83
	29,96	30,44	29,97	30,45	30,67	30,66	30,32	30,72	32,51	32,38	30,91	29,84
	•				·	•					30,56	29,87

Table K.2: Comparison of Rate-based (Aspen Plus) and Equilibrium (Aspen Plus & HYSYS) for Scenario 2B5

#### Scenario 6w

				Comp	arison H	HYSYS a	nd Plus	- Scena	rio 6w			
	SI	F1	SI	F2	Zł	าน	L	in	0	.1	Rate-k	pased
	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	Plu	us
EM-Factor	0,591	0,603	0,599	0,612	0,669	0,68	0,708	0,722	0,664	0,68	IAF =	0.29
Removal grade[%]	79	78,98	79,01	79,03	79,02	78,92	79,04	79,03	79,04	79,07	79,	04
Rich loading	0,4426	0,4418	0,4426	0,4420	0,4426	0,4413	0,4427	0,4419	0,4426	0,4420	0,48	370
Temp-profile	45,34	46,50	45,33	46,49	45,26	46,37	46,31	46,30	44,16	45,22	42,55	44,55
	48,31	49,56	48,30	49,56	48,17	49,37	49,33	49,40	47,04	48,24	46,10	44,16
	48,99	50,16	48,99	50,16	48,82	49,94	50,02	50,10	48,00	49,13	48,02	43,77
	48,77	49,87	48,79	49,90	48,59	49,65	49,90	49,96	48,19	49,26	48,93	43,35
	48,15	49,21	48,20	49,28	47,99	49,01	49,47	49,47	48,07	49,11	49,30	42,92
	47,28	48,33	47,39	48,46	47,19	48,20	48,85	48,80	47,81	48,84	49,39	42,4
	46,20	47,23	46,41	47,46	46,25	47,24	48,12	48,02	47,49	48,52	49,35	42,03
	44,89	45,89	45,16	46,18	45,15	46,12	47,28	47,15	47,11	48,15	49,23	41,5
	43,47	44,40	43,78	44,75	43,96	44,90	46,35	46,20	46,70	47,75	49,08	41,02
	41,98	42,83	42,34	43,23	42,69	43,57	45,33	45,16	46,25	47,31	48,91	40,49
	40,49	41,23	40,89	41,69	41,32	42,12	44,22	44,05	45,75	46,83	48,72	39,9
	39,06	39,67	39,50	40,19	39,85	40,52	43,05	42,86	45,21	46,29	48,52	39,38
	37,72	38,24	38,24	38,82	38,29	38,78	41,82	41,60	44,61	45,71	48,31	38,79
	36,58	37,04	37,11	37,64	36,57	36,87	40,55	40,28	43,95	45,06	48,09	38,18
	35,52	35,92	36,05	36,52	34,73	34,76	39,27	38,90	43,22	44,33	47,86	37,54
	34,50	34,83	35,00	35,39	33,39	33,34	37,93	37,49	42,40	43,53	47,62	36,88
	33,46	33,70	33,92	34,22	32,34	32,29	36,63	36,04	41,50	42,62	47,37	36,18
	32,39	32,53	32,80	32,98	31,47	31,45	35,38	34,60	40,48	41,60	47,10	35,46
	31,27	31,29	31,60	31,65	30,71	30,72	34,20	33,18	39,33	40,43	46,83	34,7
	30,08	29,95	30,32	30,18	30,00	30,06	33,14	31,82	38,02	39,09	46,54	33,92
	29,12	28,95	29,29	29,11	29,33	29,41	32,22	30,58	36,52	37,52	46,24	33,10
	28,31	28,19	28,43	28,29	28,65	28,78	31,50	29,53	34,76	35,66	45,93	32,24
	27,61	27,59	27,69	27,65	27,96	28,12	30,88	28,57	32,60	33,39	45,60	31,34
Į	26,98	27,10	27,01	27,13	27,21	27,43	30,32	27,64	29,92	30,53	45,27	30,4
											44,91	29,4

Table K.3: Comparison of Rate-based (Aspen Plus) and Equilibrium (Aspen Plus & HYSYS) for Scenario 6w

#### Scenario Goal1

				Compai	ison HY	SYS and	d Plus -	Scenari	o Goal1			
	SF	1	SF		Zł			in	1	.1	Rate-l	pased
	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	Plu	us
EM-Factor	0,92	0,896	0,891	0,91	0,995	1,015	1,055	1,074	1,015	1,025	IAF =	0,51
Removal grade[%]	90,1	90,11	90.11	90,11	90.10	90,12	90,11	90,11	90,09	90,09	90,	11
Rich loading	0.4904	0,487	0.4874	0,487	0.4873	0,4871	0.4875	0,4871	0,4872	0,4869	0,48	370
Temp-profile	44,98	47,36	44,88	47,36	44,82	47,26	44,78	47,23	44,07	46,47	48,83	43,05
	47,43	50,18	47,31	50,18	47,20	50,04	47,24	50,09	46,52	49,33	50,88	42,39
	47,90	50,59	47,76	50,60	47,62	50,43	47,78	50,59	47,22	50,00	50,91	41,70
	47,67	50,27	47,53	50,29	47,36	50,09	47,68	50,40	47,36	50,04	50,79	40,98
	47,10	49,63	47,00	49,70	46,81	49,48	47,30	49,95	47,30	49,89	50,65	40,23
	46,28	48,76	46,24	48,89	46,06	48,68	46,74	49,33	47,17	49,66	50,49	39,45
	45,17	47,63	45,26	47,88	45,13	47,71	46,04	48,59	46,99	49,40	50,32	38,65
	43,70	46,15	43,90	46,48	43,96	46,51	45,22	47,73	46,76	49,10	50,14	37,83
	41,99	44,44	42,31	44,85	42,65	45,16	44,27	46,74	46,49	48,76	49,94	36,99
	40,15	42,57	40,59	43,05	41,17	43,62	43,19	45,63	46,18	48,38	49,72	36,14
	38,26	40,63	38,85	41,18	39,53	41,87	42,00	44,39	45,80	47,94	49,48	35,28
	36,45	38,74	37,15	39,36	37,73	39,92	40,71	43,03	45,37	47,45	49,23	34,42
	34,84	37,04	35,65	37,72	35,79	37,80	39,33	41,55	44,86	46,90	48,95	33,56
	33,55	35,67	34,39	36,35	33,82	35,58	37,91	39,98	44,27	46,26	48,66	32,73
	32,41	34,43	33,24	35,06	31,92	33,35	36,40	38,35	43,59	45,53	48,34	31,92
	31,38	33,24	32,15	33,79	30,70	32,03	34,90	36,69	42,79	44,70	48,00	31,15
	30,42	32,07	31,11	32,54	29,87	31,14	33,46	35,05	41,86	43,73	47,63	30,42
	29,54	30,93	30,11	31,29	29,27	30,48	32,11	33,49	40,78	42,61	47,24	29,75
	28,74	29,82	29,18	30,07	28,80	29,92	30,90	32,06	39,52	41,30	46,81	29,14
	28,01	28,72	28,30	28,87	28,41	29,42	29,85	30,79	38,07	39,76	46,37	28,60
	27,53	28,04	27,73	28,13	28,08	28,94	28,99	29,72	36,34	37,93	45,89	28,12
	27,23	27,61	27,35	27,66	27,77	28,47	28,34	28,91	34,32	35,75	45,38	27,71
	27,06	27,33	27,13	27,36	27,49	28,00	27,81	28,23	32,03	33,18	44,85	27,36
	26,95	27,14	26,98	27,15	27,20	27,52	27,34	27,61	29,51	30,24	44,28	27,07
•											43,68	26,84

Table K.4: Comparison of Rate-based (Aspen Plus) and Equilibrium (Plus & HYSYS) for Scenario Goal1

#### Scenario F17

				Compa	arison H	YSYS ar	nd Plus	Scena	rio F17			
	SI	F1	SI	F2	ZI	าน	Li	in	0	.1	Rate-	based
	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	HYSYS	Plus	Pl	us
EM-Factor	0,92	0,896	0,891	0,91	0,995	1,015	1,055	1,074	1,015	1,025	IAF =	0,51
Removal grade[%]	83,51	83,51	83,5	83,49	83,54	83,49	83,51	83,51	83,49	83,5	83	,48
Rich loading	0,4354	0,4837	0,4353	0,4836	0,4354	0,4836	0,4353	0,4837	0,4353	0,4836	0,4	836
Temp-profile	46,56	47,67	46,54	47,67	46,46	47,60	46,41	47,59	45,88	47,08	48,72	43,19
	49,70	50,36	49,66	50,35	49,54	50,25	49,58	50,34	49,10	49,89	51,03	42,62
	50,38	50,65	50,35	50,66	50,20	50,51	50,36	50,74	50,09	50,50	51,13	42,03
	50,17	50,21	50,16	50,24	49,98	50,06	50,28	50,46	50,29	50,48	50,98	41,43
	49,58	49,47	49,60	49,54	49,40	49,34	49,85	49,91	50,20	50,28	50,80	40,81
	48,75	48,51	48,84	48,65	48,65	48,47	49,24	49,20	50,00	50,01	50,61	40,17
	47,72	47,31	47,90	47,57	47,75	47,43	48,51	48,39	49,74	49,69	50,40	39,53
	46,45	45,83	46,68	46,16	46,69	46,20	47,69	47,47	49,44	49,34	50,18	38,88
	45,04	44,18	45,33	44,57	45,54	44,87	46,78	46,45	49,11	48,95	49,94	38,22
	43,56	42,45	43,90	42,90	44,29	43,40	45,80	45,34	48,73	48,52	49,69	37,56
	42,07	40,74	42,46	41,23	42,93	41,80	44,75	44,15	48,31	48,04	49,42	36,91
	40,65	39,13	41,09	39,66	41,46	40,10	43,64	42,87	47,84	47,51	49,14	36,26
	39,37	37,74	39,86	38,30	39,90	38,33	42,47	41,53	47,31	46,92	48,84	35,62
	38,31	36,66	38,81	37,20	38,21	36,57	41,26	40,16	46,72	46,27	48,52	35,00
	37,32	35,71	37,85	36,20	36,41	34,88	40,02	38,78	46,06	45,53	48,18	34,40
	36,36	34,83	36,85	35,25	35,20	33,92	38,78	37,43	45,31	44,71	47,83	33,83
	35,41	33,99	35,85	34,33	34,33	33,32	37,51	36,16	44,46	43,78	47,45	33,30
	34,44	33,20	34,82	33,46	33,64	32,89	36,27	35,00	43,49	42,73	47,06	32,80
	33,44	32,45	33,74	32,63	33,06	32,54	35,08	33,97	42,39	41,54	46,65	32,34
	32,40	31,74	32,61	31,84	32,55	32,24	33,97	33,10	41,12	40,18	46,22	31,93
	31,66	31,34	31,80	31,39	32,07	31,95	32,99	32,41	39,64	38,64	45,76	31,57
	31,12	31,12	31,21	31,14	31,61	31,67	32,19	31,92	37,93	36,91	45,29	31,25
	30,72	30,99	30,77	31,00	31,15	31,40	31,48	31,52	35,85	34,99	44,79	30,98
	30,42	30,91	30,44	30,91	30,67	31,13	30,82	31,18	33,33	32,95	44,28	30,75
											43,75	30,55

Table K.5: Comparison of Rate-based (Aspen Plus) and Equilibrium (Aspen Plus & HYSYS) for Scenario F17

## Appendix L – Data from simulation with default Murphree efficiency (HYSYS)

Default efficiencies of	iciencies		า scenar	io, comp	bared wi	th estin	nated M	urphree	each scenario, compared with estimated Murphree efficiencies	cies
SCENARIO	H14		2B5		ew 6		Goal1		F17	
Performance										
Removal grade	90.0	%	87.3	%	79.0	%	90.1	%	83.5	%
rich loading	0.48		0.50		0.46		0.50		0.48	
Simulation										
Removal grade	89.64	%	86.80	%	79.80	%	90.39	%	82.80	%
rich loading	0.4921		0.4619		0.4446		0.4883		0.4332	
number of stages		14		10		8		13	~	<b>∞</b>
From the top	EM	Temp	EM	Temp	EM	Temp	EM	Temp	EM	Temp
stage 1	0,2281	44,7420	0,2288	45,1199	0,2204	43,2570	0,2321	44,5271	0,2316	44,6293
stage 2	0,2327	47,5736	0,2370	47,7228	0,2249	45,3781	0,2360	46,7850	0,2388	47,0896
stage 3	0,2318	48, 1973	0,2361	48,0537	0,2211	45,4028	0,2343	47,0592	0,2351	47,2408
stage 4	0,2279	47,9273	0,2300	47,4268	0,2115	44,3041	0,2300	46,5992	0,2271	46,2780
stage 5	0,2219	47,2082	0,2202	46,2509	0,1969	42,4206	0,2236	45,7525	0,2149	44,5751
stage 6	0,2136	46,1629	0,2066	44,6176	0,1775	39,8190	0,2148	44,5842	0,1963	42,1847
stage 7	0,2026	44,8054	0,1888	42,5241	0,1537	36,4545	0,2028	43,0755	0,1716	39,0642
stage 8	0,1883	43,1245	0,1670	39,9692	0,1263	32,1137	0,1870	41,1959	0,1426	35,1543
stage 9	0,1708	41,1260	0,1423	36,9582			0,1661	38,9476		
stage 10	0,1511	38,8131	0,1175	33,5340			0,1420	36,3798		
stage 11	0,1315	36,2787					0,1188	33,6217		
stage 12	0,1137	33,6392					0,0998	30,8545		
stage 13	0,0987	30,9876					0,0856	28,2022		
stage 14	0,0866	28,3315								

Table L.1: Data from simulation of all scenarios with default Murphree efficiencies (HYSYS, Kent-Eisenberg)

# Appendix M – Data from simulation with different Amine Packages (HYSYS)

#### Scenario H14

	SF1 (	90,12%)			SF2	(89,94%)			Zhu*1,106	(90,00%)	
	90,12	89,76	92,4		89,94	89,55	92,12		90	89,64	92,14
EM	0,4936	0,4925	0,4994	EM	0,4931	0,4919	0,4986	EM	0,4932	0,4922	0,4986
	K-E	L-M	A-G		K-E	L-M	A-G		K-E	L-M	A-G
0,245	46,4342258	46,375271	48,2461886	0,24	46,4113685	46,3431799	48,2162529	0,2544	45,5944732	45,5226925	47,244311
0,2425	49,8081863	49,7342237	51,78971	0,235	49,7839479	49,6961117	51,752214	0,2424	48,5798781	48,491851	50,3915384
0,24	50,5942462	50,5205212	52,5506441	0,23	50,5815423	50,489371	52,5156987	0,2306	49,2122628	49,1254149	51,0035465
0,2375	50,3916977	50,3274063	52,4021596	0,225	50,407563	50,3177753	52,3806515	0,2187	48,9628532	48,8854323	50,7954208
0,235	49,7221879	49,6784739	51,8765501	0,22	49,7927544	49,7138016	51,8873336	0,2067	48,3200054	48,2605762	50,263583
0,2325	48,717496	48,7132793	51,0893233	0,215	48,8857809	48,8304612	51,1645391	0,1991	47,4315337	47,402061	49,5367493
0,23	47,3740912	47,4405605	50,0220597	0,23	47,7042106	47,6939947	50,210008	0,1949	46,3151667	46,3333785	48,6206317
0,2	45,64572	45,8305971	48,6051231	0,2	46,1033341	46,1824434	48,8819033	0,171	44,9382058	45,02989	47,4774334
0,17	43,6919687	44,0351228	46,9209835	0,17	44,2540034	44,4649699	47,2895943	0,159	43,3962696	43,5854605	46,171319
0,14	41,6084485	42,1485705	45,0376821	0,14	42,2624546	42,6761226	45,5065485	0,1472	41,6926451	42,0027997	44,6644414
0,11	39,5754089	40,2934553	43,0464597	0,11	40,2756708	40,8585492	43,6198219	0,1353	39,8032042	40,2688013	42,9345308
0,08	37,7206045	38,5666054	41,0696074	0,08	38,4241064	39,157909	41,7420489	0,1233	37,8416443	38,4499175	40,9717039
0,05	36,1177076	37,0377215	39,2542841	0,055	36,7998207	37,6462777	40,0088318	0,1114	35,9157309	36,6094998	38,7811946
0,0475	34,7967801	35,7595895	37,7537596	0,0525	35,4279717	36,3524216	38,5148982	0,0995	34,1213457	34,8109839	36,3917526
0,045	33,6428227	34,6115189	36,3722083	0,05	34,202939	35,1660927	37,0940872	0,0111	32,5014427	33,0929277	33,8578673
0,0425	32,5978031	33,5349374	35,0252761	0,0475	33,0791142	34,0360983	35,6776956	0,0111	31,3176839	31,852152	32,2315027
0,04	31,6304739	32,4991771	33,6751182	0,045	32,0309215	32,9366462	34,2373797	0,0111	30,3944828	30,8889038	31,1053444
0,0375	30,7194473	31,4857051	32,3036075	0,0425	31,0455979	31,8521395	32,7618493	0,0111	29,633161	30,0917737	30,2526249
0,035	29,852258	30,480374	30,8994102	0,04	30,1060051	30,7701351	31,2454384	0,0111	28,9731376	29,3943022	29,5351991
0,0001	29,0155655	29,4694028	29,4465191	0,0001	29,1991052	29,6772334	29,6749331	0,0111	28,376442	28,7545898	28,8711183
0,0001	28,3244528	28,6472166	28,3838979	0,0001	28,4550561	28,7939661	28,5379972	0,0111	27,8119185	28,1444996	28,2128189
0,0001	27,7288275	27,9528013	27,5642882	0,0001	27,8190383	28,0538746	27,6640677	0,0111	27,2559137	27,5315307	27,5316798
0,0001	27,2037386	27,3439944	26,9035992	0,0001	27,259634	27,4068143	26,9623044	0,0111	26,6968454	26,9004847	26,8099251
0,0001	26,7299504	26,7966397	26,3483613	0,0001	26,7562372	26,8263997	26,37277	0,0111	26,1352527	26,2467091	26,0152418

	Lin*1,159	(90,01%)			0.1 *1,101	(90,01%)	
	90,01	89,63	91,85		90,01	89,87	91,92
EM	0,4933	0,4922	0,4977	EM	0,4932	0,4928	0,498
	K-E	L-M	A-G		K-E	L-M	A-G
0,197	45,5320875	45,4506475	47,1908803	0,1101	44,7875923	44,6188325	46,1441072
0,197	48,5994623	48,4980007	50,4116948	0,1101	47,8157598	47,6108184	49,3022913
0,197	49,3691855	49,2651499	51,1371241	0,1101	48,7530004	48,5468479	50,1825108
0,197	49,2950103	49,1932886	51,067633	0,1101	48,9316644	48,730695	50,3308709
0,197	48,8591013	48,7636835	50,6961444	0,1101	48,8307824	48,6356862	50,2387658
0,1854	48,1980825	48,1154456	50,1460617	0,1101	48,6135331	48,4242047	50,0545142
0,1739	47,3738681	47,3127945	49,4638142	0,1101	48,3322484	48,1493883	49,8203502
0,1623	46,4034553	46,3748567	48,6554694	0,1101	48,0007417	47,826357	49,5456983
0,1507	45,2906169	45,3098147	47,715692	0,1101	47,6211323	47,4566592	49,2297736
0,1391	44,0421069	44,126284	46,6383209	0,1101	47,1882573	47,0365621	48,8681068
0,1275	42,6713357	42,8388432	45,4196878	0,1101	46,6955688	46,5597929	48,4542549
0,1159	41,2026646	41,4702824	44,0616085	0,1101	46,1344955	46,0183666	47,9808822
0,1043	39,610637	40,0065247	42,5739669	0,1101	45,4936315	45,4027192	47,4395034
0,0927	37,9776636	38,5034235	40,9754415	0,1101	44,7609489	44,7016003	46,8195179
0,0811	36,3542442	36,9927776	39,2908635	0,1101	43,9217992	43,9018557	46,1069869
0,0695	34,7941013	35,5073346	37,5207097	0,1101	42,9590958	42,9882033	45,2919077
0,058	33,3362422	34,074093	35,7271286	0,1101	41,853358	41,943239	44,3438617
0,0464	32,0000833	32,7115544	33,9720087	0,1101	40,5836482	40,7474721	43,2288232
0,0348	30,7886265	31,4311958	32,3070409	0,1101	39,1285389	39,3807524	41,9066487
0,0232	29,6978804	30,2425144	30,7720015	0,1101	37,3972112	37,7739185	40,3247269
0,0116	28,7251112	29,1601539	29,4031197	0,1101	35,4216904	35,9237264	38,4110083
0,0116	27,8722519	28,2101949	28,2501178	0,1101	33,2139572	33,8043621	36,0671237
0,0116	27,0762598	27,3161221	27,1949969	0,1101	30,8240497	31,4027426	33,1652772
0,0116	26,3114794	26,4403434	26,1650436	0,1101	28,2918834	28,6937152	29,5667061

Table M.1: Data from simulation of scenario H14 with different Amine Packages

#### Scenario 2B5

	SF1*0,778	8 (87,30%)			SF2*0,79	(87,31%)			Zhu*0,88	(87,29%)	
	87,3	86,63	87,86		87,31	86,66	87,89		87,29	86,63	87,88
EM	0,4635	0,4615	0,4643	EM	0,4635	0,4615	0,4644	EM	0,4634	0,4615	0,4643
	K-E	L-M	A-G		K-E	L-M	A-G		K-E	L-M	A-G
0,1906	46,441007	46,3885456	48,1312483	0,1896	46,4528457	46,3902322	48,1363314	0,2026	46,3648186	46,3052196	48,0200398
0,1887	49,4236972	49,3477662	51,2277414	0,1857	49,4429024	49,3535033	51,2366594	0,1931	49,3087064	49,2232304	51,0769353
0,1867	50,0198783	49,9253846	51,7390509	0,1817	50,0508443	49,9426338	51,756439	0,1837	49,880093	49,7759566	51,564373
0,1848	49,7774947	49,6628621	51,445848	0,1778	49,8309519	49,7032307	51,4816434	0,1742	49,6285977	49,5056076	51,2615279
0,1828	49,1734784	49,0364376	50,8276609	0,1738	49,2664763	49,1173018	50,8978701	0,1647	49,0451389	48,9028478	50,6624294
0,1809	48,3323143	48,1718446	49,9893316	0,1699	48,4909811	48,3186412	50,1182969	0,1586	48,2781527	48,116243	49,8941806
0,1789	47,2631248	47,0809453	48,9237246	0,1817	47,5270866	47,3310834	49,1449549	0,1552	47,3525779	47,1718717	48,9656676
0,1556	45,931612	45,7344767	47,578342	0,158	46,2619845	46,0474832	47,8560978	0,1362	46,2464573	46,0500628	47,8468784
0,1323	44,4431562	44,2424027	46,0505158	0,1343	44,8258867	44,6032501	46,376499	0,1267	45,03704	44,8297568	46,6062393
0,1089	42,8760513	42,6849608	44,4080677	0,1106	43,3041856	43,0860336	44,7814504	0,1173	43,7083583	43,4975411	45,2113813
0,0856	41,3094649	41,1394403	42,7244139	0,0869	41,7788294	41,5753222	43,1488718	0,1078	42,2612189	42,0562054	43,6464078
0,0622	39,8277853	39,6864726	41,0875956	0,0632	40,3344017	40,1496696	41,5716345	0,0982	40,7085823	40,5204729	41,904677
0,0389	38,4620532	38,3516877	39,5987746	0,0435	39,0169936	38,8523811	40,1549555	0,0887	39,031628	38,8729558	39,987515
0,037	37,3480952	37,2664801	38,3540403	0,0415	37,9077695	37,7604472	38,954263	0,0793	37,2715299	37,1543188	37,9070715
0,035	36,3421048	36,2892808	37,1670017	0,0395	36,8771631	36,7499039	37,7976501	0,00881	35,4570228	35,3857155	35,6981673
0,0331	35,3798548	35,3550823	36,0153919	0,0375	35,8687128	35,7656556	36,6092443	0,00881	34,2832297	34,2399579	34,4521268
0,0311	34,4330242	34,4332076	34,8771972	0,0356	34,8599919	34,7822801	35,3754476	0,00881	33,4555502	33,4300243	33,650953
0,0292	33,4893668	33,5090894	33,7297326	0,0336	33,8415271	33,7877113	34,0988214	0,00881	32,8225638	32,8080394	33,0456133
0,0272	32,5443261	32,5756312	32,5553376	0,0316	32,8105327	32,7757308	32,7824065	0,00881	32,3005316	32,2930278	32,5209455
0,0001	31,5955494	31,6282358	31,3451681	0,0001	31,7648129	31,7410843	31,4297002	0,00881	31,8415612	31,8386149	32,0242444
0,0001	30,9511987	30,9809803	30,6017399	0,0001	31,0581827	31,041637	30,6210297	0,00881	31,4172168	31,4175469	31,5303615
0,0001	30,5038654	30,5272413	30,1256751	0,0001	30,568844	30,5574196	30,1232934	0,00881	31,0106397	31,0128331	31,0269104
0,0001	30,1884188	30,2032298	29,8124311	0,0001	30,2239266	30,2166767	29,8075801	0,00881	30,6098907	30,6131921	30,5154959
0,0001	29,9577506	29,9652496	29,6013419	0,0001	29,9725265	29,9686618	29,5997539	0,00881	30,6742999	30,6626694	30,2674148

	Lin*0,935	(87,32%)			0.1 *0,886	(87,29%)	
	87,32	86,7	87,85		87,29	86,78	87,87
EM	0,4635	0,4616	0,4644	EM	0,4634	0,4618	0,4643
	K-E	L-M	A-G		K-E	L-M	A-G
0,1589	46,3130173	46,2676696	47,9584959	0,0886	45,5525108	45,5039813	47,1953991
0,1589	49,3306149	49,2687619	51,0916443	0,0886	48,5492183	48,4833169	50,3115086
0,1589	50,0175141	49,9450814	51,6924194	0,0886	49,4088242	49,3343814	51,0869835
0,1589	49,9034911	49,8201806	51,5237663	0,0886	49,5389144	49,4575479	51,1620856
0,1589	49,4705413	49,3753423	51,0721347	0,0886	49,4152003	49,3269403	51,0188998
0,1496	48,8547514	48,7462523	50,456433	0,0886	49,1911869	49,0957344	50,7938716
0,1403	48,1185332	47,9965775	49,7268771	0,0886	48,9145356	48,8115434	50,524247
0,1309	47,28099	47,1460148	48,8942065	0,0886	48,5983026	48,4874711	50,2184641
0,1216	46,3490499	46,2023947	47,9588257	0,0886	48,2439683	48,1250842	49,8761442
0,1122	45,3277477	45,1719708	46,9199877	0,0886	47,8489547	47,7217863	49,4937958
0,1029	44,2246911	44,0630487	45,778774	0,0886	47,4087231	47,2731511	49,066356
0,0935	43,0498061	42,8874444	44,5396339	0,0886	46,9177701	46,7735924	48,5876172
0,0842	41,8185302	41,6608525	43,2117626	0,0886	46,3692159	46,2164912	48,0500444
0,0748	40,5488139	40,4026249	41,8099528	0,0886	45,7553564	45,5941048	47,4446383
0,0655	39,2655097	39,1349421	40,3553567	0,0886	45,0666389	44,8973846	46,7604745
0,0561	37,9347622	37,8274465	38,8754645	0,0886	44,2915368	44,1157294	45,9841766
0,0468	36,6303532	36,5492683	37,4032271	0,0886	43,4166252	43,236671	45,0991946
0,0374	35,377165	35,3218506	35,9759447	0,0886	42,4265238	42,2455041	44,084631
0,0281	34,2037029	34,1711095	34,6337269	0,0886	41,3031108	41,1249148	42,9136967
0,0187	33,1410069	33,1268718	33,4200298	0,0886	40,0239147	39,8545039	41,5511908
0,00935	32,224969	32,2237414	32,3810077	0,0886	38,5627541	38,4108805	39,9501452
0,00935	31,4970727	31,5031355	31,5665284	0,0886	36,8488477	36,7255726	38,0462604
0,00935	30,878545	30,8868942	30,8457383	0,0886	34,8505171	34,7690935	35,749635
0,00935	30,3171294	30,3227955	30,1493016	0,0886	32,5074239	32,47582	32,936282

Table M.2: Data from simulation of scenario 2B5 with different Amine Packages

#### Scenario 6w

SF1*0,591 (79,00%)					SF2*0,599	(79,01%)			Zhu*0,669 (79,02%)			
	79	78,28	79,53		79,01	78,29	79,53		79,02	78,31	79,54	
EM	0,4426	0,4406	0,4433	EM	0,4426	0,4406	0,4433	EM	0,4426	0,4407	0,4433	
	K-E	L-M	A-G		K-E	L-M	A-G		K-E	L-M	A-G	
0,1448	45,3437118	45,2631779	46,7942146	0,1438	45,3322283	45,2652914	46,8029346	0,1539	45,25502	45,1889499	46,7207597	
0,1433	48,3076912	48,1960163	49,865542	0,1408	48,2975408	48,2053022	49,8812852	0,1466	48,1695055	48,07833	49,7527581	
0,1418	48,991069	48,8630434	50,4320044	0,1374	48,990846	48,8854131	50,4591364	0,1395	48,823279	48,7188827	50,2988355	
0,1404	48,7715543	48,6303382	50,1126804	0,1348	48,7920002	48,6755497	50,1595434	0,1323	48,5938195	48,4786321	49,9788395	
0,1389	48,1460258	47,9925078	49,4171982	0,1318	48,2034636	48,0760846	49,4972693	0,1250	47,9902671	47,8650401	49,3176562	
0,1374	47,2750391	47,1107877	48,4840047	0,1288	47,3928806	47,2548307	48,6162837	0,1204	47,1920118	47,0578482	48,4758725	
0,1359	46,19534	46,0237151	47,3273269	0,1378	46,4072978	46,2596449	47,5373351	0,1179	46,2459956	46,104753	47,482228	
0,1182	44,8943392	44,7212793	45,9170423	0,1198	45,1646008	45,0128168	46,1716883	0,1034	45,1462898	45,0008109	46,3187206	
0,1005	43,4679217	43,2998683	44,3474394	0,1018	43,7840802	43,6343779	44,6419853	0,0962	43,9646225	43,8178943	45,0542222	
0,0827	41,9805287	41,8232126	42,6830827	0,0839	42,3390496	42,196992	43,0178905	0,0890	42,6897286	42,5458012	43,6632122	
0,0650	40,4917605	40,3494266	40,9938435	0,0659	40,890929	40,7602306	41,3653155	0,0818	41,31775	41,1818853	42,1279489	
0,0473	39,0628727	38,9380336	39,3626651	0,0479	39,5031955	39,3845283	39,7636551	0,0746	39,8493473	39,7277874	40,4340609	
0,0296	37,7215397	37,6173635	37,8877099	0,0329	38,2443328	38,1338264	38,3087753	0,0674	38,2872102	38,1863032	38,5703815	
0,0281	36,5797838	36,4955298	36,6733357	0,0314	37,1120166	37,0100712	37,0778513	0,0602	36,5675692	36,4950325	36,5331441	
0,0266	35,5247169	35,461203	35,5601651	0,0300	36,0493776	35,9543076	35,9322039	0,0067	34,7259576	34,6824282	34,3397735	
0,0251	34,4962868	34,454081	34,4672481	0,0285	34,9971777	34,9091872	34,798271	0,0067	33,3862389	33,3569268	32,9151299	
0,0236	33,4594765	33,4382001	33,350652	0,0270	33,9210665	33,841569	33,6353187	0,0067	32,3396052	32,3170878	31,9059262	
0,0222	32,3909416	32,3890547	32,1834049	0,0255	32,7967101	32,7278334	32,4163451	0,0067	31,4696893	31,450551	31,1037173	
0,0207	31,270301	31,2851332	30,9425386	0,0240	31,6028618	31,5468692	31,1181409	0,0067	30,7060679	30,6882374	30,3917663	
0,0001	30,0780343	30,1054608	29,6107093	0,0001	30,3159409	30,2741906	29,7195629	0,0067	30,0025178	29,9846197	29,7095413	
0,0001	29,1162154	29,1502026	28,617918	0,0001	29,2853878	29,2549567	28,6879879	0,0067	29,3258112	29,3094432	29,0243594	
0,0001	28,313683	28,3493127	27,8349126	0,0001	28,4301764	28,4083385	27,8762571	0,0067	28,6517656	28,6386793	28,3291446	
0,0001	27,6109263	27,6423627	27,186772	0,0001	27,6854437	27,6701914	27,2080248	0,0067	27,9553033	27,9462268	27,6212814	
0,0001	26,9770221	26,9954868	26,6276587	0,0001	27,0134156	27,0051424	26,6302252	0,0067	27,2084945	27,2030309	26,8942388	

	Lin*0,708	(79,04%)			0.1*0,664	(79,04%)	
	79,04	78,37	79,52		79,04	78,52	79,46
EM	0,4427	0,4408	0,4433	EM	0,4426	0,4412	0,4431
	K-E	L-M	A-G		K-E	L-M	A-G
0,1204	46,3130173	45,0955887	46,6507817	0,0664	44,1550848	44,0969364	45,661799
0,1204	49,3306149	48,0664352	49,772315	0,0664	47,0423852	46,9671529	48,7475005
0,1204	50,0175141	48,8404505	50,4496308	0,0664	48,0020429	47,9215931	49,6357498
0,1204	49,9034911	48,7500155	50,2747684	0,0664	48,1890552	48,105133	49,745914
0,1204	49,4705413	48,2887921	49,7625448	0,0664	48,0670004	47,9790373	49,5772316
0,1133	48,8547514	47,623756	49,0648838	0,0664	47,8113356	47,7187385	49,2967588
0,1062	48,1185332	46,8385712	48,2518386	0,0664	47,486445	47,3889914	48,9589
0,0991	47,28099	45,9643216	47,3440889	0,0664	47,1146521	47,0123662	48,5810842
0,0920	46,3490499	45,0139812	46,3456464	0,0664	46,7023967	46,5953279	48,1675304
0,0850	45,3277477	43,9949632	45,2540518	0,0664	46,2496339	46,1378397	47,7157669
0,0779	44,2246911	42,9136369	44,0675999	0,0664	45,7534053	45,6368019	47,2194375
0,0708	43,0498061	41,7768631	42,7903056	0,0664	45,2089762	45,0872786	46,6684248
0,0637	41,8185302	40,5922545	41,4359688	0,0664	44,6100848	44,4829865	46,0491678
0,0566	40,5488139	39,3700275	40,0271508	0,0664	43,9490777	43,8160184	45,3470561
0,0496	39,2655097	38,1220432	38,58896	0,0664	43,2171802	43,0781125	44,5537955
0,0425	37,9347622	36,8201814	37,1424978	0,0664	42,4040147	42,2605744	43,6840513
0,0354	36,6303532	35,5081354	35,6841558	0,0664	41,4969942	41,3515402	42,721644
0,0283	35,377165	34,1976277	34,2262282	0,0664	40,4802149	40,3351691	41,6425412
0,0212	34,2037029	32,905907	32,7933928	0,0664	39,3325018	39,1908347	40,4176162
0,0142	33,1410069	31,6574102	31,4199383	0,0664	38,0249324	37,8913778	39,0103994
0,0071	32,224969	30,4853055	30,154347	0,0664	36,5183162	36,399074	37,3613211
0,0071	31,4970727	29,435411	29,0680473	0,0664	34,760174	34,6609781	35,3984399
0,0071	30,878545	28,444433	28,0732392	0,0664	32,5989153	32,5277923	33,0121639
0,0071	30,3171294	27,4436153	27,1051908	0,0664	29,9185772	29,8810104	30,0273898

Table M.3: Data from simulation of scenario 6w with different Amine Packages

#### **Scenario Goal1**

	SF1*0,920	(90,10%)			SF2*0,891	(90,11%)			Zhu*0,995	(90,10%)	
	90,1	90,68	92,05		90.11	89,74	91,06		90.10	89,73	91,07
EM	0.4904	0,4893	0,4929	EM	0.4874	0.4861	0,4896	EM	0.4873	0,4861	0,4896
	K-E	L-M	A-G		K-E	L-M	A-G		K-E	L-M	A-G
0,2254	44,9779401	44,9379624	46,6847171	0,2138	44,8793681	44,8494604	46,5900126	0,22885	44,8166129	44,7688424	46,4661818
0,2231	47,4347861	47,3783518	49,3250486	0,2094	47,3062286	47,2638402	49,2029522	0,218104	47,2047233	47,1371099	49,0381832
0,2208	47,8960614	47,8286209	49,7752346	0,2049	47,7569433	47,7062133	49,6395975	0,207458	47,6188174	47,5393514	49,4467381
0,2185	47,6653619	47,5876681	49,5617952	0,2005	47,5309706	47,471605	49,4218792	0,196712	47,3584857	47,2683316	49,2056117
0,2162	47,1041637	47,0164426	49,0590056	0,1960	46,9971955	46,9296166	48,9312623	0,185966	46,8068503	46,7036618	48,7051668
0,2139	46,281642	46,1857659	48,327636	0,1916	46,2398449	46,1663058	48,2416008	0,1791	46,0642476	45,9484655	48,034534
0,2116	45,1693562	45,0726728	47,3331033	0,2049	45,2587235	45,180249	47,3343775	0,175319	45,1288884	45,0056676	47,1867441
0,1840	43,7002175	43,6169794	45,9972403	0,1782	43,8981501	43,8269808	46,0623313	0,153827	43,9624416	43,8380935	46,1201796
0,1564	41,9928303	41,9436655	44,4128445	0,1515	42,3061294	42,2572186	44,552207	0,143081	42,6511186	42,5331918	44,9009869
0,1288	40,1505045	40,1591454	42,6500056	0,1247	40,5866815	40,5766388	42,8815258	0,132435	41,1734539	41,0732087	43,4861612
0,1012	38,2616467	38,380063	40,7980861	0,0980	38,8482964	38,8918954	41,1374791	0,121689	39,5345887	39,4673548	41,8508441
0,0736	36,4507913	36,6496654	38,9742742	0,0713	37,1538648	37,2649324	39,4269617	0,110943	37,7260293	37,7155918	39,9809732
0,0460	34,8424734	35,1246358	37,3161229	0,0490	35,6464823	35,822848	37,8735876	0,100197	35,7939369	35,8606674	37,8764188
0,0437	33,5486787	33,9026305	35,9563097	0,0468	34,3887608	34,6229926	36,5454319	0,08955	33,8216876	33,9573291	35,5658971
0,0414	32,413141	32,823603	34,6621803	0,0446	33,2420634	33,5244612	35,2446902	0,00995	31,9173983	32,0746298	33,1324199
0,0391	31,375659	31,8196231	33,3801842	0,0423	32,1532519	32,4691783	33,9121307	0,00995	30,7031359	30,8751988	31,7700644
0,0368	30,4180192	30,8644636	32,0966338	0,0401	31,1094595	31,4374455	32,5436698	0,00995	29,8729591	30,0503208	30,9008938
0,0345	29,5379079	29,950282	30,8095522	0,0379	30,1146925	30,4252931	31,1475882	0,00995	29,2687517	29,4412091	30,2505542
0,0322	28,7376377	29,0768318	29,5226176	0,0356	29,177987	29,4349929	29,7405867	0,00995	28,7976576	28,9628942	29,6923635
0,0001	28,0098154	28,2388844	28,2406836	0,0001	28,3041803	28,4693514	28,339363	0,00995	28,4114933	28,5665053	29,1708518
0,0001	27,5333107	27,6842268	27,4908626	0,0001	27,7273369	27,833722	27,5381895	0,00995	28,0753035	28,2162406	28,6631515
0,0001	27,2322907	27,3285391	27,0548123	0,0001	27,3541989	27,4191801	27,0801659	0,00995	27,770395	27,8878476	28,1610235
0,0001	27,0571941	27,1127452	26,8108132	0,0001	27,1262676	27,1620223	26,8258377	0,00995	27,4864077	27,5728054	27,6600285
0,0001	26,9544896	26,9790573	26,6788942	0,0001	26,984001	26,9988784	26,686691	0,00995	27,1968992	27,2444606	27,1430787

	Lin*1,055	(90,11%)			0.1*1,015	(90,09%)	
	90,11	89,76	91		90,09	89,89	91,19
EM	0.4875	0,4862	0,4894	EM	0,4872	0,4865	0,49
	K-E	L-M	A-G		K-E	L-M	A-G
0,17935	44,775511	44,7260847	47,1860194	0,1015	44,0736494	43,9954806	45,6793363
0,17935	47,2415561	47,1759786	49,7706575	0,1015	46,5170678	46,4198811	48,2937903
0,17935	47,7809333	47,7067805	50,3306534	0,1015	47,2181831	47,1160161	48,9787139
0,17935	47,6762569	47,5942571	50,2119412	0,1015	47,3567212	47,25172	49,1078273
0,17935	47,3001513	47,2093661	49,8058813	0,1015	47,3030662	47,1953142	49,0601213
0,1688	46,7420617	46,6418116	49,2071112	0,1015	47,1692086	47,058352	48,9404138
0,15825	46,0447875	45,9379324	48,4645187	0,1015	46,9866651	46,8725001	48,7770545
0,1477	45,2200932	45,1087207	47,5897003	0,1015	46,7620265	46,6443555	48,5758376
0,13715	44,2692302	44,1575556	46,5862212	0,1015	46,4937481	46,3723165	48,3352229
0,1266	43,1947684	43,0886024	45,4584756	0,1015	46,1767925	46,0520554	48,0507671
0,11605	42,0039218	41,9099724	44,2150209	0,1015	45,8047132	45,6783666	47,7162815
0,1055	40,7095432	40,6355635	42,8705194	0,1015	45,3699629	45,2444144	47,3242209
0,09495	39,3329507	39,2872184	41,4480154	0,1015	44,8634205	44,7387549	46,8652805
0,0844	37,9061285	37,8988587	39,983296	0,1015	44,273304	44,1476778	46,3283199
0,07385	36,3987211	36,4438838	38,4482974	0,1015	43,5864227	43,4623204	45,6994204
0,0633	34,9015766	35,0009348	36,9259863	0,1015	42,7878788	42,672476	44,96148
0,05275	33,4559369	33,6039535	35,4521709	0,1015	41,8596702	41,7565673	44,0930184
0,0422	32,1078435	32,2891812	34,0650862	0,1015	40,7801055	40,6910387	43,0664776
0,03165	30,896945	31,0897785	32,7997163	0,1015	39,5245217	39,4591566	41,8460242
0,0211	29,8514418	30,0343751	31,6862657	0,1015	38,066861	38,0396024	40,3838158
0,01055	28,9923407	29,1500808	30,7533352	0,1015	36,3391925	36,3704924	38,6164847
0,01055	28,3417778	28,4711369	30,0370494	0,1015	34,3241662	34,4321152	36,4600375
0,01055	27,8106674	27,905625	29,4404343	0,1015	32,0255487	32,2006486	33,8095528
0,01055	27,3375407	27,3901138	28,89657	0,1015	29,5100701	29,6789934	30,5339106

Table M.4: Data from simulation of scenario Goal1 with different Amine Packages

#### Scenario F17

	SF1*0,67	1 (83,51%)			SF2*0,68	(83,50%)			Zhu*0,76	(83,54%)	
	83,51	82,9	83,88		83,5	82,88	83,86		83,54	82,93	83,9
EM	0,4354	0,4336	0,4356	EM	0,4353	0,4336	0,4355	EM	0,4354	0,4337	0,4357
	K-E	L-M	A-G		K-E	L-M	A-G		K-E	L-M	A-G
0,1644	46,5638618	46,4854016	47,9924756	0,1632	46,535464	46,4776756	48,0273314	0,1748	46,4550151	46,4010113	47,944278
0,1627	49,6986308	49,5917898	51,2001989	0,1598	49,6647088	49,5855025	51,2448118	0,1666	49,5413384	49,4648729	51,1168142
0,161	50,3824386	50,2599244	51,7697829	0,1564	50,3548189	50,2627904	51,8244221	0,1585	50,1973398	50,1069257	51,6660093
0,1594	50,1724243	50,0357465	51,4756909	0,153	50,1623581	50,0582998	51,547797	0,1503	49,9772862	49,8733151	51,3681991
0,1577	49,5803863	49,4296086	50,8317086	0,1496	49,6043633	49,487762	50,9344696	0,142	49,4048791	49,2875214	50,752249
0,156	48,7539877	48,5902769	49,9628817	0,1462	48,8366427	48,7074821	50,1161668	0,1368	48,6495041	48,5186813	49,966058
0,1543	47,7170617	47,5438532	48,8734133	0,1564	47,8950067	47,7545231	49,1038917	0,1339	47,7481282	47,6043851	49,0296368
0,1342	46,4454712	46,2683737	47,5250763	0,136	46,6846617	46,536264	47,7981451	0,1175	46,6864649	46,532325	47,92041
0,1141	45,0360559	44,8621755	46,0106167	0,1156	45,3265549	45,1755207	46,3202641	0,1093	45,5380399	45,3754901	46,706707
0,0939	43,555496	43,392556	44,3948272	0,0952	43,8957117	43,7476838	44,7397886	0,1012	44,2858262	44,1200209	45,3616385
0,0738	42,0690391	41,9231949	42,7512572	0,0748	42,45902	42,3194243	43,1267863	0,093	42,9268867	42,7625435	43,8692544
0,0537	40,6471963	40,5219419	41,1710137	0,0544	41,0872163	40,9598112	41,5674946	0,0847	41,4619722	41,3058416	42,2175821
0,0336	39,3671511	39,2623539	39,7603713	0,0374	39,8569386	39,7428672	40,1663906	0,0765	39,897602	39,7557832	40,397179
0,0319	38,3136512	38,2239963	38,628372	0,0357	38,8141252	38,7120075	39,0030522	0,0684	38,2121419	38,1210266	38,4052637
0,0302	37,3179524	37,2456168	37,5960907	0,034	37,8474214	37,7566023	37,9235853	0,0076	36,4094747	36,333694	36,2642712
0,0285	36,3610336	36,3044699	36,5828629	0,0323	36,8530941	36,77536	36,8558094	0,0076	35,2028267	35,1350044	34,980192
0,0268	35,4079878	35,3663172	35,5506857	0,0306	35,8501492	35,7856108	35,7635162	0,0076	34,325948	34,2646745	34,1204863
0,0252	34,4390604	34,4112929	34,4796465	0,0289	34,8174888	34,7663636	34,6260133	0,0076	33,6393613	33,5837006	33,4622302
0,0235	33,4413121	33,4264668	33,3560828	0,0272	33,7404919	33,7030527	33,4280315	0,0076	33,0635289	33,0130211	32,8939554
0,0001	32,4037723	32,4004089	32,1713108	0,0001	32,6053542	32,5811609	32,15898	0,0076	32,5516376	32,5058619	32,3613589
0,0001	31,6643048	31,666889	31,3896857	0,0001	31,7994047	31,7840343	31,3309559	0,0076	32,0726962	32,0335292	31,8369005
0,0001	31,124269	31,1291999	30,8337113	0,0001	31,2117521	31,2020814	30,7502649	0,0076	31,6083483	31,5773318	31,3154307
0,0001	30,7227815	30,7275356	30,4017676	0,0001	30,7741566	30,7686296	30,3196983	0,0076	31,145663	31,124176	30,7938302
0,0001	30,4184839	30,421212	30,0368103	0,0001	30,4415741	30,438958	29,9815875	0,0076	30,6742999	30,6626694	30,2674148
	lin*0.81 (83.51%)				0 1 *0 76	1 (83 49%)					

	Lin*0,81	(83,51%)			0.1 *0,761	L (83,49%)	
	83,51	82,94	83,84		83,49	83,13	83,93
EM	0,4353	0,4337	0,4355	EM	0,4353	0,4342	0,4357
	K-E	L-M	A-G		K-E	L-M	A-G
0,1368	46,4120033	46,3403595	47,9047755	0,1	45,8819901	45,4913291	47,0134148
0,1368	49,5803871	49,4845026	51,1640905	0,1	49,1022207	48,5962461	50,2598217
0,1368	50,3581506	50,249813	51,8348802	0,1	50,0925831	49,5443602	51,1242514
0,1368	50,2767697	50,1574115	51,6741672	0,1	50,2883746	49,7086995	51,2232898
0,1368	49,8508306	49,7198823	51,2025611	0,1	50,199762	49,586717	51,0717089
0,1288	49,2366859	49,0939199	50,5598837	0,1	49,9985325	49,3493598	50,8257731
0,1208	48,5072525	48,3531565	49,8071437	0,1	49,7403572	49,0535228	50,5311422
0,1127	47,6865202	47,5222156	48,9606599	0,1	49,4415376	48,716744	50,1995217
0,1047	46,7834318	46,6108161	48,0233602	0,1	49,1050804	48,3427747	49,8318964
0,0966	45,8034134	45,6251025	46,9922072	0,1	48,7289884	47,9302664	49,425523
0,0886	44,7523903	44,5715096	45,8638725	0,1	48,3087823	47,475696	48,9759706
0,0805	43,6376874	43,4581269	44,6398395	0,1	47,8392575	46,9742839	48,4776535
0,0725	42,4694337	42,2952229	43,3322264	0,1	47,313085	46,4202276	47,9238115
0,0644	41,2599885	41,0952971	41,963928	0,1	46,7234073	45,8066327	47,306327
0,0564	40,0240882	39,8731098	40,5617403	0,1	46,0596165	45,1253213	46,6153605
0,0483	38,779784	38,6456494	39,1520414	0,1	45,3097279	44,3665237	45,8388492
0,0403	37,5121675	37,4325099	37,7424452	0,1	44,4598402	43,5184288	44,961796
0,0322	36,269328	36,1991215	36,352975	0,1	43,492469	42,5665731	43,9651988
0,0242	35,0789163	35,023104	35,0155157	0,1	42,3866082	41,4928943	42,8244857
0,0161	33,9742898	33,9324938	33,7744185	0,1	41,1157985	40,2746669	41,5070232
0,0081	32,9939789	32,964676	32,6870931	0,1	39,6446902	38,8821631	39,9682498
0,0081	32,1862812	32,1666602	31,8239186	0,1	37,9287428	37,2754473	38,1449078
0,0081	31,4780987	31,4656231	31,0796848	0,1	35,8545875	35,3990736	35,9428175
0,0081	30,8211877	30,8145532	30,3905617	0,1	33,3337217	33,0816047	33,2135459

Table M.5: Data from simulation of scenario F17 with different Amine Packages